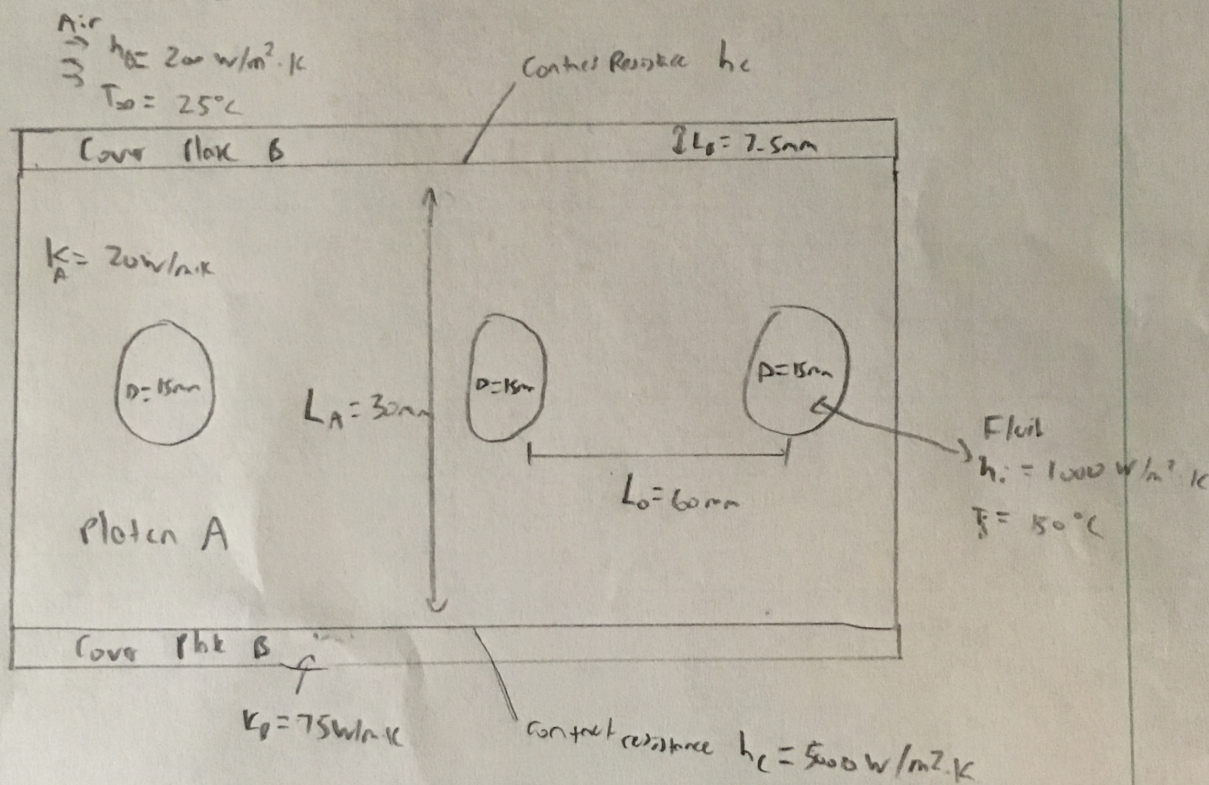


- ① Purpose - To determine
- Total heat rate from a single channel per unit length
 - Temperature T_s
 - If the center-line spacing L_0 is doubled, what would be the new total heat rate and temperature T_s
 - If we insulate the lower surface, the total heat rate would reduce in half? would temperature T_s increase or decrease?
 - If we attach one rectangular fin per channel on each cover plate, what would be the new heat rate.
 - Thermal circuits for both cases without the fins and with the fins

Drawings and Diagrams



* because interface conductance (h_c) is inversely proportional to contact resistance (R_{contact}) we can solve.

$$(500 \text{ W/m}^2\cdot\text{K})^{-1} = R_{\text{con}} = .0002 \text{ m}^2\cdot\text{K/W}$$

Sources

- Bergman, Inghis, Ozisik, N. "A textbook for heat Transfer Fundamentals". 6th ed. Harper & Row, Inc (1998)

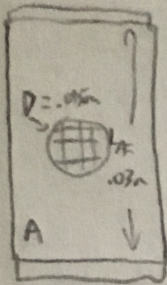
Design Consideration

- Steady state
- Constant properties
- 1D heat transfer
- No heat generation
- Multidimensional heat transfer
- Shape factor
- Fins for part c

Given and variables - See diagram and drawings.

