

Discharge coefficient $C = 0.594$

4. $D = 10 \text{ in} = 0.83 \text{ ft}$

$Q = 25 \text{ gal/min} = 0.056 \text{ ft}^3/\text{s}$

Velocity through section

$$V_1 = C \sqrt{\frac{2gh[(y_m/y_A) - 1]}{(A_1/A_2)^2 - 1}}$$

$\frac{25(0.1337)}{60}$

$sg = 0.83$

$\mu = 2.5 \times 10^{-6} \text{ lb-s/ft}^2$

$d_1 = 1.0 \text{ in}$

$d_2 = 7.0 \text{ in}$

deflection of manometer

$$h = \left(\frac{V_1}{C}\right)^2 \frac{(A_1/A_2)^2 - 1}{2g[(y_m/y_A) - 1]}$$

Area of Pipe

$$A_1 = \frac{\pi (0.83)^2}{4} = 0.541 \text{ ft}^2$$

Area of the diameter

$$A_2 = \frac{\pi d^2}{4} = \frac{\pi (0.083)^2}{4} = 5.41 \times 10^{-3} \text{ ft}^2$$

Specific Weight

$\gamma_A = sg \cdot 62.4 \text{ lb/ft}^3$

$\gamma_A = (0.83)(62.4)$
 $= 51.79 \text{ lb/ft}^3$

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Velocity Flow

$V_1 = \frac{Q}{A} = \frac{0.056}{0.541} = 0.1035 \text{ ft/s}$

$V_1 = \frac{\mu}{\rho}$

density of water = 1.94

$\rho = sg \times \text{density of water}$

$0.83 \cdot 1.94$

$\rho = 1.6102 \text{ slugs/ft}^3$

$= \frac{2.5 \times 10^{-6}}{1.6102}$

$V = 1.55 \times 10^{-6} \text{ ft}^2/\text{s}$

Reynolds number

$N_R = \frac{V_1 D}{\nu}$

$\frac{(0.1035)(0.83)}{1.55 \times 10^{-6}}$

$N_R = 5.54 \times 10^4$

$$h = \left(\frac{V_1}{C}\right)^2 \frac{(A_1/A_2)^2 - 1}{2g[(y_m/y_A) - 1]}$$

$$= \left(\frac{0.1035}{0.594}\right)^2 \frac{(0.541/5.41 \times 10^{-3})^2 - 1}{2(32.2)[(62.4/51.79) - 1]}$$

$h = 23 \text{ ft}$

$$h = \left(\frac{0.1035}{0.594}\right)^2 \frac{(0.541/0.264)^2 - 1}{2(32.2)[62.4/51.79 - 1]}$$

$= 0.028 \left(\frac{3.199}{13.193}\right)$

$h = 0.00678 \text{ ft}$

b) Diameter of orifice is $7.0 \text{ in} = 0.58 \text{ ft}$

$A_2 = \frac{\pi d_a^2}{4}$
 $\frac{\pi (0.58)^2}{4}$
 $= 0.264 \text{ ft}^2$

Diameter ratio

$B = \frac{d}{D} = \frac{7.0}{10}$
 $B = 0.7$