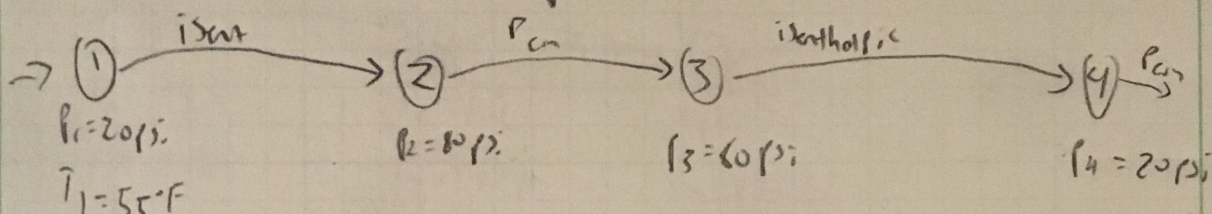
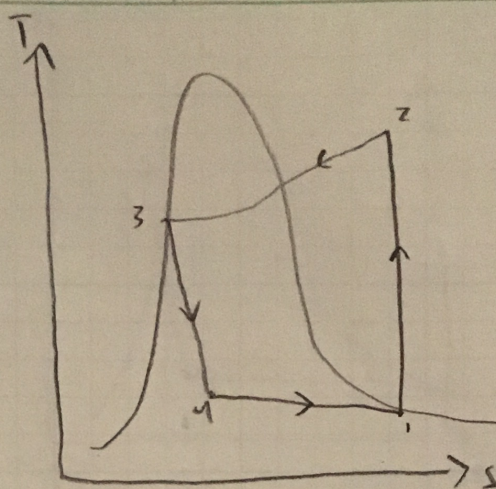
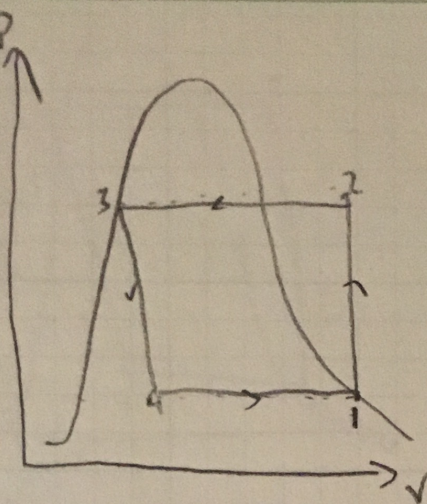


11.11)



Tables

$$h_1 = 102.79 \text{ Btu/lbm}$$

$$h_2 = 115.01 \text{ Btu/lbm}$$

$$h_3 = 33.39 \text{ Btu/lbm}$$

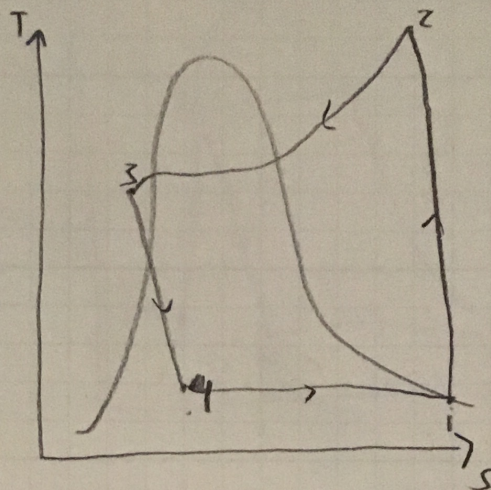
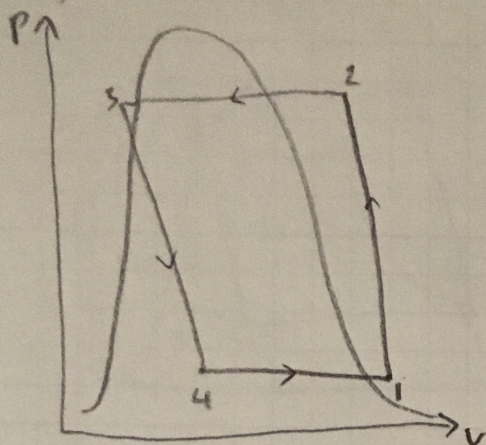
$$h_4 = 33.9 \text{ Btu/lbm}$$

