

Curtis Domingues Exam 2 March 22 2020

Problem 1:

> Purpose: a-g

a) Determine depth of given channel if $T = 2.309y$ and slope of channel is 0.1 percent. (use table 14.3)

b) Determine reaction forces acting upon pipe-elbow to obtain proper pipe support.

c) Determine maximum log size in channel. Log is known to have a square-cross section and is barley floating.

Next, determine if the largest possible log will be stable or not.

d) Determine the pressure drop across a nozzle used to measure flow, knowing the ratio of nozzle-pipe diameter is 0.5.

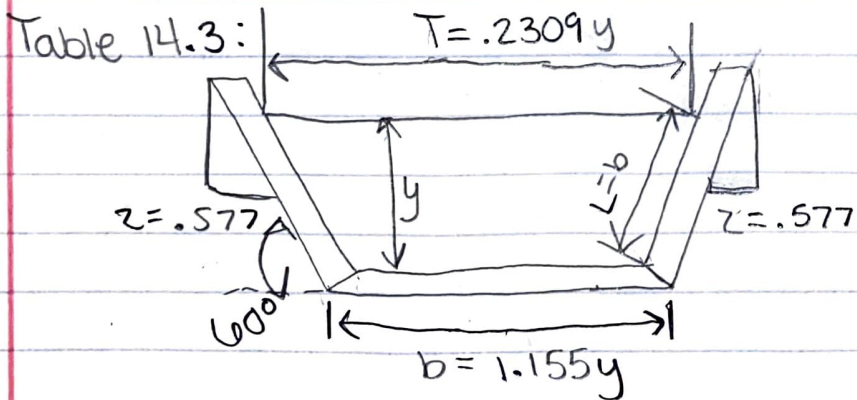
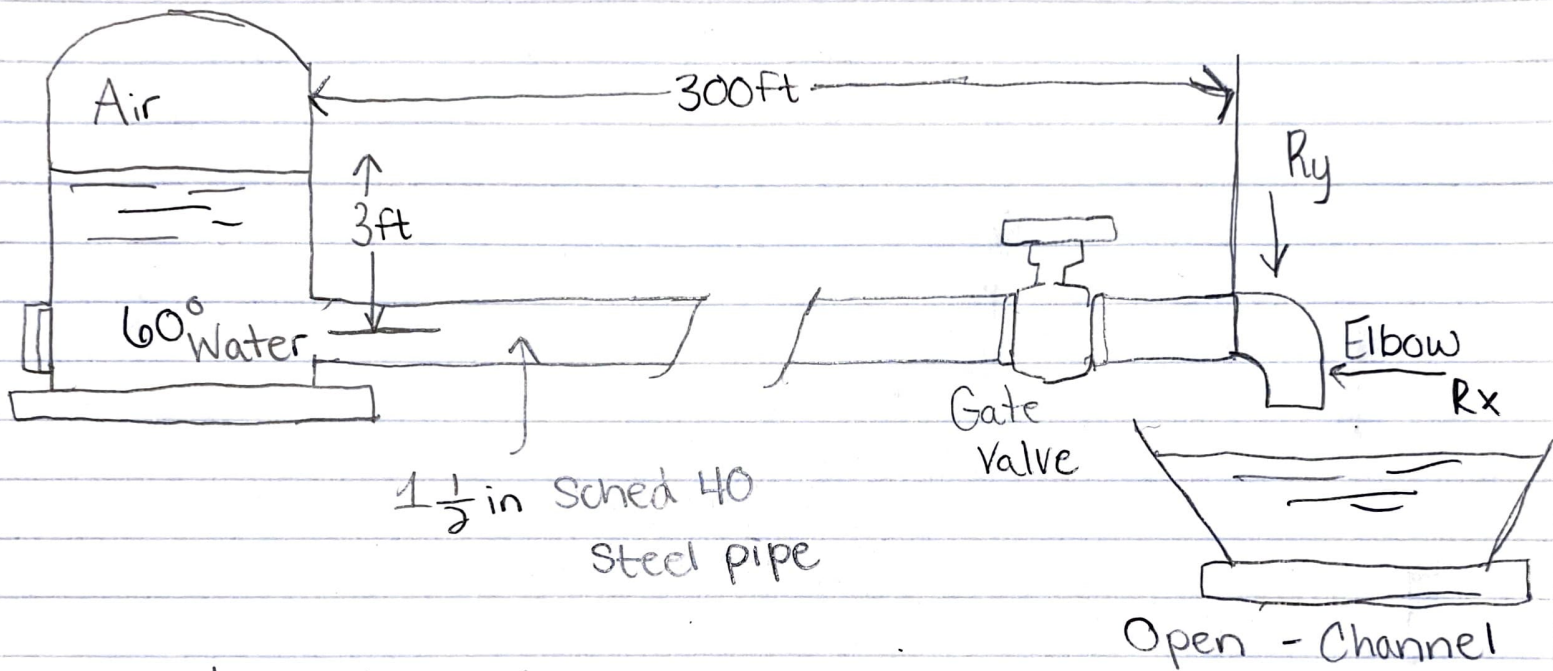
e) Determine the pressure increment produced if the gate valve is closed suddenly.

