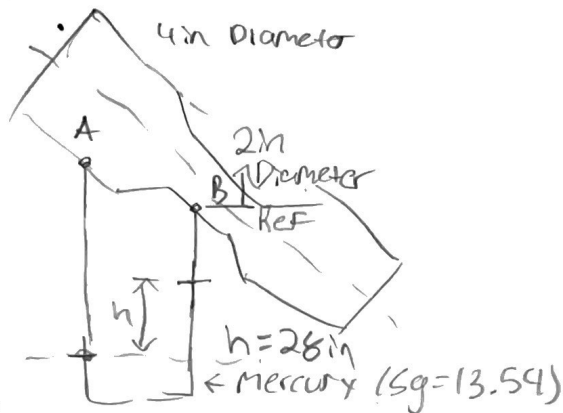


29) FBD



$$A_B V_B = A_A V_A$$

$$\frac{\pi D_B^2}{4} V_B = \frac{\pi D_A^2}{4} V_A$$

$$V_B = \left(\frac{4}{2}\right)^2 V_A$$

$$\gamma_{oil} = S_{g,oil} \times \gamma_{water} = 0.9 \times 62.4$$

$$\gamma_{oil} = 56.16 \text{ lb/ft}^3$$

$$\gamma_{Hg} = S_{g,Hg} \times \gamma_{water}$$

$$= 13.54 \times 62.4$$

$$\gamma_{Hg} = 844.3 \text{ lb/ft}^3$$

Apply Bernoulli's

$$\frac{P_A}{\gamma_o} + \frac{V_A^2}{2g} + z_A = \frac{P_B}{\gamma_o} + \frac{V_B^2}{2g} + z_B \Rightarrow \frac{(P_A - P_B) + \gamma_o(z_A - z_B)}{\gamma_o} = \frac{V_B^2 - V_A^2}{2g}$$

$$(P_A - P_B) = \gamma_o(z_B - z_A - h) + \gamma_{Hg}h$$

$$\frac{(56.16(z_B - z_A) + 1840.38) + 56.16(z_A - z_B)}{56.16} = \frac{(4V_A)^2 - V_A^2}{2g}$$

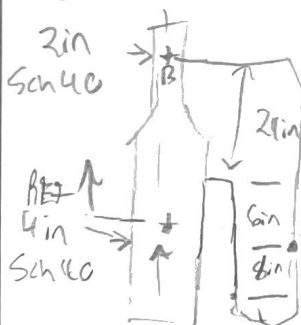
$$\Rightarrow (56.16 + 1840.38) - 56.16 = \frac{1840.38}{56.16} = \frac{15V_A^2}{64.4} \quad V_A = 11.9 \text{ ft/s}$$

Volume Flow rate

$$Q = A \times V = \left(\frac{\pi D_A^2}{4}\right) \times V_A = \frac{\pi (4 \text{ in})^2}{4} \times 11.86$$

$$Q = 1.035 \text{ ft}^3/\text{s}$$

32) FBD



$$\gamma_{oil} = 55.0 \text{ lb/ft}^3$$

$$d_B = 2 \text{ in} = 0.167 \text{ ft}$$

$$d_A = 4 \text{ in} = 0.333 \text{ ft}$$

$$Q = \frac{0.085 \text{ ft}^3/\text{s}}{1.02 \text{ ft}^3/\text{s}}$$

$$Q_1 = \pi/4 d_A^2 V_1 = (0.333)^2 \times 0.085 \text{ ft}^3/\text{s}$$

$$Q_2 = \pi/4 (0.167)^2 \times 0.0219 \text{ ft}^3/\text{s}$$

$$h = d \ln \left( \frac{0.243}{0.05} \right) = \frac{1.08 \text{ in}}{12} = 0.09 \text{ ft}$$

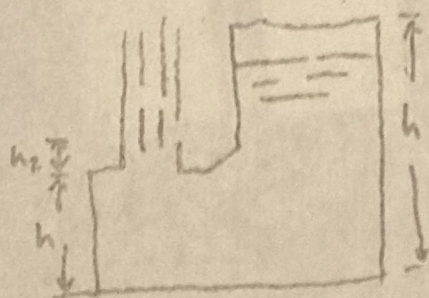
Volume Flow rate

$$Q = \frac{0.085 \times 0.0219 \sqrt{2 \times 32.2 \times 0.09}}{\sqrt{(0.085)^2 - (0.0219)^2}}$$

$$Q = 54.56 \times 10^{-3} \text{ ft}^3/\text{s}$$

Chpt. 6 1091

$h = 2.6 \text{ m}$ ,  $h_1 = .85 \text{ m}$  (elevation of base),  $h_2 = 75 \text{ mm}$  or  $.075 \text{ m}$  (elevation of top)



→ No Energy Loss

$$h_j = h - (h_1 + h_2)$$

$$h_j = 2.6 \text{ m} - (.85 \text{ m} + .075 \text{ m})$$

$$= 2.6 \text{ m} - .925 \text{ m}$$

$$= 1.675 \text{ m}$$