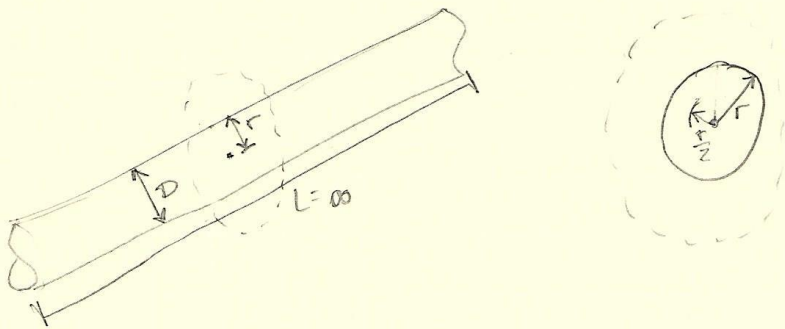


MET 440	Test 3	Carter Fishback	1
1. <u>Purpose</u> To Determine a solution using the infinite body model for Transient Flow in a long rod. The solution must be used to solve for the radius that would result a temperature of 30°C at the center of the rod when time, t, equals 1338s. At that time, also find the temp at the surface and when $r/2$. <u>Drawings</u>  <u>Sources</u> Bayazitoglu, Y. & Ozisik, N., "Textbook for Heat Transfer fundamentals" Begell House Inc., (2012) <u>Design Considerations</u> - Transient Flow through a cylinder body - Long cylinder assumption means infinite L can be assumed - Time dependent - Constant properties <u>Data and variables</u> $T_i = 70^{\circ}\text{C} = 343\text{ K}$ $T_{\text{center}} = 30^{\circ}\text{C} = 303\text{ K}$ $T_{\infty} = 25^{\circ}\text{C} = 298\text{ K}$ $t = 1338\text{ s}$ $r_i = \text{radius of cylinder}$ $r_o = r/2$ $\rho = 1190\text{ kg/m}^3$ $C_p = 1465\text{ J/kg}\cdot\text{K}$ $k = 0.19\text{ W/m}\cdot\text{K}$ $h_{\infty} = 20.42\text{ W/m}^2\cdot\text{K}$			

Carter Fishback

MET 440	Test 3	Carter Fishback	2
<u>Procedure</u> 1. Use radial - Infinite cylinder equation and solve for r 2. Iterate For r value: • Guess r • Find Bi • Interpolate from table 5.1 to get C_1 and J_1 • Plug into equation with guessed r • Compute LHS and RHS • find % difference 3. Use r to find half the radius 4. Use $\theta = \theta_0 J_0\left(\frac{r}{r_0}\right)$ equation to find the temp at the given time and $\frac{r}{2}$ location 5. Repeat step 4 at the surface of the cylinder			

