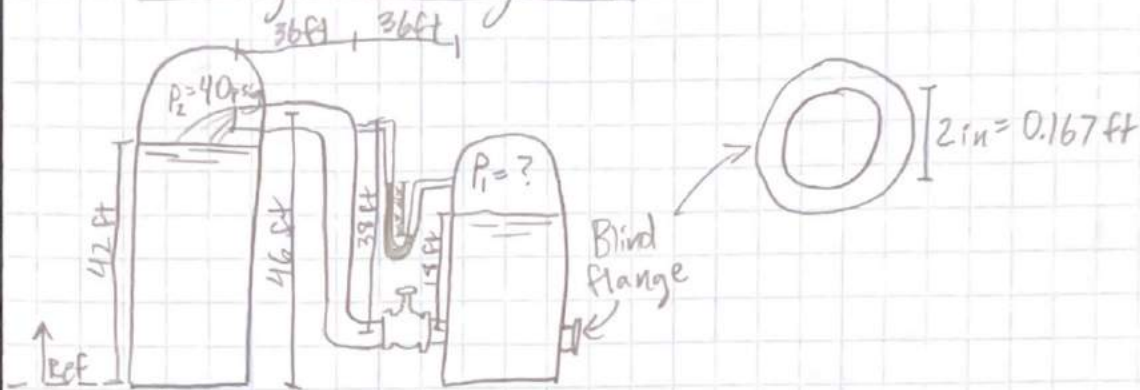


Fluid Mechanics Test #2

Brady
Semtner

① Purpose: Find force magnitude + location on a blind flange on the bottom of the right tank if the flow rate is 150 gpm.

Drawings + Diagrams:



Sources: Mott + Untener: Applied Fluid Mechanics
8th edition

Design considerations:

Assume:

- Incompressible fluids
- Steady flow
- Isothermal at 77°F
- Alcohol + mercury don't mix

Data + Variables:

$$Q = 150 \text{ gpm} = 0.3342 \frac{\text{ft}^3}{\text{s}}$$

$$\gamma_{\text{EA}} = 49.01 \frac{\text{lb}}{\text{ft}^3}$$

$$D_{\text{pipe}} = 0.1723 \text{ ft}$$

$$P_2 = 40 \text{ psig} = 5760 \frac{\text{lb}}{\text{ft}^2}$$

$$\gamma_{\text{Hg}} = 844.9 \frac{\text{lb}}{\text{ft}^3}$$

$$f_T = 0.019 \quad f = 2.99 \times 10^{-5} \frac{1}{\text{ft}}$$

Materials:

Ethyl Alcohol, Mercury, Air

Procedure & Calculations:

- First I'll find pressure at P_1
- I'll use these equations

$$\Delta P = \gamma h \quad Q = vA \quad \frac{P_1}{\gamma} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\gamma} + \frac{v_2^2}{2g} + z_2 + h_{L1-2}$$

- $Q = vA$ used to find v_2

$$v_2 = \frac{Q}{A} \quad A = \frac{\pi}{4} D^2 = \frac{\pi}{4} (0.1723)^2 = 0.02332 \text{ ft}^2$$

$$v_2 = \frac{0.3342 \frac{\text{ft}^3}{\text{s}}}{0.02332 \text{ ft}^2} = 14.333 \frac{\text{ft}}{\text{s}}$$

- Darcy's equation + energy losses at valve, entrance, & elbows

$$h_L = f \cdot \frac{L}{D} \cdot \frac{v_2^2}{2g} + K_{\text{entrance}} \cdot \frac{v_2^2}{2g} + K_{\text{valve}} \cdot \frac{v_2^2}{2g} + 2 K_{\text{elbows}} \cdot \frac{v_2^2}{2g}$$
$$h_L = f \cdot \frac{L}{D} \cdot \frac{v_2^2}{2g} + 0.5 \frac{v_2^2}{2g} + 8 f_r \frac{v_2^2}{2g} + 2 \cdot 30 f_r \frac{v_2^2}{2g}$$

$$f = \frac{64}{Re} = \frac{64}{\frac{5.0 \times 10^{-6}}{0.1723 \text{ ft}}} = 2.9 \cdot 10^{-5}$$