Next, determine if any change in cavitation occurs in the system.

f) Determine the largest drag force experienced by a log half the size of the "max log" found in part c.

g) Determine the force acting on the blind flange in the tank given it's diameter is equal to pipe diameter.

Diagrams 3 Drawings:



> Sources: "Mott, R., Utener, J.A., "Applied Fluid Mechanics,"
7th Edition.
Pearson Education, INS (2015)

> Design Considerations: a-g

- Constant properties
- Incompressible fluid
- pressurized tank
- Constant Temperature

> Data & Variables: a-g

> For Trapezoidal open channel: (Table 14.3)

$$A = 1.73y^2 \quad W_p = 3.46y \quad R = y/2 \quad R = \frac{A}{W_p}$$

> Given Data:

Water @ 60° $Q = 75 \text{ gpm}$
Pipe $L = 300 \text{ Ft}$ Pipe Size = 1 1/2 in.
 $\rho = 830 \text{ kg/m}^3$
Hickorywood

> Sched 40 steel pipe (Pg. 50)

Flow area = .01414 ft^2

ID = .1342 ft

$E = 200 \text{ GPa}$

$\delta = .0120 \text{ ft}$

Nozzle ratio = .5 "Manning's n " = .017 (Table 14.1)

> Textbook variables:

$f = .02$ (Table 10.5 pg 242)
Kelbow = 20 Ft (Fig 10.24)
 $K_{\text{valve}} = 8 \text{ Ft}$ (Table 10.4)

> Water

$\gamma_{\text{water}} = 62.4 \text{ lb/Ft}^3$

$E_{\text{water}} = 316,000 \text{ psi}$

$V_k = 1.21 \times 10^{-5}$

> Conversions:

$$1 \frac{\text{slug}}{\text{ft}^3} = 1 \frac{\text{lb} \cdot \text{s}^2}{\text{ft}^4}$$

$$1 \text{ psi} = 144 \text{ psf} \quad 1 \text{ lb} \cdot \text{f/s}^2 = .138 \text{ N}$$

$$1 \text{ GPa} = 145038 \text{ psi}$$

> Procedure: a-g

- a) To find the depth of the channel I will use the known Flow rate, slope, and "Manning's n " to solve for the term " $AR^{2/3}$ ".
- Next, I will use the trapezoidal channel from table 14.2 to get all unknown variables in terms of " y ". Then I will rearrange the flow rate equation so that Q is isolated. Lastly, I will assume a depth " y " and compare the results of Q_{calc} and Q_{actual} . I will repeat this process through iteration until Q_{calc} equals the known value of Q . This will determine the true depth of the channel.
- b) For part b I will use Bernoulli's equation to determine the pressure at the entrance of the tank. NOTE: since the elbow is open to the atmosphere, pressure and velocity at the elbow will cancel. Next, I will use the sum of forces equations to determine the forces exerted on the pipe-elbow. Thus, I will solve for R_x and R_y .
- c) To find the largest log the channel can carry, I will use the channel depth found in part a, as well as the given density & cross-section of hickory wood. Furthermore, since the log is known to be "barley floating", I will assume $Weight = F_b$. This will allow me to assume the volume of the log is nearly equal to its volume displaced. Effectively, I will set the volume of the log equal to the volume of water displaced, allowing me to create a ratio between V and V_d . Lastly, I will manipulate volumetric dimensions to solve for the "height" of the log.

c) ... Continued

To determine the stability of the found log, I will use the found channel depth from part a. Since stability is dependent on I & V_d , I will solve for both. I will also use the known channel and log dimensions to solve for y_{CG} and y_{CB} . NOTE: Since V_d requires length to solve, I will assume a length of the log. NOTE: This assumption will not effect result as it will cancel out mathematically. Lastly, I will determine MB and compare it to y_{CG} to verify the stability of the log.

d) To determine the pressure drop across the nozzle I will manipulate the "Nozzle Equation" to solve for Δp . Next, I will determine unknown variable C by solving for N_R (β is given as .5). Once C is known, I will evaluate the equation and solve for the Δp .

e) To determine wave velocity (c) I will use the associated equation. First, I will convert all known variable to common units. NOTE: In order to achieve units of f/s I will convert slugs/ ft^3 to $lb \cdot s^2/ft^4$. Once all units agree I will evaluate and solve for C . Once C is known I will multiply it by density and velocity to determine Δp .