MET 440	Test 3	Carter Fishback	3
Calculations $C(r,t) = \frac{T(r,t) - T_{\infty}}{T_i - T_{\infty}}$ $\theta_0^* = C_1 e^{-\int_1^2 Z}$ $\theta^* = \theta_0^* J_0(\int_1^2 r^*)$ $r^* = \frac{r}{r_0}$ $\tau = \frac{\alpha t}{r_0^2}$ $Bi = \frac{h(\frac{r_0}{2})}{k} \rightarrow Bi < .1 = \text{Lump Capacitance}$ $Bc = \frac{hr_0}{k}$ $\alpha = \frac{k}{\rho C_p}$			
Temp @ center point After $T_{\text{center}} = 293 \text{ K}$ and $t = 1338 \text{ s}$ $\frac{T(r,t) - T_{\infty}}{T_i - T_{\infty}} = C_1 e^{-\int_1^2 Z} \rightarrow \ln\left(\frac{T(r,t) - T_{\infty}}{C_1(T_i - T_{\infty})}\right) = -\int_1^2 \left(\frac{\alpha t}{r_0^2}\right)$ $\frac{T(r,t) - T_{\infty}}{T_i - T_{\infty}} = C_1 \exp\left[-\int_1^2 \left(\frac{k}{\rho C_p}\right) \frac{t}{r_0^2}\right]$ $r = \sqrt{\frac{-\int_1^2 (\alpha t)}{\ln\left[\frac{T(r,t) - T_{\infty}}{T_i - T_{\infty}} \frac{1}{C_1}\right]}}$ * Iteration is used to compare the LHS to the RHS * - r was guessed to find $Bi = \frac{hr_0}{k}$ - Bi used to fix C_1 and $\int_1^2$ - Iterations on excel $\frac{303 \text{ K} - 298 \text{ K}}{343 \text{ K} - 298 \text{ K}} = C_1 e^{-\int_1^2 \left(\frac{0.19 \frac{\text{W}}{\text{m}\cdot\text{K}}}{1190 \frac{\text{kg}}{\text{m}^3} (1165)} (1338 \text{ s})\right) \frac{1}{r^2}}$ $.1111 = C_1 e^{-\int_1^2 \left(\frac{1.46 \times 10^{-4}}{r^2}\right)}$ $\ln\left(\frac{.1111}{C_1}\right) = -\int_1^2 \left(\frac{1.46 \times 10^{-4}}{r^2}\right)$ $\frac{\ln\left(\frac{.1111}{C_1}\right)}{-\int_1^2} = (1.46 \times 10^{-4}) \frac{1}{r^2} \rightarrow r^2 = \frac{(1.46 \times 10^{-4})(-\int_1^2)}{\ln\left(\frac{.1111}{C_1}\right)}$ $r = \sqrt{\frac{(1.46 \times 10^{-4})(-\int_1^2)}{\ln\left(\frac{.1111}{C_1}\right)}}$ - Interpolation was done to calculate the exact C_1 and $\int_1^2$ values from Bi charts. * By Iteration, $r = 0.01 \text{ m} = 10 \text{ mm} @ 0.076\%$ $D = .02 \text{ m} = 20 \text{ mm}$			

Carter Fishback

MET440	Test 3	Carter Fishback	4
<u>Calculations Cont.</u> Temp @ the surface - Bi is same as in Excel Radius solution - ξ_1 is same as Excel Radius solution Equation: $\frac{T(r,t) - T_{\infty}}{T_i - T_{\infty}} = \left(C_1 e^{-\xi_1^2 \tau} \right) J_0 \left(\xi_1 \left(\frac{r_o}{r} \right) \right)$ $Bi = \frac{hr}{k} = \frac{(20.42)(.01)}{.19} = 1.07$ from Excel iterations $C_1 = 1.216$ $\tau = \frac{\alpha t}{r^2} = \frac{(1.09 \times 10^{-7})(1338 s)}{(.01 m)^2} = 1.458$ $\xi_1 = 1.28$ $\frac{T(r,t) - 298}{343 - 298} = \left[(1.216) e^{(-1.28^2 (1.458))} \right] J_0 \left(1.28 \left(\frac{.01}{.01} \right) \right)$ $\frac{T(r,t) - 298}{45} = .1116 \cancel{J_0(1.28)} \xrightarrow{\text{Table B.4}} \xrightarrow{\text{Interpolation}} .6303$ $\frac{T(r,t) - 298}{45} = .1116(.6303)$ $\frac{T(r,t) - 298}{45} = .0703$ $T(r,t) = (.0703)(45) + 298 = 301.16$ $T(\text{surface}) = 301.16 K = 28.014 ^\circ C$			