$$L = 36 + 38 + 36 = 110 \text{ ft}$$

$$h_L = 5.78 \text{ ft} \quad \text{Plugged into excel sheet from last test}$$

Plug into Bernoulli's

$$P_1 = \left(\frac{P_2}{\gamma} + \frac{v_2^2}{2g} + z_2 + h_{L1-2} - z_1 \right) \gamma$$

$$P_1 = \left(\frac{5760 \frac{\text{lb}}{\text{ft}^2}}{49.01 \frac{\text{lb}}{\text{ft}^3}} + 46 \text{ ft} + \frac{(14.333 \frac{\text{ft}}{\text{s}})^2}{2(32.2 \frac{\text{ft}}{\text{s}^2})} + 5.78 \text{ ft} \cdot 26 \text{ ft} \right) \cdot 49.01 \frac{\text{lb}}{\text{ft}^3} \Rightarrow P_1 = 7179.62 \frac{\text{lb}}{\text{ft}^2}$$

- Now plug into $\Delta P = \gamma h$ + add surface pressure (P_1) to find pressure at flange depth

$$\Delta P = \gamma h + P_1$$

$$\Delta P = (49.01 \frac{\text{lb}}{\text{ft}^3}) (18 \text{ ft}) + 7179.62 \frac{\text{lb}}{\text{ft}^2} = 8061.8 \frac{\text{lb}}{\text{ft}^2}$$

- Use $F = P \cdot A$ to find force magnitude and $L_p = \frac{I_c}{L_c A} + L_c$ to find location

$$F = 8061.8 \frac{\text{lb}}{\text{ft}^2} \cdot 0.02332 \text{ ft}^2 = 188.01 \text{ lb} = F$$

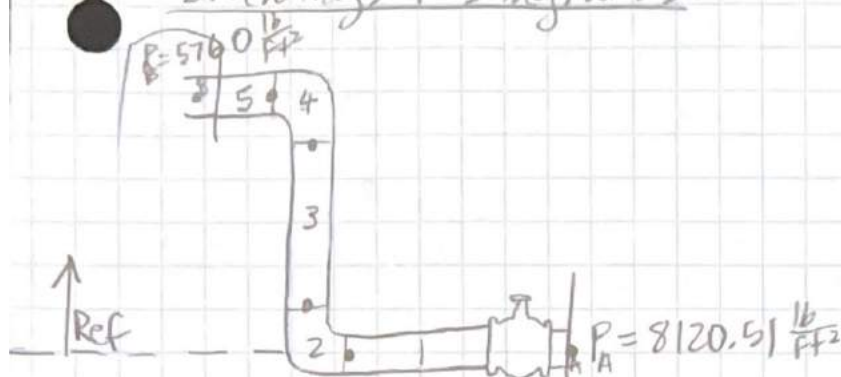
Centroid of circle = $\frac{D}{2} \Rightarrow$ Location at centroid. checked with

$$\text{math: } L_p = \frac{I_c}{L_c A} + L_c = \frac{0.00146 \text{ ft}^4}{(18 \text{ ft})(0.02332 \text{ ft}^2)} + 18 \text{ ft} \Rightarrow L_p = 18.0035 \text{ ft}$$

$$I_c = \frac{\pi D^4}{64} = \frac{\pi (0.1723)^4}{64} = 0.00146 \text{ ft}^4$$

② Purpose: Find Horizontal + Vertical forces in the system.

Drawings + Diagrams:



Sources: Mott + Untener: Applied Fluid Mechanics 8th edition

Design Considerations:

Assume:

- Incompressible Fluids
- Steady Flow
- Isothermal at 77°F

Data + Variables:

$$\bar{P}_{EA} = 1.53 \frac{\text{slug}}{\text{ft}^3} \quad Q = 150 \text{ gpm} = 0.334 \frac{\text{ft}^3}{\text{s}} \quad v = 14.333 \frac{\text{ft}}{\text{s}}$$