Procedure and Calculations :-)

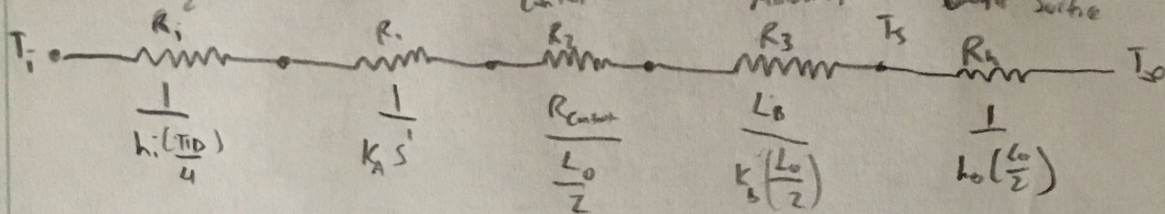
- First we need to find the shape factor for the figure and simplify the geometry.
- Because its symmetrical lets focus on only one circular channel.



(use 2. Shape factor table. $S = \frac{2\pi L}{\cosh^{-1}(D/D)}$ assume 1m for length

$$S = \frac{2\pi \cdot 1m}{\cosh^{-1}(2 \cdot 0.05m / 0.05m)} \quad S = 4.77$$

- Calculate total resistance in the section by getting each individual resistance



$$R_{total} = R_1 + R_2 + R_3 + R_4$$

$$R_1 = \frac{1}{h \cdot \left(\frac{\pi \cdot D}{4}\right)} = \frac{1}{1000 W/m^2 \cdot K \cdot \left(\frac{\pi \cdot 0.05m}{4}\right)} = 0.084 m \cdot K/W$$

$$R_2 = \frac{1}{kA \cdot S'} = \frac{1}{(200 W/m \cdot K) \cdot (1.19)} = 0.0420 m \cdot K/W$$

$S' = \text{for } \frac{1}{4} \text{ section. } S = \frac{4.77}{4} \quad S' = 1.19$

$$R_3 = \frac{R_{con}}{\frac{L_0}{Z}} = \frac{0.002 m^2 \cdot K/W}{\frac{0.06m}{2}} = 0.00666 m \cdot K/W$$

$$R_4 = \frac{L_6}{k_b \left(\frac{L_0}{2}\right)} = \frac{0.0075m}{(75 W/m \cdot K) \cdot \left(\frac{0.06m}{2}\right)} = 0.00333 m \cdot K/W$$

$$R_h = \frac{1}{h_0 \left(\frac{L_0}{2}\right)} = \frac{1}{(200 W/m^2 \cdot K) \cdot \left(\frac{0.06m}{2}\right)} = 0.1666 m \cdot K/W$$

$$R_{total} = 0.084 + 0.0420 + 0.00666 + 0.00333 + 0.1666$$

$$R_{total} = 0.3026 m \cdot K/W$$

• And transfer (q_i) for a single channel from the quarter section.

$$q_i = 4 \frac{T_i - T_\infty}{R_{tot}} = 4 \frac{150^\circ\text{C} - 25^\circ\text{C}}{3028 \text{ m}^2/\text{W}} \quad (q_i = 1652) \text{ W or } 1.652 \text{ kW}$$

• Procedure and calculations for b)

From thermal circuit in part a, we can find T_s by rearranging the equation:

$$T_s = T_\infty + \frac{q_i}{2L_0 h_0} = 25^\circ\text{C} + \frac{1652 \text{ W}}{2(0.6)(200 \text{ W/m}^2\cdot\text{K})}$$

$$T_s = 93.8^\circ\text{C}$$

material for a and b

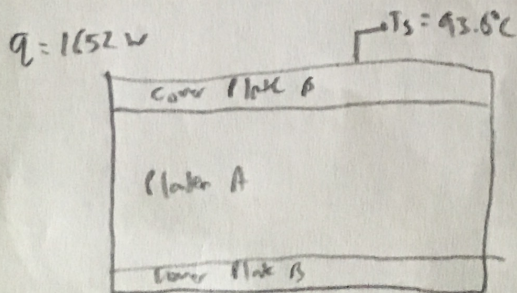
- material A - Plate
- material B - Cover plate
- fluid air
- fluid