Carter Fishback

MET 440	Test 3	Carter Fishback	5
Calculations Cont. Temp @ $\frac{r}{2}$ Equation: $\frac{T(r,t) - T_{\infty}}{T_i - T_{\infty}} = \left(C_1 e^{-\beta_1^2 L} \right) J_0 \left(\beta_1 \left(\frac{r_0}{r} \right) \right)$ $C_1 = \text{const}$ $\beta_1 = \text{const}$ $L = 1.458$ $\frac{T(r,t) - 298}{343 - 298} = \left[(1.216 e^{-1.28^2 (1.458)}) \right] J_0 (1.28 \cancel{(.5)})$ ^{Interpolation} $\frac{T(r,t) - 298}{45} = .1116 \cancel{J_0(.64)}^{.8997}$ $T(r,t) = .1004 (45) + 298$ $T\left(\frac{r}{2}\right) = 302.52 \text{ K} = 29.37^\circ\text{C}$			

Carter Fishback

MET440	Test 3	Carter Fishback	6
<u>Summary</u> The radius, r, found to cause the given conditions is $r = 10 \text{ mm}$ or $D = 20 \text{ mm}$. At the time, $t = 1338 \text{ seconds}$, and radius, $r = 10 \text{ mm}$, The temp at $\frac{r}{2}$ is $T_{\frac{r}{2}} = 29.37^\circ\text{C}$ and $T_{\text{surface}} = 28.014^\circ\text{C}$. <u>Materials</u> - Long Plastic rod - Low Convective Fluid <u>Analysis</u> The Fluid that the rod was in had a low convection coefficient and the rod had a low thermal conductivity. These two factors contributed to the slow cooling of the rod. To calculate the radius, a long infinite cylinder was considered. This is because the heat transfer through the end faces can be assumed negligible.			

