

$T_2 = T_1 + \text{Compressor discharge temp rise}$

$$T_2 = T_1 + \text{assume } 100^\circ\text{F} (55.56^\circ\text{C})$$

$$T_2 = 40^\circ\text{F} + 100^\circ\text{F} = 140^\circ\text{F} (60^\circ\text{C})$$

$$\gamma_2 = 1.13$$

$$\Delta T_{1s} = 40^\circ\text{F} \left(\frac{P_{\text{cond}}}{P_1} \right)^{\frac{(\gamma-1)}{\gamma}} = 40^\circ\text{F} \left(\frac{220 \text{ psia}}{34.14 \text{ psia}} \right)^{\frac{(1.13-1)}{1.13}} = 121.5^\circ\text{F} \quad (66.4^\circ\text{C})$$

$$T_{2s} = T_1 + \Delta T_{1s} = 40^\circ\text{F} + 121.5^\circ\text{F} = 161.5^\circ\text{F}$$

$$\eta_c = \frac{(T_{2s} - T_1)}{T_2 - T_1} = \frac{161.5^\circ\text{F} - 40^\circ\text{F}}{140^\circ\text{F} - 40^\circ\text{F}} = 151.5^\circ\text{F}$$

$$h_4 = 24.864 + 0.8 \cdot 83.397 = 92.01$$

$$\dot{m} = \frac{\dot{Q}_{in}}{h_4 - h_3} = \frac{941.055}{94.5 - 92} = 125.47 \text{ lb}_m/\text{s}$$

Problem 1

C) It is assumed that the refrigerant enters the evaporator as a saturated vapor (100% quality) and

exits the condenser as a saturated liquid (100% quality).

$$COP = \frac{Q_{out}}{W_{in}} = \frac{452.53}{3262.22} = 0.138$$

D)

$$Q_{out} = 452.53 \text{ Btu/s}$$

$$W_{in} = \dot{m} (h_2 - h_1) = 125.47 \text{ lb}_m/\text{s} \cdot (125.5 - 99.5) \text{ Btu/lb}_m = 3262.22 \text{ Btu/s}$$

Problem 1