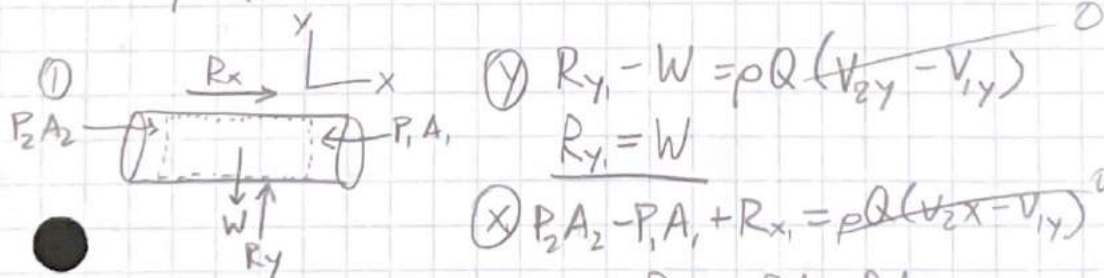
$$A = 0.0233 \text{ ft}^2$$

Materials:

Ethyl Alcohol

Procedure + calculations:

$$\Sigma F = \rho Q \Delta v$$



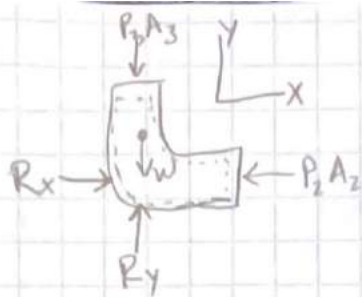
$$\textcircled{y} \quad R_{y1} - W = \rho Q (v_{2y} - v_{1y})$$

$$R_{y1} = W$$

$$\textcircled{x} \quad P_2 A_2 - P_1 A_1 + R_{x1} = \rho Q (v_{2x} - v_{1x})$$

$$R_{x1} = P_2 A_2 - P_1 A_1$$

②



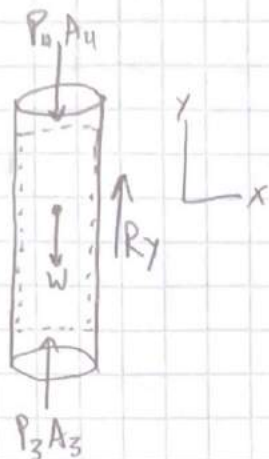
⊗ $R_{x2} - P_2 A_2 = \rho Q (v_{2x} - v_{1x})$

$R_{x2} = P_2 A_2 + \rho Q (-v_{1x})$

⊙ $R_{y2} - W - P_3 A_3 = \rho Q (v_{2y} - v_{1y})$

$R_{y2} = W + P_3 A_3 + \rho Q (v_{2y})$

③

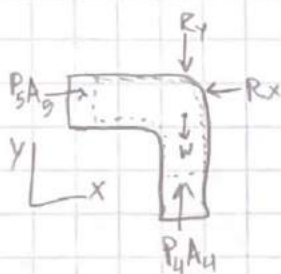


⊙ $R_{y3} - W + P_3 A_3 - P_4 A_4 = \rho Q (v_{2y} - v_{1y})$

$R_{y3} = W + P_4 A_4 - P_3 A_3$

⊗ Nothing in x direction

④



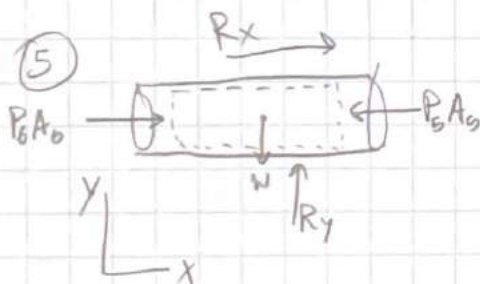
⊗ $P_5 A_5 - R_{x4} = \rho Q (v_{2x} - v_{1x})$

$R_{x4} = P_5 A_5 - \rho Q (v_{2x})$

⊙ $P_4 A_4 - W - R_{y4} = \rho Q (v_{2y} - v_{1y})$

$R_{y4} = P_4 A_4 - W - \rho Q (0 - v_{1y})$

⑤



⊗ $R_{x5} + P_6 A_6 - P_5 A_5 = \rho Q (v_{2x} - v_{1x})$

$R_{x5} = P_5 A_5 - P_6 A_6$

⊙ $R_{y5} - W = \rho Q (v_{2y} - v_{1y})$

$R_{y5} = W$

$\Sigma R_x = R_{x1} + R_{x2} + R_{x3} + R_{x4} + R_{x5}$

$R_x = P_2 A_2 - P_1 A_1 + P_2 A_2 + \rho Q (-v) + P_5 A_5 - \rho Q (v) + P_5 A_5 - P_6 A_6$

