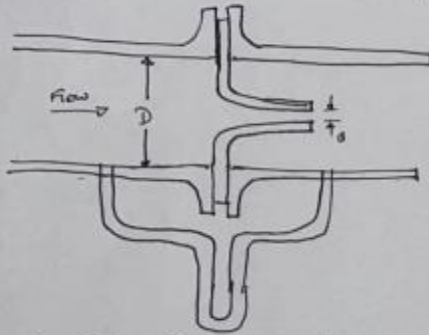


15.9) A flow nozzle is to be installed in a 5-in type K copper tube carrying linseed oil at 77°F. A mercury manometer is used to measure pressure difference across the nozzle when the expected range of flow rate is from 700 $\frac{\text{gal}}{\text{min}}$ to 1000 $\frac{\text{gal}}{\text{min}}$. The manometer scale ranges from 0 to 8 in of mercury. Determine the appropriate diameter of the nozzle.



$$A_1 = \frac{\pi}{4} (0.4004)^2 = 0.12592 \text{ ft}^2$$

$$d = \sqrt{\frac{4A_2}{\pi}} = \sqrt{\frac{4(0.07692 \text{ ft}^2)}{\pi}}$$

$$d = 0.312921$$

USED EXCEL TO FIND OPTIMAL 'd'.
THE CHOSEN/ENTERED WAS ONLY 0.5% OFF
FROM OPTIMAL CALCULATED IN EXCEL, SEE
ATTACHED SPREADSHEET.

GIVEN: $D = 5 \text{ in TYPE K COPPER} \rightarrow D = 0.4004 \text{ ft}$

$$Q = 700 \frac{\text{gal}}{\text{min}} = 1000 \frac{\text{gal}}{\text{min}} \cdot \frac{1 \text{ ft}^3}{7.48 \text{ gal}} \cdot \frac{1 \text{ min}}{60 \text{ s}} = 2.227 \frac{\text{ft}^3}{\text{s}}$$

$$h = 8 \text{ in} \cdot \frac{1 \text{ ft}}{12 \text{ in}} = 0.6667 \text{ ft}$$

$$\gamma_o = 62.4 \frac{\text{lb}}{\text{ft}^3}, \gamma_m = 844.9 \frac{\text{lb}}{\text{ft}^3}$$

$$\nu_m = 844.9 \frac{\text{lb}}{\text{ft}^3}$$

$$\eta = 0.0115 \frac{\text{lb}}{\text{ft} \cdot \text{s}}, \nu = 2.74 \times 10^{-5} \frac{\text{ft}^2}{\text{s}}$$

SOLUTION: $C = 0.9975 - 0.53 \sqrt{\frac{\beta}{Re}}$, USE 0.95 FIRST

$$\beta = \frac{d}{D}, Re = \frac{VD}{\nu}$$

$$Q = CA_1 \sqrt{\frac{2gh[(\gamma_m/\gamma_o)-1]}{(A_1/A_2)^2 - 1}}$$

$$\rightarrow \left(\frac{Q}{CA_1}\right)^2 = \frac{2gh[(\gamma_m/\gamma_o)-1]}{(A_1/A_2)^2 - 1}$$

$$\rightarrow \left(\frac{A_1}{A_2}\right)^2 - 1 = \frac{2gh[(\gamma_m/\gamma_o)-1]}{\left(\frac{Q}{CA_1}\right)^2}$$

$$\rightarrow \frac{A_1}{A_2} = \sqrt{\frac{2gh[(\gamma_m/\gamma_o)-1]}{\left(\frac{Q}{CA_1}\right)^2} + 1}$$

$$\rightarrow A_2 = \frac{A_1}{\sqrt{\frac{2gh[(\gamma_m/\gamma_o)-1]}{\left(\frac{Q}{CA_1}\right)^2} + 1}}$$

$$= \frac{0.12592 \text{ ft}^2}{\sqrt{\frac{2(32.2 \text{ ft/s}^2)(0.6667 \text{ ft})[(844.9 \text{ lb/ft}^3/62.4 \text{ lb/ft}^3)-1]}{\left(\frac{2.227 \text{ ft}^3/\text{s}}{(0.95)(0.12592 \text{ ft}^2)}\right)^2} + 1}}$$

$$A_2 = 0.076906 \text{ ft}^2$$

AutoSave Off Flow Nozzle (Pr. 15.9) - Saved

File Home Insert Draw Page Layout Formulas Data Review View Help

G14 =SQRT(4*F14/PI())

	A	B	C	D	E	F	G	H	I	J	K	L	M
1	Problem 15.9												
2	D=	0.4004 ft											
3	Y_Linseed=	58 lb/ft3											
4	Q=	2.227 ft3/s											
5	h=	0.6667 ft											
6	Y_m=	844.9 lb/ft3											
7	g=	32.2 ft/s2											
8	nu=	0.00038 ft2/s											
9			C	A1(ft2)	A2(ft2)	d(ft)	beta	V(ft/s)	Re	C	%diff		
10			0.95	0.12592	0.07691	0.31292	0.78152	17.6865	18441.9	0.95499	0.52%		
11			0.95499	0.12592	0.07665	0.31241	0.78024	17.6865	18441.9	0.95503	0.00%		
12			0.95503	0.12592	0.07665	0.3124	0.78023	17.6865	18441.9	0.95503	0.00%		
13			0.95503	0.12592	0.07665	0.3124	0.78023	17.6865	18441.9	0.95503	0.00%		
14			0.95503	0.12592	0.07665	0.3124	0.78023	17.6865	18441.9	0.95503	0.00%		
15													
16													
17													
18													

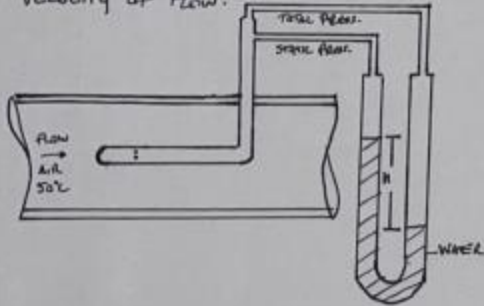
Sheet1

Ready Accessibility: Good to go

57°F Mostly cloudy

9:59 PM 10/23/2022

15.15) A PITOT-STATIC TUBE IS INSERTED INTO A DUCT CARRYING AIR AT STANDARD ATMOSPHERIC PRESSURE AND A TEMPERATURE OF 50°C . A DIFFERENTIAL MANOMETER READS 0.24 in OF WATER. CALCULATE VELOCITY OF FLOW.



GIVEN: $h = 0.24 \text{ in} \cdot \frac{1 \text{ ft}}{12 \text{ in}} = 0.02 \text{ ft}$

$\gamma_g = \gamma_a = 62.4 \frac{\text{lb}}{\text{ft}^3}$

$\gamma_f = 10.71 \frac{\text{lb}}{\text{ft}^3} \cdot \frac{636578 \times 10^{-9} \frac{\text{ft}^3}{\text{ft}^3}}{1.2 \frac{\text{ft}^3}{\text{ft}^3}} = 0.068179 \frac{\text{lb}}{\text{ft}^3}$

SOLUTION: $V_f = \sqrt{2gh(\gamma_g - \gamma_f) / \gamma_f}$
 $= \sqrt{\frac{2(32.2 \frac{\text{ft}}{\text{s}^2})(0.02 \text{ ft})(62.4 \frac{\text{lb}}{\text{ft}^3} - 0.068179 \frac{\text{lb}}{\text{ft}^3})}{(0.068179 \frac{\text{lb}}{\text{ft}^3})}}$

$V_f = 34.32 \frac{\text{ft}}{\text{s}}$