Summary for a and b

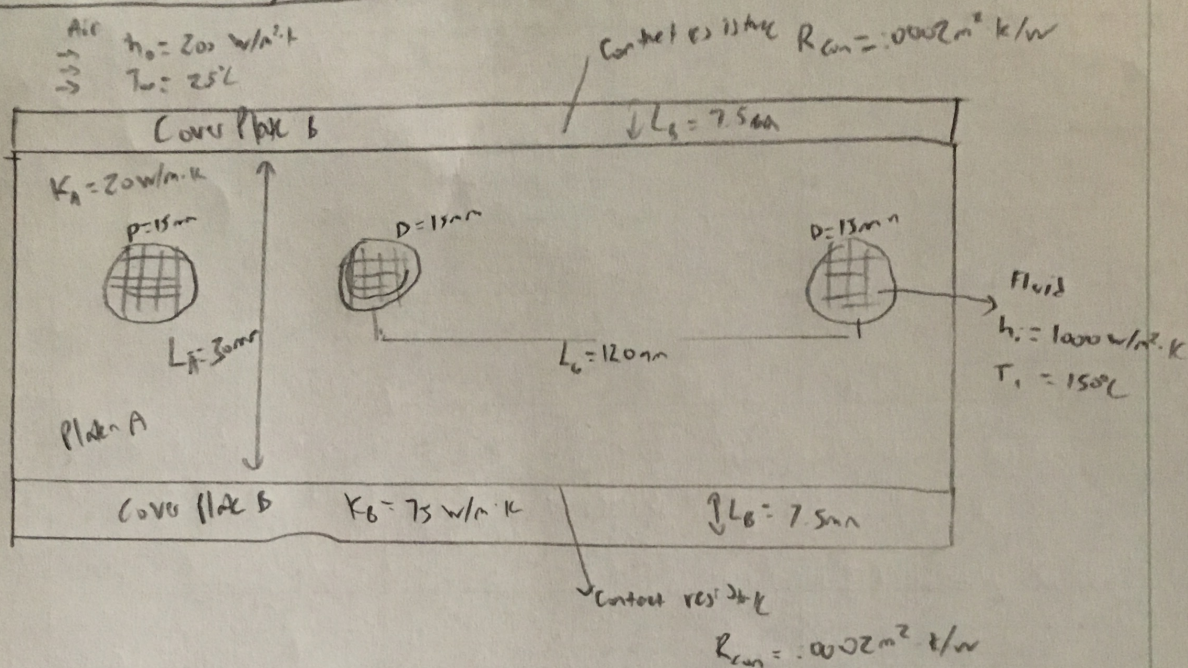
The heat transfer rate from a single channel per unit length is 1652 W and the surface temperature is 93.8°C

Analysis for a and b

The poor contact of plates A and cover plates B, should be resolved for the system to perform better. Here is a figure with the found surface temp and heat transfer rate.



Drawings and diagrams for part c)



Procedure and calculations

- Thermal circuit and shape factor is the same since we are using a quarter section of the figure.

$$R_{total} = R_i + R_1 + R_2 + R_3 + R_h$$

$$R_i = \frac{1}{h_i \left(\frac{\pi D}{4} \right)} = \frac{1}{1000 \text{ W/m}^2\cdot\text{K} \left(\frac{\pi \cdot 0.015 \text{ m}}{4} \right)} = .084 \text{ mK/W}$$

$$R_1 = \frac{1}{K_A S'} = \frac{1}{(20 \text{ W/m}\cdot\text{K}) (1.19)} = .0420 \text{ mK/W}$$

$$R_2 = \frac{R_{con}}{\frac{L_C}{2}} = \frac{.0002 \text{ m}^2 \cdot \text{K/W}}{\frac{.12 \text{ m}}{2}} = .00333 \text{ mK/W}$$

$$R_3 = \frac{L_B}{K_B \left(\frac{L_C}{2} \right)} = \frac{.0075 \text{ m}}{(75 \text{ W/m}\cdot\text{K}) \left(\frac{.12 \text{ m}}{2} \right)} = .001666 \text{ mK/W}$$

$$R_h = \frac{1}{h_i \left(\frac{L_C}{2} \right)} = \frac{1}{(200 \text{ W/m}^2\cdot\text{K}) \left(\frac{.12 \text{ m}}{2} \right)} = .08333 \text{ mK/W}$$

