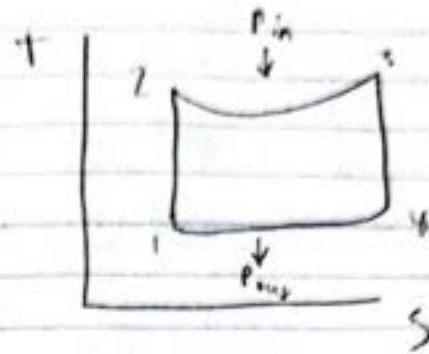
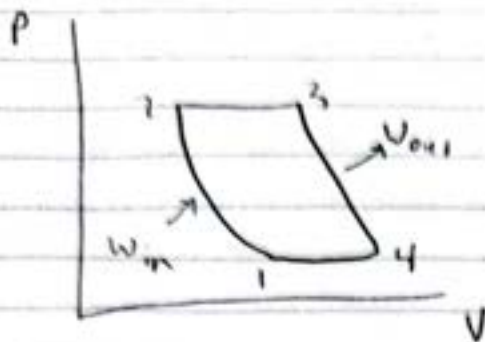


9-80



Process ① $\xrightarrow{\text{isent}}$ ② $\xrightarrow{P \text{ const}}$ ③ $\xrightarrow{\text{isent}}$ ④ $\xrightarrow{P \text{ const}}$

$$T_1 = 273^\circ \text{K}$$

$$P_1 = 70 \text{ kPa}$$

$$T_2 = 527^\circ \text{K}$$

$$P_2 = 700 \text{ kPa}$$

$$T_3 = 1027^\circ \text{K}$$

$$P_3 = 700 \text{ kPa}$$

$$T_4 = 532^\circ \text{K}$$

$$P_4 = 70 \text{ kPa}$$

$$T_2 = T_1 \cdot (P_2/P_1)^{\frac{\gamma-1}{\gamma}}$$

$$T_2 = 273 \cdot (10)^{\frac{1.4-1}{1.4}}$$

$$T_2 = 527^\circ \text{K}$$

$$Q_{in} = C_p(T_3 - T_2)$$

$$T_3 = 527 + \frac{500}{1}$$

$$T_3 = 1027^\circ \text{K}$$

$$T_4 = T_3 \left(\frac{P_4}{P_3} \right)^{\frac{\gamma-1}{\gamma}}$$

$$T_4 = 1027 \left(\frac{1}{10} \right)^{\frac{1.4-1}{1.4}}$$

$$T_4 = 532^\circ \text{K}$$

$$P_2 = P_1 \cdot P$$

$$P_2 = 10 \cdot 70 = 700 \text{ kPa}$$

$$T_3 = 1027^\circ \text{K}$$

$$T_4 = 532^\circ \text{K}$$

$$W_{1-2} = C_p(T_2 - T_1)$$

$$W_{1-2} = 1(527 - 273)$$

$$W_{1-2} = 254 \text{ kJ/kg}$$

$$W_{3-4} = C_p(T_3 - T_4)$$

$$W_{3-4} = 1(1027 - 537)$$

$$W_{3-4} = 495 \text{ kJ/kg}$$

$$P = m(W_{3-4} - W_{1-2})$$

$$P = 1(495 - 254)$$

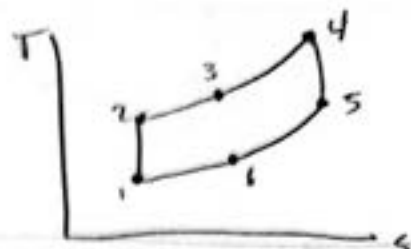
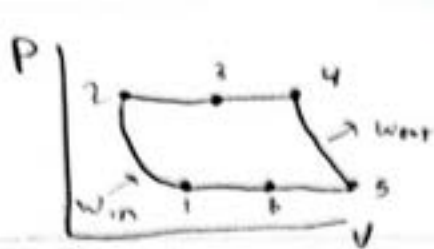
$$P = 241 \text{ kW}$$