Carter Fishback

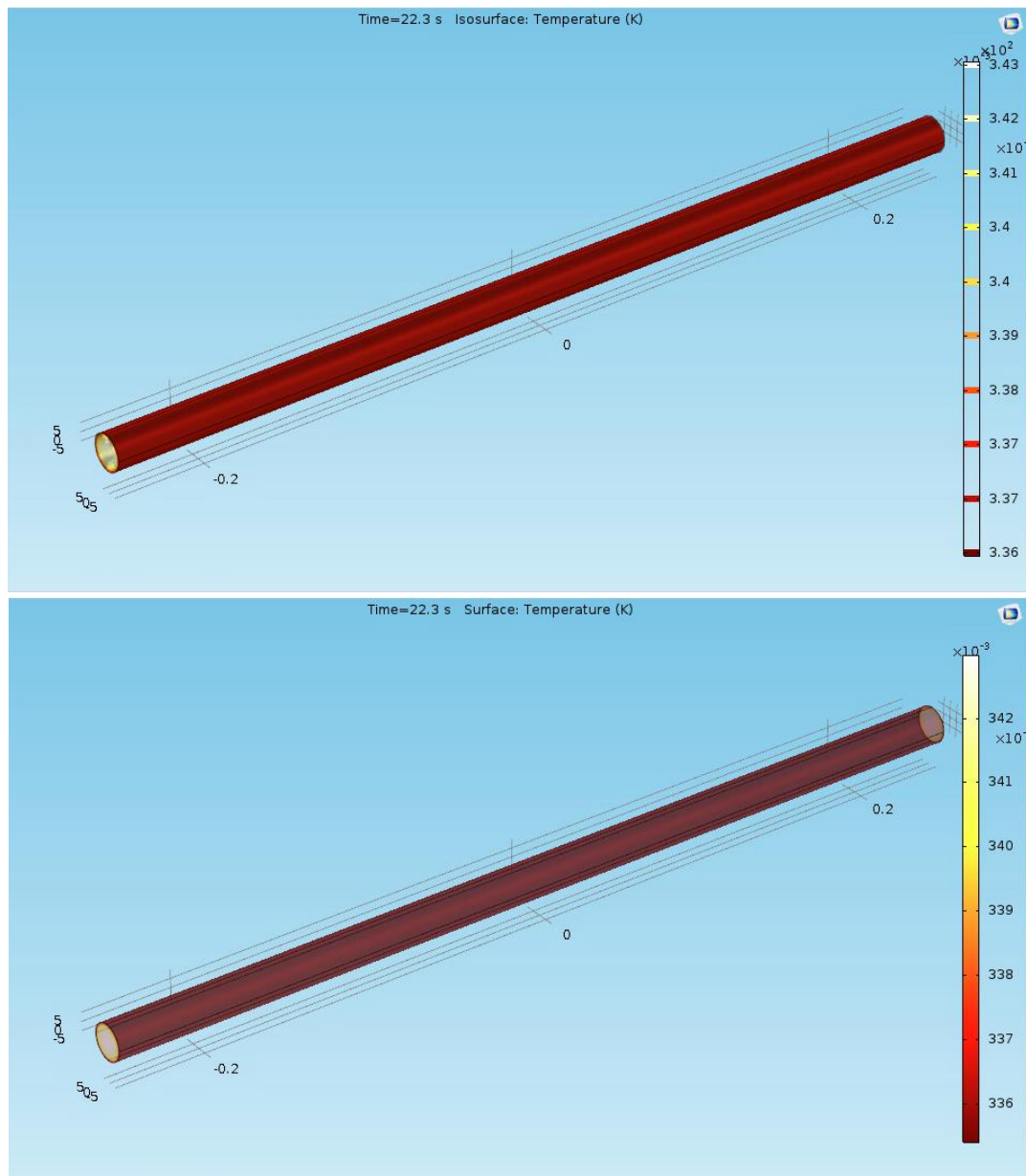
Iteration Process

Constants						Problem 1 Iterations									
Variable		Value	Unit			r (m) guessed	Biot Number	alpha	C1	z1	Theta	LHS	RHS	% Diff	
Initial Temp	Ti	343.15	K			0.025	2.69	1.09E-07	1.39	1.730	0.11	0.02500	0.01314	47.43%	
Center Temp	Tc	303.15	K			0.020	2.15	1.09E-07	1.35	1.628	0.11	0.02000	0.01244	37.81%	
Fluid Temp	Tf	298.15	K			0.010	1.07	1.09E-07	1.216	1.280	0.11	0.01000	0.00999	0.0759%	
Time	t	1338	s			0.009	0.97	1.09E-07	1.202	1.241	0.11	0.00900	0.00971	-7.86%	
Density	Rho	1190	kg/m^3			0.0099	1.06	1.09E-07	1.2150	1.2764	0.11	0.00990	0.00997	-0.67%	
Specific Heat	Cp	1465	J/kg*K			0.00995	1.07	1.09E-07	1.2163	1.2799	0.11	0.00995	0.00999	-0.41%	
Convection Coefficient	hf	20.42	W/m^2*K												
Thermal Conductivity	k	0.19	W/m*K												
C Constant	C1	Based on Tables													
z Constant	z1	Based on Tables													
Radius	r	0.010000	m												
		10	mm												

Test 3: Problem 2

Author

Carter Fishback



Carter Fishback

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1 Purpose

Verify the time that it takes for 3 points along the circles radius to reach a calculated temperature through computational methods. Compute the percent error between the two methods.

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2 Sources

Bayazitoglu, Y. & Ozisik, N., "A Textbook for Heat Transferfundamentals", Begell House Inc., (2012)

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3 Data and Variables

Date	Nov 3, 2019 6:01:43 PM
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3.1 Variables