$$Q_L = \dot{m}_{\text{ref}} (\Delta h)_{\text{ref}} = (15/3600 \text{ lbm/s}) (169 \text{ Btu/lbm}) = 7042 \text{ Btu/s}$$

$$\dot{m}_e = \frac{Q_L}{h_1 - h_4} = \frac{7042}{102.79 - 33.39} = 0.1015 \text{ lbm/s}$$

$$\dot{W}_{in} = \dot{m}_e (h_2 - h_1) = (0.1015) (115.01 - 102.79) \left| \frac{1 \text{ hr}}{3600 \text{ s}} \right| = 0.176 \text{ hp}$$

11.17)



$$\begin{array}{cccc}
 \textcircled{1} & \longrightarrow & \textcircled{2} & \longrightarrow & \textcircled{3} & \longrightarrow & \textcircled{4} \\
 T_1 = -5^\circ\text{C} & & T_2 = 70^\circ\text{C} & & T_3 = 49^\circ\text{C} & & T_4 = -21^\circ\text{C} \\
 P_1 = 1.21 \text{ bar} & & P_2 = 1.21 \text{ bar} & & P_3 = 1.15 \text{ bar} & & P_4 = 1.15 \text{ bar}
 \end{array}$$

Superheated tables

$$h_1 = 248.795 \text{ kJ/kg} \quad h_2 = 300.61 \text{ kJ/kg} \quad h_3 = 114.30 \text{ kJ/kg} \quad h_4 = 114.30 \text{ kJ/kg}$$

$$s_1 = 0.9537 \text{ kJ/kg}\cdot\text{K} \quad s_2 = 0.9537 \text{ kJ/kg}\cdot\text{K}$$

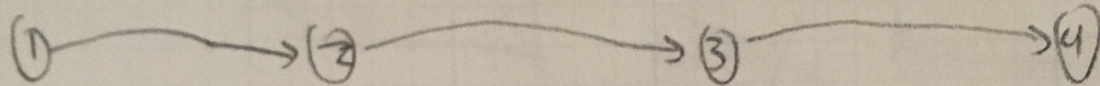
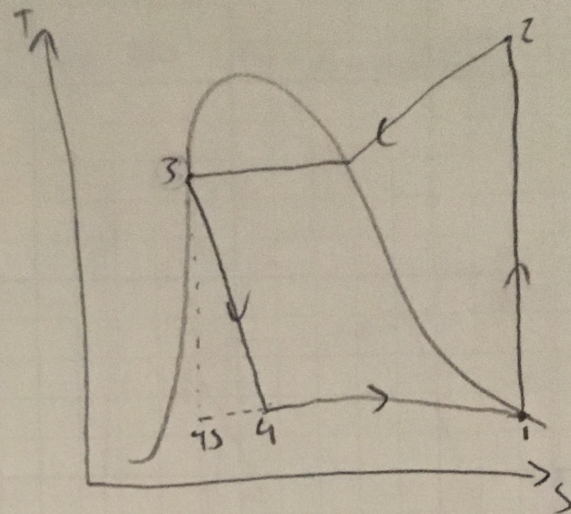
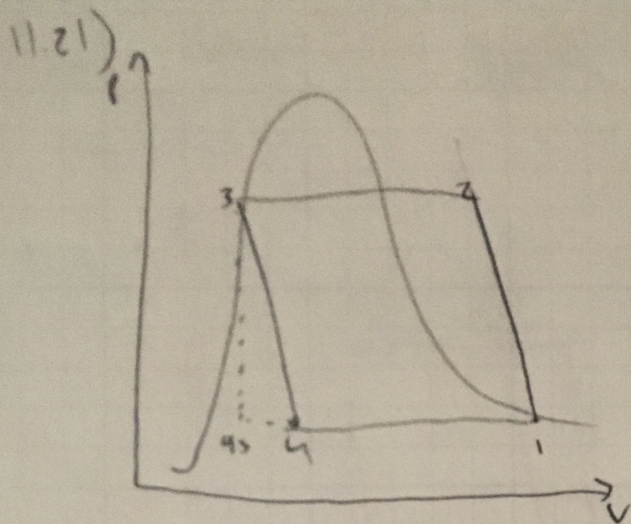
$$a) \dot{Q}_c = \dot{m} Q_c = \dot{m} (h_1 - h_4)$$