$R_x = A(P_2 - P_1 + P_2 + P_5 + P_5 - P_6) - 2\rho Q (v)$

$R_x = A(2P_2 + 2P_5 - P_1 - P_6) - 2\rho Q (v)$

$$\sum R_y = R_{y1} + R_{y2} + R_{y3} + R_{y4} + R_{y5}$$

$$R_y = W + W + P_3 A + \rho Q L v + W + P_4 A - P_3 A + P_4 A - W + \rho Q L v + W$$

$$R_y = 3W + 2P_4 A + 2\rho Q L v$$

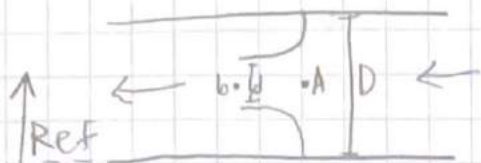
$$2\rho Q L v = 2(1.53 \frac{\text{lb} \cdot \text{s}^2}{\text{ft}^3}) (0.334 \frac{\text{ft}^3}{\text{s}}) (14.333 \frac{\text{ft}}{\text{s}}) = 14.65 \text{ ft} \cdot \text{lb}$$

$$R_x = 0.0233 \text{ ft}^2 (2P_2 + 2P_5 - P_1 - P_6) - 14.65 \text{ lb} \cdot \text{ft}$$

$$R_y = 3W + 2P_4 (0.0233 \text{ ft}^2) + 14.65 \text{ lb} \cdot \text{ft}$$

③ Purpose: Find pressure drop across flow nozzle

Drawings & Diagrams:



Sources: Mott & Untener: Applied Fluid Mechanics 8th edition

Design Considerations:

Assume:

- Incompressible Fluids
- Steady Flow
- Isothermal at 77°F

Data & Variables:

$$Q = 0.3342 \frac{\text{ft}^3}{\text{s}} \quad \beta = 0.5$$

From problem ①

$$V_1 = 14.333 \frac{\text{ft}}{\text{s}}$$

$$\rho_{\text{EA}} = 1.53 \frac{\text{slugs}}{\text{ft}^3}$$

$$D = 0.1723 \text{ ft}$$

$$\gamma_{\text{EA}} = 49.01 \frac{\text{lb}}{\text{ft}^3}$$

$$\mu_{\text{EA}} = 2.1 \cdot 10^{-5} \frac{\text{lb} \cdot \text{s}}{\text{ft}^2}$$

Materials:

Ethyl Alcohol

Procedure & Calculations:

• Find d :

$$\beta = \frac{d}{D} \Rightarrow 0.5 = \frac{d}{0.1723 \text{ ft}} \Rightarrow d = 0.08615 \text{ ft}$$

• Find Area in tube & in throat of nozzle:

$$A_1 = \frac{\pi D^2}{4} = \frac{\pi (0.1723)^2}{4} = 0.0233 \text{ ft}^2$$

$$A_2 = \frac{\pi d^2}{4} = \frac{\pi (0.08615)^2}{4} = 0.005829 \text{ ft}^2$$

• Find N_R :

$$N_R = \frac{\rho V D}{\mu} = \frac{(1.53 \frac{\text{slugs}}{\text{ft}^3})(14.333 \frac{\text{ft}}{\text{s}})(0.1723 \text{ ft})}{2.1 \cdot 10^{-5} \frac{\text{lb} \cdot \text{s}}{\text{ft}^2}} = 180051.78$$

• Find C :

$$C = 0.9975 - 6.53 \sqrt{\frac{\beta}{N_R}} = 0.9975 - 6.53 \sqrt{\frac{0.5}{180051.78}} \Rightarrow C = 0.9866$$

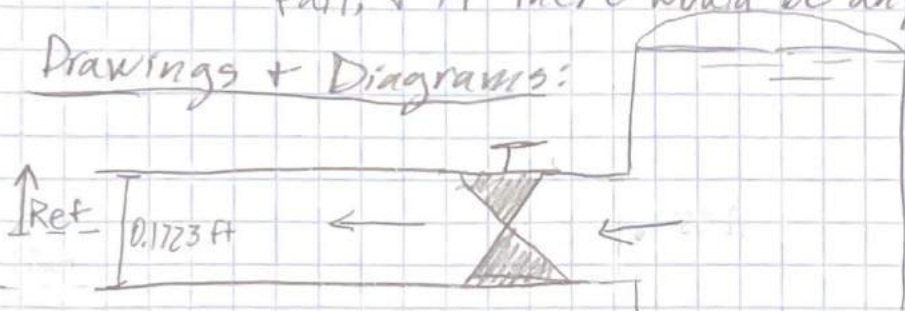
• Plug into this equation to find pressure drop:

$$V_1 = C \sqrt{\frac{2g(P_1 - P_2)}{\left(\frac{A_1}{A_2}\right)^2 - 1}} \quad 14.333 \frac{\text{ft}}{\text{s}} = 0.9866 \sqrt{\frac{(2)(32.2 \frac{\text{ft}}{\text{s}^2})(\Delta P)}{\left(\frac{0.0233 \text{ ft}^2}{0.005829 \text{ ft}^2}\right) - 1}}$$

• This gives: $\Delta P = 482.08 \frac{\text{lb}}{\text{ft}^2}$

④ Purpose: Find pressure increment in pipe if valve closes, if it would fail, & if there would be any cavitation.

Drawings + Diagrams:



Sources: Mott + Untener: Applied Fluid Mechanics 8th edition

Design Considerations:

Assume:

- Isothermal at 77°F
- Incompressible fluid (Ethyl Alcohol)

Data + Variables:

$$E = 200 \text{ GPa} \quad E_{\text{steel}} = 1.00 \quad D_{\text{outer}} = 2.375 \text{ in} = 0.1979 \text{ ft} \quad D_{\text{inner}} = 0.1723 \text{ ft}$$

$$Y_{\text{steel}} = 0.40 \quad \delta = t_{\text{basic wall thickness}} = 0.154 \text{ in} = 0.0128 \text{ ft} \quad \rho_{\text{EA}} = 1.53 \frac{\text{slug}}{\text{ft}^3}$$

Materials:

$$E_{\text{Ethyl Alcohol}} = 130,000 \text{ psi} = 18720000 \frac{\text{lb}}{\text{ft}^2}$$

Ethyl Alcohol, steel

Procedure + Calculations:

$$P = P_{oper} + \Delta P$$

$$\Delta P = \rho v C$$

$$C = \frac{\sqrt{\frac{E_0}{\rho}}}{\sqrt{1 + \frac{E_0 D_{inner}}{E \delta}}}$$

$$t = \frac{P D_{outer}}{2(SE + PY)}$$

For the pipe not to break: $t < t_{actual}$

$$t < 0.0128 \text{ ft}$$

$$E = 200 \text{ GPa} = 2.9 \cdot 10^7 \text{ Psi} = 4176000000 \frac{\text{lb}}{\text{ft}^2}$$

$$\frac{P_A}{\rho} + \frac{v_A^2}{2g} + z_A = \frac{P_B}{\rho} + \frac{v_B^2}{2g} + z_B + h_{LA-B}$$

$$P_{oper} = 8061.8 \frac{\text{lb}}{\text{ft}^2} \leftarrow \text{From problem ①} \rightarrow v = 14.333 \text{ ft/s}$$

$$C = \frac{\sqrt{\frac{18720000 \frac{\text{lb}}{\text{ft}^2}}{1.53 \frac{\text{slug}}{\text{ft}^3}}}}{\sqrt{1 + \frac{(18720000 \frac{\text{lb}}{\text{ft}^2})(0.1723 \text{ ft})}{(4176000000 \frac{\text{lb}}{\text{ft}^2})(0.0128 \text{ ft})}}} = 3396.9 \frac{\text{ft}}{\text{s}}$$

$$\Delta P = \rho v C = (1.53 \frac{\text{slug}}{\text{ft}^3})(14.333 \frac{\text{ft}}{\text{s}})(3396.9 \frac{\text{ft}}{\text{s}}) = 74476.7 \frac{\text{lb}}{\text{ft}^2}$$

$$P = P_{oper} + \Delta P = 8061.8 \frac{\text{lb}}{\text{ft}^2} + 74476.7 \frac{\text{lb}}{\text{ft}^2} = \boxed{82538.5 \frac{\text{lb}}{\text{ft}^2}}$$

$$t = \frac{P D_{outer}}{2(SE + PY)} = \frac{(82538.5 \frac{\text{lb}}{\text{ft}^2})(0.1979 \text{ ft})}{2((2882189.92 \frac{\text{lb}}{\text{ft}^2})(1.00) + (82538.5 \frac{\text{lb}}{\text{ft}^2})(0.4))} \quad S = 20 \text{ ksi} = 2882189.92 \frac{\text{lb}}{\text{ft}^2}$$

$$t = 0.0028 \text{ ft} \quad \boxed{0.0028 \text{ ft} < 0.0128 \text{ ft} \therefore \text{Pipe won't break}}$$