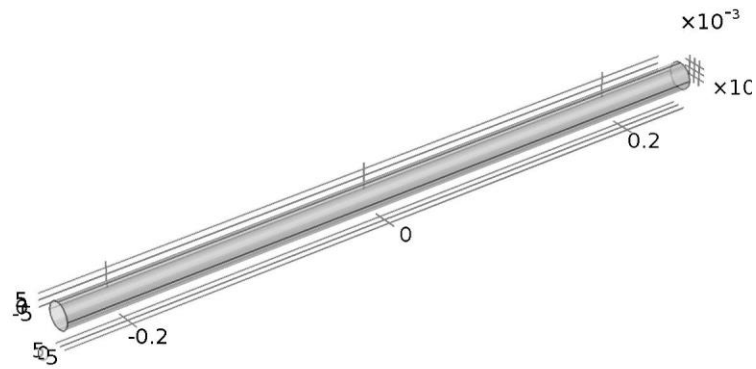
Parameters

Name	Expression	Value	Description
ro	10[mm]	0.01 m	Radius of the Rod
L	1[m]	1 m	Length of the Rod
Ti	343[K]	343 K	Initial Rod Temp
Tf	298[K]	298 K	Ambient Temp
Tc	303[K]	303 K	Temperature at center at t
to	1338[s]	1338 s	Time of interest
tp	25[min]	1500 s	Time range
rho1	1190[kg/m ³]	1190 kg/m ³	Density
Cp1	1465[J/kg/K]	1465 J/(kg·K)	Specific Heat
ko	0.19[W/m/K]	0.19 W/(m·K)	Thermal Conductivity
ho	20.42[W/m ² /K]	20.42 W/(m ² ·K)	Convection Coefficient

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4 Drawings

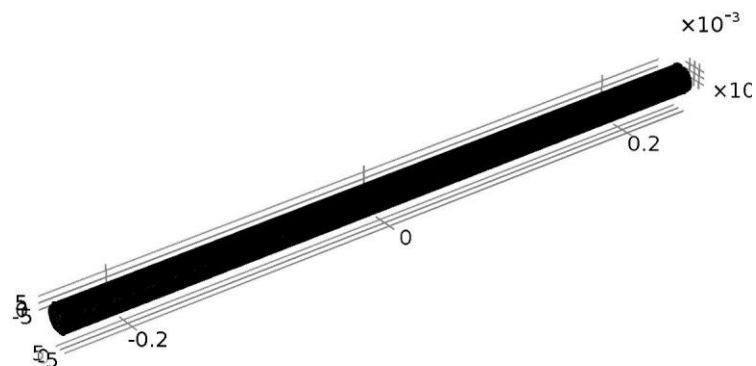
4.1 Geometry 1

*Geometry 1*

Units

Length unit	m
Angular unit	deg

4.2 Mesh 1

*Mesh 1*

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4.3 3D Data Points

4.3.1 Center Point

Data

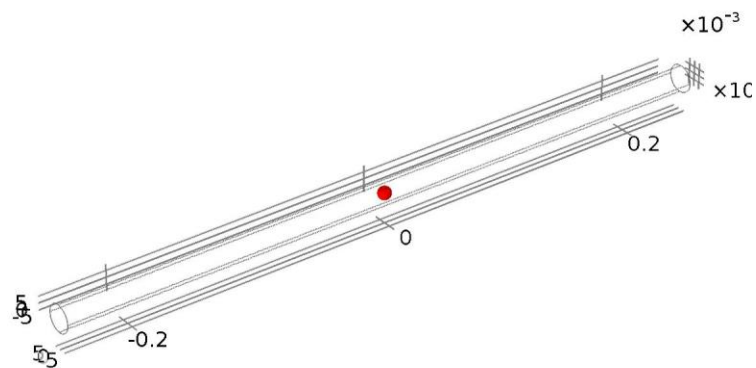
Description	Value
Data set	Study 1/Solution 1