$$\eta_{th} = \frac{\text{Power}}{q_{in}}$$

$$\eta_{th} = \frac{241}{500}$$

$$\eta_{th} = 0.482 = 48.2\%$$

9-99



Process	1	2	3	4	5	6
Process	1-2	2-3	3-4	4-5	5-6	6-1
P	$P_1 = 100 \text{ kPa}$	$P_2 = 1000 \text{ kPa}$	$P_3 = 1000 \text{ kPa}$	$P_4 = 1000 \text{ kPa}$	$P_5 = 100 \text{ kPa}$	$P_6 = 100 \text{ kPa}$
T	$T_1 = 303 \text{ K}$	$T_2 = 585 \text{ K}$	$T_3 = 546 \text{ K}$	$T_4 = 1073 \text{ K}$	$T_5 = 556 \text{ K}$	$T_6 = 595 \text{ K}$
Equation	$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{\gamma-1}{\gamma}}$	$T_3 = T_2 - 10 \text{ K}$	$\frac{T_5}{T_4} = \left(\frac{P_5}{P_4}\right)^{\frac{\gamma-1}{\gamma}}$	$T_6 = T_5 - (T_3 - T_2)$		
Calculation	$T_2 = 303(10)^{1.4}$	$T_3 = 556 - 10$	$T_5 = 1073 \left(\frac{1}{10}\right)^{1.4}$	$T_6 = 556 - (546 - 5)$		
Result	$T_2 = 585 \text{ K}$	$T_3 = 546 \text{ K}$	$T_5 = 555.76 \text{ K}$	$T_6 = 595 \text{ K}$		

$$W_{1-2} = C_p (T_2 - T_1)$$

$$W_{1-2} = 1 (585 - 303)$$

$$W_{1-2} = 282 \text{ kJ/kg}$$

$$W_{3-4} = C_p (T_4 - T_5)$$

$$W_{3-4} = 1 (1073 - 556)$$

$$W_{3-4} = 517 \text{ kJ/kg}$$

$$W_{net} = (W_{3-4} - W_{1-2})$$

$$W_{net} = 517 - 282 = 235$$

$$m = \frac{W_{net} \text{ given}}{W_{net} \text{ calc}}$$

$$m = \frac{115}{235} = 0.489 \text{ kg/s}$$

$$q_{in} = m C_p (T_4 - T_3)$$

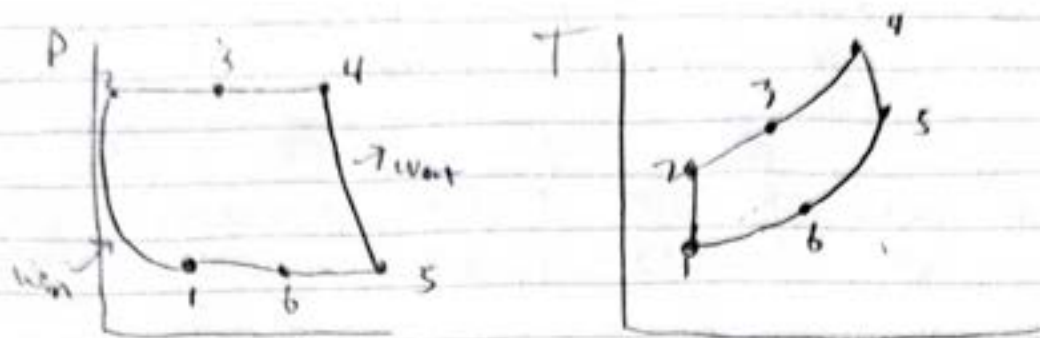
$$q_{in} = 0.489 (1073 - 546)$$

$$q_{in} = 258 \text{ kW}$$

$$q_{out} = m C_p (T_6 - T_1)$$

$$q_{out} = 0.489 (595 - 303)$$

$$q_{out} = 143 \text{ kW}$$



Process	Process	Process	Process	Process	Process	Process
1-2	2-3	3-4	4-5	5-6	6-1	1-2
Isentropic	Isentropic	Isentropic	Isentropic	Isentropic	Isentropic	Isentropic
1	2	3	4	5	6	1
$P_1 = 100 \text{ kPa}$	$P_2 = 700 \text{ kPa}$	$P_3 = 700 \text{ kPa}$	$P_4 = 700 \text{ kPa}$	$P_5 = 100 \text{ kPa}$	$P_6 = 100 \text{ kPa}$	$P_1 = 100 \text{ kPa}$
$T_1 = 310^\circ \text{K}$	$T_2 = 612^\circ \text{K}$	$T_3 = 774^\circ \text{K}$	$T_4 = 1150^\circ \text{K}$	$T_5 = 783^\circ \text{K}$	$T_6 = 310^\circ \text{K}$	$T_1 = 310^\circ \text{K}$
$h_1 = 310.24$	$h_2 = 618.3$	$h_3 = 738.4$	$h_4 = 1219.3$	$h_5 = 803.3$	$h_6 = 310.24$	$h_1 = 310.24$
$P_{r1} = 1.555$	$P_{r2} = 17.4$		$P_{r4} = 700$			