$$= 0.07 (248.795 - 114.30) = 9.4161 \text{ kW}$$

$$\dot{W}_{in} = \dot{m} (h_2 - h_1) = 0.07 (300.61 - 248.795) = 3.6271 \text{ kW}$$

$$b) \eta = \frac{h_2 - h_1}{h_2 - h_1} = \frac{287.162 - 248.795}{300.61 - 248.795} = 0.7409$$

$$c) \text{COP} = \frac{Q_c}{W_{in}} = \frac{Q_c}{W_{in}} = \frac{9.4161}{3.6271} = 2.596$$



$$P_1 = 120 \text{ kPa}$$

$$x_1 = 1$$

$$P_2 = 799 \text{ kPa}$$

$$T_2 = 702$$

$$P_3 = 799 \text{ kPa}$$

$$x_3 = 0$$

$$P_4 = 120 \text{ kPa}$$

$$x_4 = 0.34$$

Saturated table

$$h_1 = 236.44 \text{ kJ/kg}$$

$$h_2 = 306.92 \text{ kJ/kg}$$

$$h_3 = 95.41 \text{ kJ/kg}$$

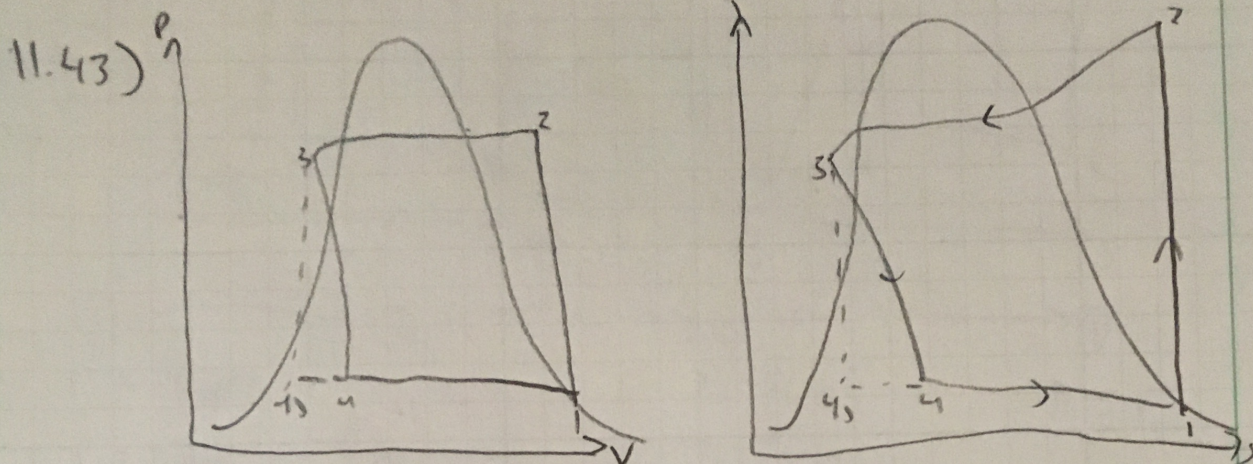
$$h_4 = 95.94 \text{ kJ/kg}$$

$$a) \dot{m} = \frac{\dot{w}_{in}}{h_2 - h_1} = \frac{.45 \text{ kW}}{306.92 - 236.44} = .006435 \text{ kg/s}$$

$$b) \dot{Q}_c = \dot{m}(h_1 - h_4) = (.006435 \text{ kg/s})(236.44 - 95.94) = .911 \text{ kW}$$

$$c) \text{COP} = \frac{\dot{Q}_c}{\dot{w}_{in}} = \frac{.911 \text{ kW}}{.45 \text{ kW}} = 2.03$$

11.36) Condenser Pressure between .133 MPa — .866 MPa for condensing refrigerant.