$$R_{total} = .084 + .0420 + .00333 + .001666 + .08333$$

$$R_{total} = .2143 \text{ mK/W}$$

$$q_i = 4 \frac{T_i - T_{\infty}}{R_{tot}} = 4 \frac{15^\circ\text{C} - 25^\circ\text{C}}{0.2143 \text{ m}^2/\text{W}} \quad q_i = 2333.2 \text{ W or } 2.333 \text{ kW}$$

$$T_s = T_{\infty} + \frac{q_i}{2L_h} = 25^\circ\text{C} + \frac{2333.2 \text{ W}}{2(0.12 \text{ m})(200 \text{ W/m}^2\text{K})}$$

$$T_s = 73.6^\circ\text{C}$$

Materials

- material A - flaten
- material B - cover plate
- cool air
- hot fluid

Summary

The difference when doubling the center line space versus the original in part a.

L_0 at 60 mm	L_0 at 120 mm
$q = 1652 \text{ W}$	2333 W
$T_s = 93.8^\circ\text{C}$	73.6°C

Analysis

Resistance is inversely related to the center line spacing that's why the heat rate increased. The surface temperature decreased slightly when center line spacing is doubled. As we can see heat rate increases when center line space is increased.

Procedure and calculations d)

No need to run calculations, explanation in Summary and analysis

Materials

- material A - flask
- material B - cover plate
- cool air
- hot fluid

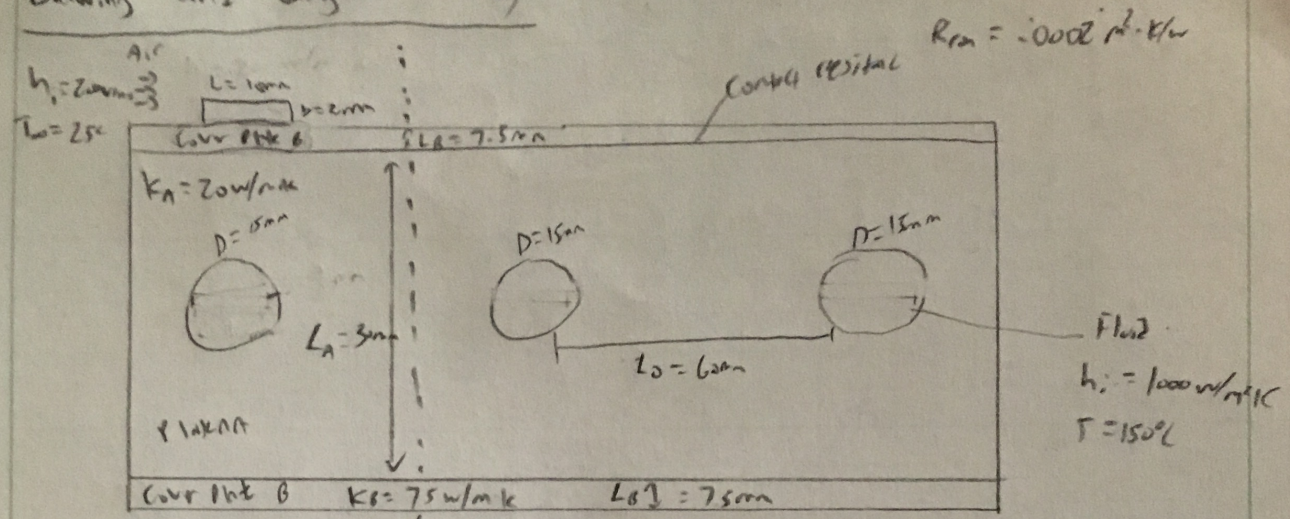
Summary

If we insulate the lower surface the heat rate would reduce in half. Because surface convection is larger than resistance. The temperature T_s would increase because of effect on T_o and the insulated lower surface.

Analysis

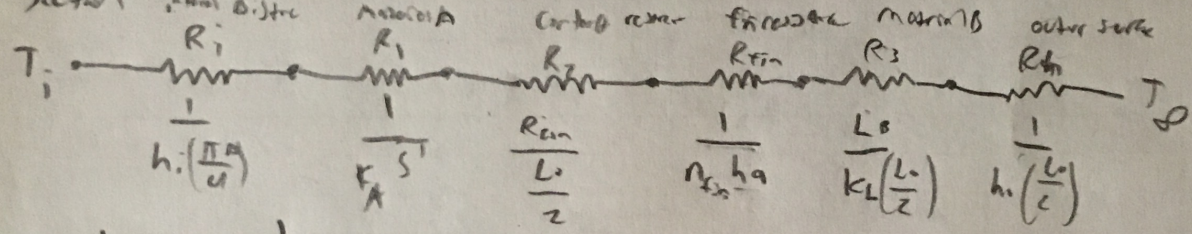
Insulating the lower surface leads to a higher surface temperature. Seems as it is already in poor contact with cover plates B and flask A, we need another solution other than insulating the lower surface. Maybe look at new material for A and B.