There will be cavitation if $P_{oper} > P_{sat@T=77^\circ\text{F}}$

The point with the lowest pressure in the system is in the left tank, which is not vaporizing. Therefore the system will not experience cavitation because the place with the lowest pressure is not vaporizing.

Part
A

Summary:

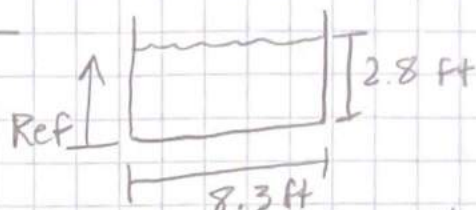
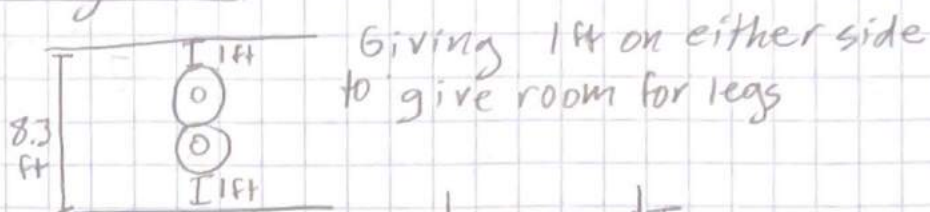
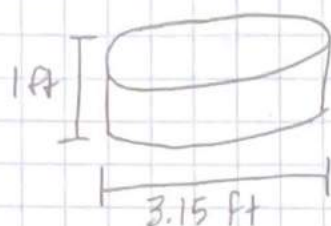
The system pumps ethyl Alcohol. If a blind flange is placed at the Bottom of the right tank, The force on it will be 188.0 lb at its centroid. As the fluid flows through the pipes, it exerts forces on the pipes at the straight portions and the elbows. If a flow nozzle were to be placed in the pipe, it would experience a pressure drop of $482.08 \frac{\text{lb}}{\text{ft}^2}$ across it. If the valve were suddenly closed, the pipe would be able to withstand the pressure and no cavitation is present in the system.

Analysis:

If a flow nozzle were to be placed in the system, there is a good chance it would experience cavitation. It would create a low pressure environment & it might damage the flow nozzle. My best solution for this would be to use a cheaper instrument to measure the flow rate like an orifice plate. When it is damaged, it will be cheaper to replace.

⑤ Purpose: Design a lazy river that won't drown a 4-year-old + determine its flow rate

Drawings + Diagrams:



Sources: Mott + Untener: Applied Fluid mechanics 8th edition

Design Considerations:

Assume:

- Average height of 4-year-old in America = 3.33 ft
- Height up to neck $\approx$ 2.8 ft
- Open channel
- Trowel finished concrete

Data + Variables:

$$\text{slope} = 0.18 \Rightarrow S = 0.001 \quad \text{Depth} = 2.8 \text{ ft}$$
$$n = 0.013 \quad \text{Width} = 8.3 \text{ ft}$$

Materials:

Water

Procedure + Calculations:

- Find A , WP , R

$$A = h \cdot b = 2.8 \text{ ft} \cdot 8.3 \text{ ft} = 23.24 \text{ ft}^2$$

$$R = \frac{A}{WP} = \frac{23.24 \text{ ft}^2}{13.9 \text{ ft}} = 1.67 \text{ ft}$$

$$WP = 2h + b = 2 \cdot 2.8 \text{ ft} + 8.3 \text{ ft} = 13.9 \text{ ft}$$

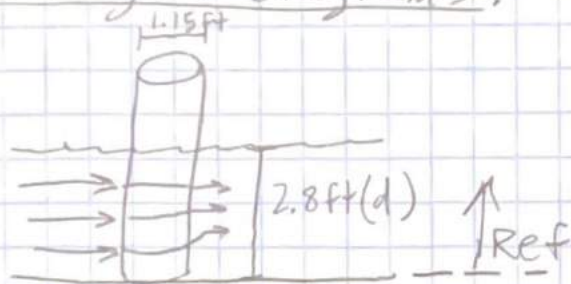
- Find Q :