① → ② → ③ → ④

$P_1 = 572.1 \text{ kPa}$
 $x_1 = 1$
 $h_1 = 261.64 \text{ kJ/kg}$
 $s_1 = 922.5 \text{ kJ/kgK}$
 $h_{w1} = 209.34 \text{ kJ/kg}$

$P_2 = 1400 \text{ kPa}$
 $h_2 = 280.05 \text{ kJ/kg}$
 $h_{w2} = 167.53 \text{ kJ/kg}$

$P_3 = 1400 \text{ kPa}$
 $h_3 = 121.25 \text{ kJ/kg}$

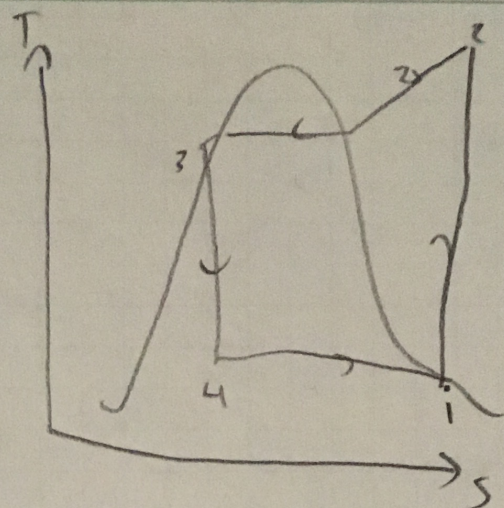
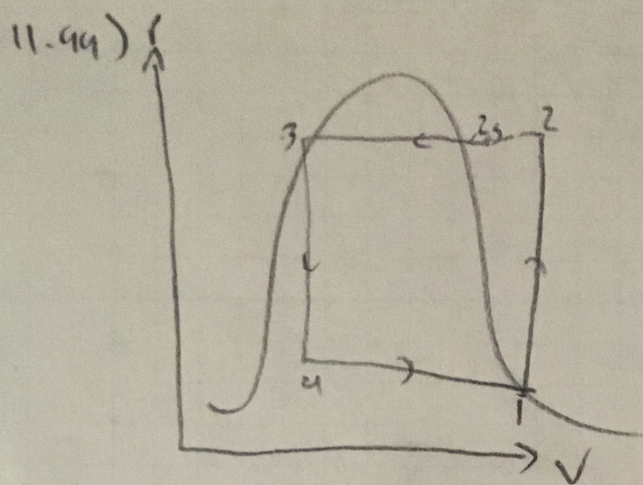
$P_4 = 572.1 \text{ kPa}$
 $x_4 = .23$
 $h_4 = 121.25 \text{ kJ/kg}$

a) $\Delta T_{\text{sub}} = T_{\text{sat}} - T_3 = 52.40^\circ\text{C} - 46.50^\circ\text{C} = 3.02^\circ\text{C}$

b) $\dot{Q}_L = \dot{m}_w (h_{w1} - h_{w2}) = (.065 \text{ kg/s}) (209.34 - 167.53) = 2.716 \text{ kW}$

c) $\text{COP} = \frac{q_L}{w_{in}}$

d) =



(1) → (2) → (3) → (4)

$T_1 = -6.06^\circ\text{C}$	$T_2 = 55^\circ\text{C}$	$T_3 = 26.09^\circ\text{C}$	$T_4 = T_1$
$P_1 = 200\text{ kPa}$	$P_2 = 800\text{ kPa}$	$P_3 = 750\text{ kPa}$	

Tables

$h_1 = 247.88\text{ kJ/kg}$	$h_2 = 286.71\text{ kJ/kg}$	$h_3 = 67.93$	$h_4 = h_3$
	$h_{2s} = 277.28$		

a)
$$h_c = \frac{h_{2s} - h_1}{h_2 - h_1} = \frac{277.28 - 247.88}{286.71 - 247.88} = 0.757$$

b)
$$\dot{Q}_{in} = \dot{m}(h_2 - h_3) = (0.522\text{ kg/s})(286.71 - 67.93) = 117.3\text{ kW}$$

c)
$$W_{in}$$