Point data

Description	Value
Entry method	Coordinates

Settings

Description	Value
x	0
y	0
z	0



Data set: Center Point

4.3.2 Half radius

Data

Description	Value
Data set	Study 1/Solution 1

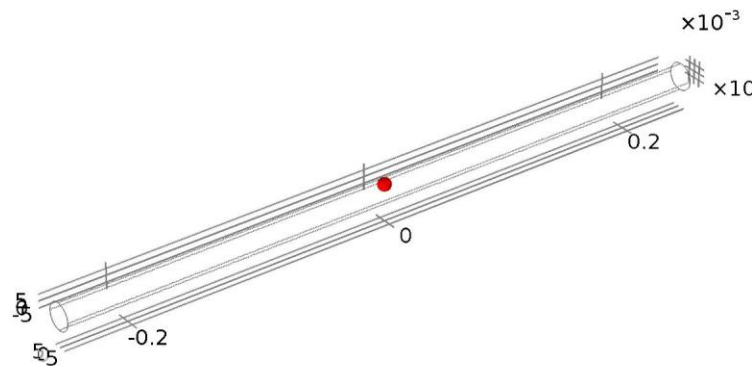
Point data

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Description	Value
Entry method	Coordinates

Settings

Description	Value
x	0
y	0
z	0.005

*Data set: Half radius***4.3.3 Surface****Data**

Description	Value
Data set	Study 1/Solution 1

Point data

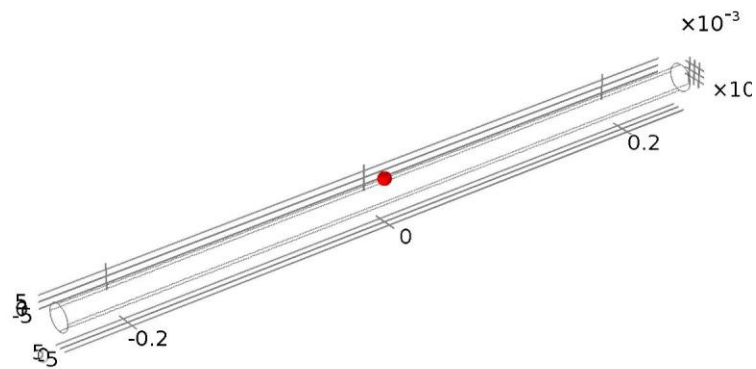
Description	Value
Entry method	Coordinates

Settings

Description	Value
x	0

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Description	Value
y	0
z	0.01

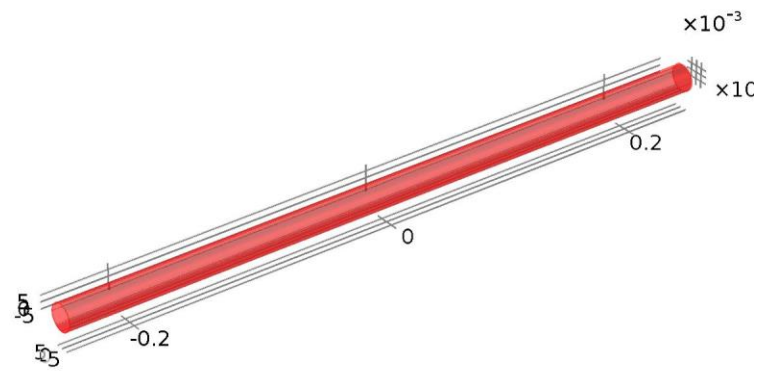
*Data set: Surface*

4.3.4 Study 1/Solution 1

Solution

Description	Value
Solution	Solution 1
Component	Save Point Geometry 1

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Data set: Study 1/Solution 1

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5 Design Considerations

Computation information

Computation time	1 min 31 s
CPU	Intel(R) Xeon(R) CPU E5-2680 v4 @ 2.40GHz, 2 cores
Operating system	Windows 8