$$Q = \left(\frac{1.49}{n} \right) A R^{\frac{2}{3}} S^{\frac{1}{2}}$$

$$Q = \left(\frac{1.49}{0.013} \right) (23.24 \text{ ft}^2) (1.67 \text{ ft})^{\frac{2}{3}} (0.001)^{\frac{1}{2}} \Rightarrow \boxed{Q = 118.57 \frac{\text{ft}^3}{\text{s}}}$$

⑥ Purpose: Find drag force a 4-year-old would experience in the lazy river.

Drawings + Diagrams:



$$\begin{aligned}C &= \pi(D) \\C &= \pi(1.15 \text{ ft}) \\C &= 3.613 \\C/2 &= 1.8 \text{ ft}\end{aligned}$$

Sources:

Mott + Untener: Applied Fluid Mechanics 8th edition

Design considerations:

Assume:

- Child is a cylinder
- $D = 1.15 \text{ ft}$
- $T = 80^\circ\text{F}$

Data + Variables:

$$Q = 118.57 \frac{\text{ft}^3}{\text{s}} \quad \rho = 1.93 \frac{\text{slugs}}{\text{ft}^3}$$

$$V = 9.15 \cdot 10^{-6} \frac{\text{ft}^2}{\text{s}}$$

$$A_{LR} = 23.24 \text{ ft}^2 \quad T = 80^\circ\text{F}$$

$$C_D = 2 \cdot 10^{-1} \text{ (from graph 17-4)}$$

$$D = 1.15 \text{ ft} \quad d = 2.8 \text{ ft}$$

Materials:

Water, 4-year-old child

Procedure + Calculations:

• Find v :

$$v = \frac{Q}{A_{LR}} = \frac{118.57 \frac{\text{ft}^3}{\text{s}}}{23.24 \text{ ft}^2} \Rightarrow v = 5.1 \frac{\text{ft}}{\text{s}}$$

• Find N_R

$$N_R = \frac{vD}{\nu} = \frac{(5.1 \frac{\text{ft}}{\text{s}})(1.15 \text{ ft})}{9.15 \cdot 10^{-6} \frac{\text{ft}^2}{\text{s}}} = 6.4 \times 10^5 \Rightarrow \text{Use graph 17-4 to find } C_D$$
$$C_D = 2 \cdot 10^{-1}$$

Find drag force:

$$A_{\text{child}} = d \cdot \frac{C}{2} = 2.8 \text{ ft} \cdot 1.8 \text{ ft} = 5.07 \text{ ft}^2$$

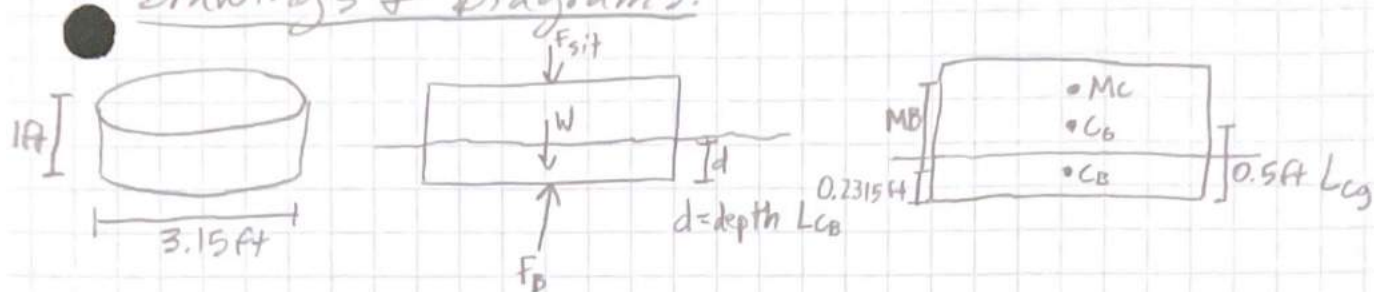
$$F_D = C_D \left(\frac{\rho v^2}{2} \right) A_{\text{child}}$$

$$F_D = (2 \cdot 10^{-1}) \left(\frac{1.93 \frac{\text{slugs}}{\text{ft}^3} \cdot (5.1 \frac{\text{ft}}{\text{s}})^2}{2} \right) (5.07 \text{ ft}^2)$$

$$F_D = 25.45 \text{ lb}$$

⑦ Purpose: If a 220 lb person sits on the tube, how deep does it go? Is it stable?