$$P_{r2} = P_r \cdot P_1$$

$$P_{r2} = 7 \cdot 1.555$$

$$P_{r2} = 10.885$$

$$h_{2s} = 541.3$$

$$\eta_c = \frac{h_{2s} - h_1}{h_2 - h_1}$$

$$h_2 = 310.24 + (541.3 - 310.24) / 0.75$$

$$h_2 = 618.3$$

$$\epsilon = \frac{h_3 - h_2}{h_5 - h_2}$$

$$h_3 = 618.3 + 0.82(803.3 - 618)$$

$$h_3 = 738.4$$

$$b_{12} = \frac{1}{P_1} \cdot P_{r1}$$

$$b_{12} = \frac{1}{7} \cdot 200$$

$$P_{r2} = 28.6$$

$$h_{2s} = 712$$

$$\eta_T = \frac{h_4 - h_{4s}}{h_4 - h_5}$$

$$h_5 = 1219 - 0.82(1219 - 712)$$

$$h_5 = 803.3$$

$$T_5 = 783^\circ \text{K}$$

$$W_{net} = W_{out} - W_{in}$$

$$W_{out} = (1719 - 868) = 851$$

$$W_{in} = (614.3 - 310) = 304$$

$$W_{net} = 851 - 304 = 547 \text{ kJ/kg}$$

$$q_{in} = h_4 - h_3$$

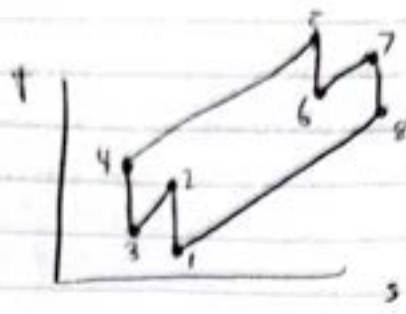
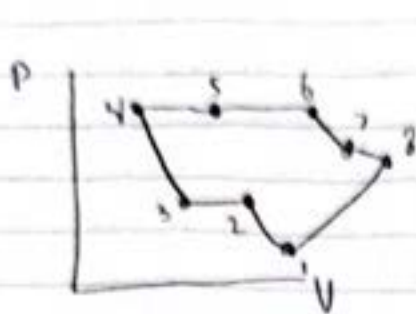
$$q_{in} = 1719 - 738.4$$

$$q_{in} = 980.6$$

$$\eta_{th} = \frac{W_{net}}{q_{in}}$$

$$\eta_{th} = \frac{547}{980.6}$$

$$\eta_{th} = 0.558 = 55.8\%$$



1	2	3	4	5	6	7	8
$P_1 = 100 \text{ kPa}$	$P_2 = 100 \text{ kPa}$	$P_3 = 100 \text{ kPa}$	$P_4 = 100 \text{ kPa}$	$P_5 = 100 \text{ kPa}$	$P_6 = 100 \text{ kPa}$	$P_7 = 100 \text{ kPa}$	$P_8 = 100 \text{ kPa}$
$T_1 = 300^\circ \text{K}$	$T_2 = 410^\circ \text{K}$	$T_3 = 300^\circ \text{K}$	$T_4 = 410^\circ \text{K}$	$T_5 = 1200^\circ \text{K}$	$T_6 = 910^\circ \text{K}$	$T_7 = 1200^\circ \text{K}$	$T_8 = 910^\circ \text{K}$
$h_1 = 300$	$h_2 = 411.3$	$h_3 = 300$	$h_4 = 411.3$	$h_5 = 1270$	$h_6 = 916.4$	$h_7 = 1270$	$h_8 = 916.4$
$P_{r1} = 1.396$	$P_{r2} = 4.159$			$P_{r5} = 239$	$P_{r6} = 70.3$		

$$P_{r2} = (P_r) P_{r1}$$

$$P_{r2} = (3) 1.396$$

$$P_{r2} = 4.159$$

$$h_2 = 411.3$$

$$T_2 = T_4 = 410^\circ \text{K}$$

$$P_{r6} = \left(\frac{1}{P_r}\right) P_{r5}$$

$$P_{r6} = \left(\frac{1}{3}\right) 239$$

$$P_{r6} = 70.3$$

$$h_6 = 916.4$$

$$T_6 = T_8 = 910^\circ \text{K}$$

$$w_{in} = 2(h_2 - h_1)$$

$$w_{in} = 2(411 - 300)$$

$$w_{in} = 222$$

$$w_{out} = 2(h_5 - h_6)$$

$$w_{out} = 2(1270 - 916) = 663$$

$$w_{net} = w_{out} - w_{in}$$

$$w_{net} = 663 - 222 = 441$$

$$m = \frac{w_{net}}{w_{ref}}$$

$$m = \frac{110,000}{441} = 250 \text{ kg/s}$$

12)