5.1 Time Dependent

Study settings

Description	Value
Include geometric nonlinearity	Off

Times	Unit
range(0,to/60,to)	s

Physics and variables selection

Physics interface	Discretization
Heat Transfer in Solids (ht)	physics

Mesh selection

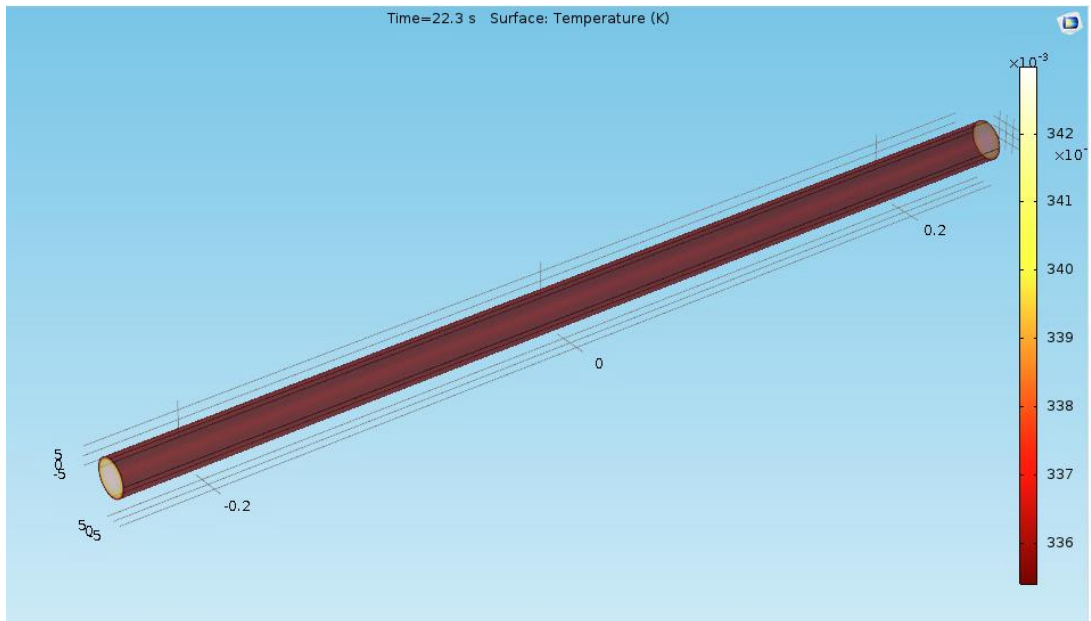
Geometry	Mesh
Geometry 1 (geom1)	mesh1

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6 Results

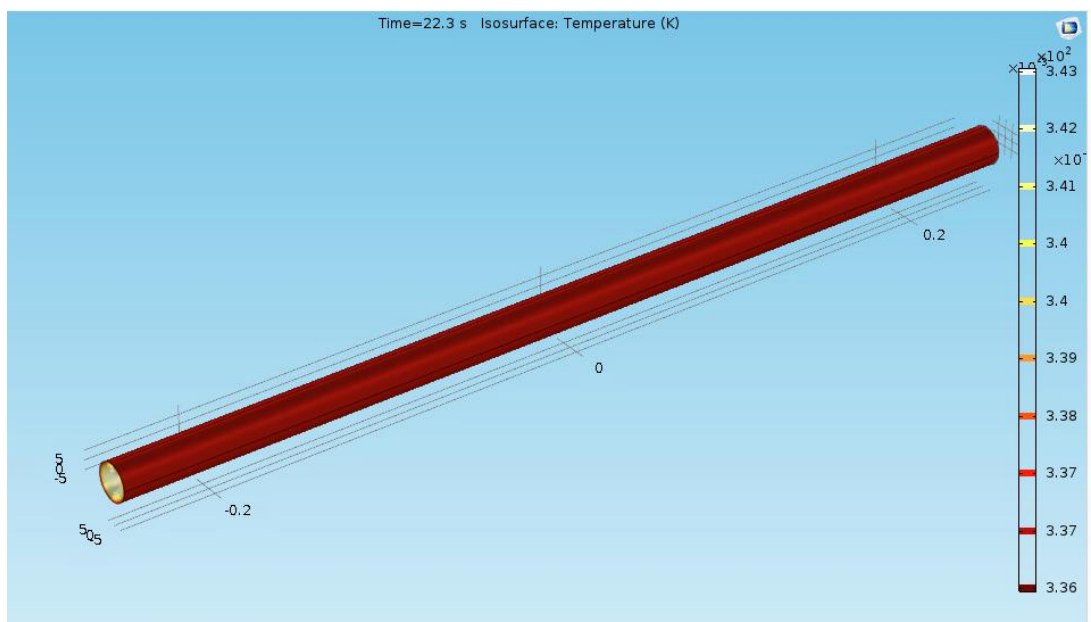
6.1 Summary

6.1.1 Temperature (ht)



Time=1338 s Surface: Temperature (K)