Drawing and Jagan for e)



Procedure and calculations:

- Thermal circuit with the fin, we are also examining from a quarter section



$$R_i = \frac{1}{h_1 \left(\frac{\pi \cdot D}{4} \right)} = \frac{1}{(20 \text{ W/m}^2\text{K}) \left(\frac{\pi \cdot 0.015 \text{ m}}{4} \right)} = 0.084 \text{ mK/W}$$

$$R_1 = \frac{1}{K_A s_1} = \frac{1}{20 \text{ W/mK} (1.4)} = 0.0420 \text{ mK/W}$$

$$R_2 = \frac{R_{con}}{\frac{L_0}{2}} = \frac{0.002 \text{ m}^2 \cdot \text{K/W}}{\frac{0.06 \text{ m}}{2}} = 0.00666 \text{ mK/W}$$

$$R_{fin} = \frac{1}{n_f h_a} = \frac{1}{1 \cdot (200 \text{ W/m}^2\text{K}) (0.01 \text{ m} \cdot 0.02 \text{ m})} = 250 \text{ mK/W}$$

$$R_3 = \frac{L_b}{K_L \left(\frac{L_b}{2} \right)} = \frac{0.075 \text{ m}}{(75 \text{ W/m}^2\text{K}) \left(\frac{0.06 \text{ m}}{2} \right)} = 0.00333 \text{ mK/W}$$

$$R_h = 0.084 + 0.0420 + 0.00666 + 250 + 0.00333 \text{ mK/W}$$

$$R_{total} = 250.136 \text{ mK/W}$$

$$Q = \frac{T_1 - T_2}{R_{total}} = \frac{150^\circ\text{C} - 25^\circ\text{C}}{250.136 \text{ mK/W}}$$

$$Q = 1.999 \text{ W}$$

materials

- material A - cover plate
- material B - Platen
- cool air - fluid
- fins

Summary

Here is a table of the heat rates

	L_0 at 6mm	L_0 at 120 mm	with fin
q	1652 W	2333 W	1.999 W

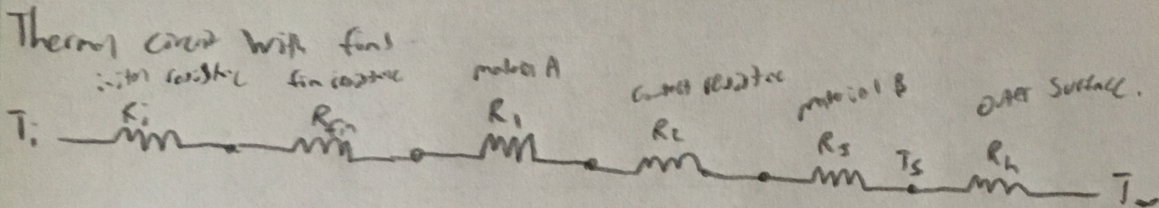
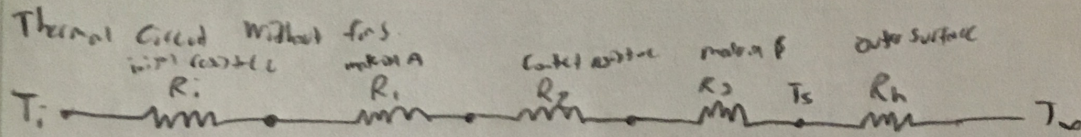
Analysis

The heat rate dropped significantly when attaching the fins.
 This is because extended surfaces removes heat by convection
 and the rate increases.

Drawings and diagrams Part F

refer to drawings and diagrams from part A and C

Procedure and calculations



materials

- material A - fins
- material B - cover plate
- copper - plates
- fluid

Summary

When attaching a fin to the cover plate we need to put the resistance for fin on the thermal circuit.

Analysis

The thermal circuit with the fin has a lower rate of heat transfer than the thermal circuit without the fins. Attaching the fins is a good way to remove the heat.