Drawings & Diagrams:



Sources: Mott & Untener: Applied Fluid Mechanics 8th edition

Design Considerations:

Assume:

- Innertube is hollow short cylinder
- 220 lb is just a force, not considering shape of person

Data & Variables:

$F_{sit} = 220 \text{ lbs}$
 $W = 2 \text{ kg} = 4.41 \text{ lbs}$
 $\gamma_{H_2O} = 62.2 \frac{\text{lb}}{\text{ft}^3}$
 $\gamma_{air} = 0.0736 \frac{\text{lb}}{\text{ft}^3}$
 $\rho_{air} = 2.28 \cdot 10^{-3} \frac{\text{slug}}{\text{ft}^3}$
 $D = 3.15 \text{ ft}$
 $h = 1 \text{ ft}$

Materials:

Water, air

Procedure & Calculations:

• I will add F_{sit} to W to simplify it

$$F = F_{sit} + W = 220 \text{ lb} + 4.41 \text{ lb} = 224.41 \text{ lb}$$

• F must $= F_B$ because it is floating $\therefore F = F_B = 224.41 \text{ lb}$

• I will find displaced Volume:

$$\frac{F_B}{\gamma_{H_2O}} = V_D = \frac{224.41 \text{ lb}}{62.2 \frac{\text{lb}}{\text{ft}^3}} \Rightarrow V_D = 3.61 \text{ ft}^3 = V_{H_2O}$$

• I will use V_{H_2O} to find depth:

$$V_{H_2O} = \frac{\pi}{4} (D^2) \cdot d \Rightarrow 3.61 \text{ ft}^3 = \frac{\pi}{4} (3.15 \text{ ft}^2) \cdot d \Rightarrow \boxed{d = 0.463 \text{ ft}}$$

- I will find the full mass of the tube with the force on it in slugs

$$m = \frac{W}{g} = \frac{224.14 \text{ lb}}{32.2 \frac{\text{ft}}{\text{s}^2}} = 6.96 \text{ slugs}$$

- I place C_B at centroid of displaced volume + C_g at centroid of the volume of the tube

$$MB > L_{cg} - L_{CB}$$

MB must be over C_g to be stable

$$MB > 0.5 \text{ ft} - 0.2315 \text{ ft}$$

$$MB > 0.2685 \text{ ft}$$

MB must be over 0.2685 ft to be stable

- I will find MB

$$MB = \frac{I}{V_d} = \frac{\frac{\pi D^4}{64}}{V_d} = \frac{\frac{\pi (3.15 \text{ ft})^4}{64}}{3.61 \text{ ft}^3} \Rightarrow MB = 1.34 \text{ ft}$$

$$I_{\text{circle}} = \frac{\pi D^4}{64}$$

$$MB = 1.34 \text{ ft}$$

$$1.34 \text{ ft} > 0.2685 \text{ ft} \therefore$$

stable

Part B

Summary:

A lazy river was designed to fit 2 innertubes of a given size and be shallow enough to be safe for a 4-year-old. I made the river 8.3 ft wide to give space for riders' legs and I made it 2.8 ft deep to be up to the neck of a 4-year-old. I found I would need a flow rate of $118.57 \frac{\text{ft}^3}{\text{s}}$. When the 4-year-old stands in the water, it experiences a drag force of 25.45 lb. If a 220 lb individual sat on the tube, it would sink 0.463 ft into the water, but it would be stable.

Analysis:

The inner tube can most likely support a much larger person, or perhaps a person holding their child. However calculations were performed assuming the tube was a cylinder so the real tube may be more or less stable. The gaps at the side are also important because if someone becomes trapped under a bunch of innertubes with people in them, they need to have a space to get to the surface. I have experienced this before in lazy rivers. If the slope was increased the required, the flow rate could be increased without having to use jets as much. The flow rate could also be increased if a smoother surface were used for the pool walls and floor.