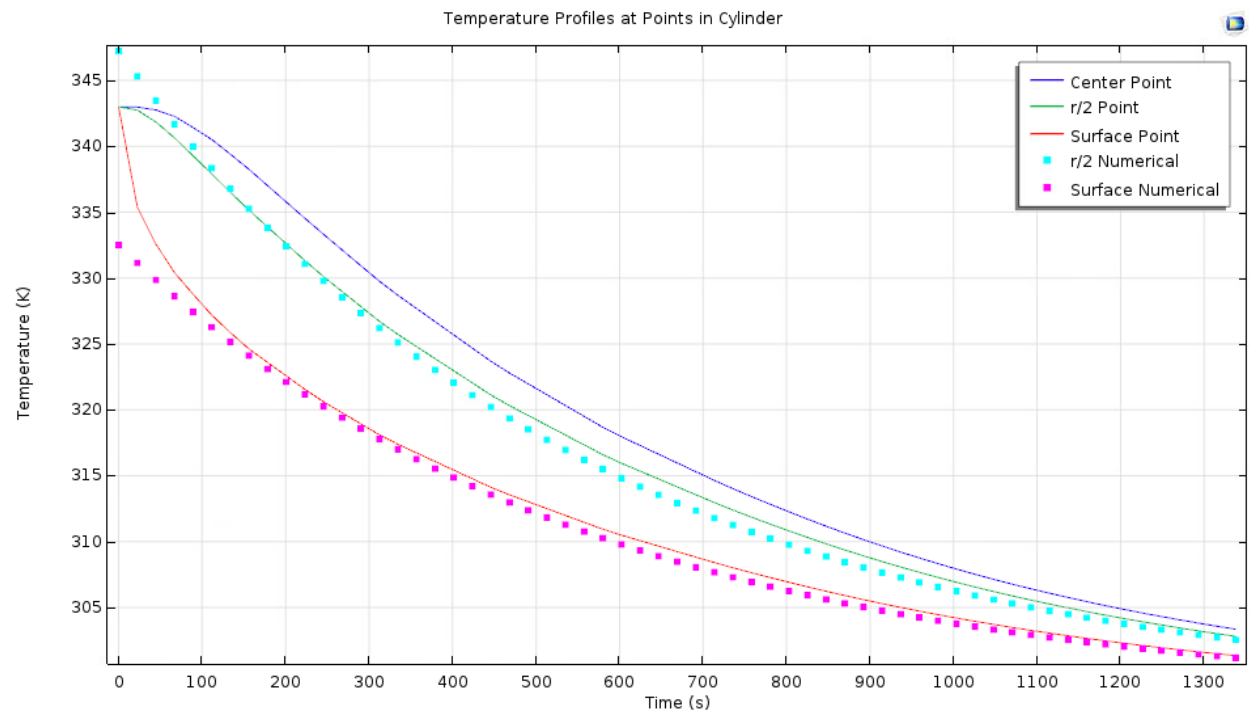
6.1.2 Isothermal Contours (ht)



Time=1338 s Isosurface: Temperature (K)

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6.1.3 1D Plot Group 3



Temperature Profiles at Points in Cylinder

6.2 Analysis

By using COMSOL, we were able to positively verify the calculations done in problem 1. The graph generated from the three points along the radius depicts the change in temperature over time. As calculated, the outside boundary cools off rapidly while the heat transfer slows down as r moves closer to the center. The numerical and analytical comparison proved that there was a small margin of error, however, both show the same trend at each point.