- f) For part f I will assume a log half the size of the max log found in part c. To determine the largest drag force said log will experience, I will use the drag force equation, inputting known variables. Note: C_D is determined from (Table 17.1). Lastly, I will evaluate and solve for F_D .
- g) To determine the force acting on the flange, I will use the h_L determined in part b. Using Bernoulli's Equation I will determine the pressure at the fluid surface in the tank (starting from the elbow since the tank is pressurized). Once, said pressure is known, I will use the " γh " equation to solve for the pressure 3 feet below the surface. Since the flange is circular, I will assume the force location to be distributed about its center.

Calculations Part A:

$$Q = \left(\frac{1.49}{n} \right) A R^{2/3} S^{1/2} \quad Q = 75 \text{ GPM} \cdot \frac{1 \text{ ft}^3/\text{s}}{449 \text{ gpm}} = .167 \text{ ft}^3/\text{s}$$

• Rearrange to solve for $A R^{2/3}$

$$A R^{2/3} = \frac{n Q}{1.49 S^{1/2}} = \frac{.017 (.167 \text{ ft}^3/\text{s})}{1.49 \sqrt{.001}} = \frac{.0028 \text{ ft}^3/\text{s}}{.04711} = .06025 \frac{\text{ft}^3}{\text{s}}$$

Since Q is known, and all variable are in terms of y , assume y value and re-iterate until $Q_{\text{calc}} = Q_{\text{actual}}$

$$\therefore R = \frac{A}{W_p}$$

$$A = 1.73 y^2 \quad W_p = 3.46 y \quad R = \frac{y}{2}$$

$$.167 \frac{\text{ft}^3}{\text{s}} = \left(\frac{1.49}{.017} \right) A R^{2/3} S^{1/2} \quad \text{For } y = .5 \text{ ft:}$$

$$Q = 87.647 \cdot .4325 \text{ ft}^2 \cdot (.39685 \text{ ft}) \cdot (.0316)$$

$$Q = .475 \text{ ft}^3$$

Reiterate: For $y = .25 \text{ ft}$

$$Q = 87.647 \cdot .108125 \text{ ft}^2 \cdot (.25 \text{ ft}) \cdot (.0316)$$

$$Q = .075 \text{ ft}^3$$

Reiterate to find $Q_{\text{calc}} = Q_{\text{act}}$

(see excell Sheet)

After iteration: For $y = .388 \text{ ft}$:

$$Q = 87.647 \cdot .197642 \text{ ft}^2 \cdot (.3056 \text{ ft}) \cdot (.0316)$$

$$Q_{\text{calc}} = .167 \text{ ft}^3 = Q_{\text{actual}} \checkmark$$

Thus, the depth of the channel (y) is .388 ft
or 4.06 in.

ANS

Calculations Part B:

Find horizontal & vertical forces pipe-elbow:

$$F = \frac{P}{A}$$

Bernoullies Equation:

$$\frac{P_1}{\gamma} + z_1 + \frac{V_1^2}{2g} = \frac{P_2}{\gamma} + z_2 + \frac{V_2^2}{2g} + h_L$$

$$\frac{P_1}{\gamma} = h_L \therefore P_1 = h_L \cdot \gamma$$

$$f = .02 \text{ (Table 10.5 pg. 242)}$$

For straight pipe (300ft)

$$h_L = f \times \frac{L}{D} \times \frac{V^2}{2g} = .02 \cdot \frac{300\text{ft}}{.125\text{ft}} \cdot \frac{11.81\text{ft/s}^2}{64.4\text{ft/s}^2} = \underline{103.95\text{ft}}$$

Gate Valve:

$$h_L = f \times 8 \times \frac{V^2}{2g} = (.02)(8) \left(\frac{11.81\text{ft/s}^2}{64.4\text{ft/s}^2} \right) = \underline{.3464\text{ft}}$$

elbow:

$$h_L = f \times 20 \times \frac{V^2}{2g} = (.02)(20) \left(\frac{11.81\text{ft/s}^2}{64.4\text{ft/s}^2} \right) = \underline{.866\text{ft}}$$

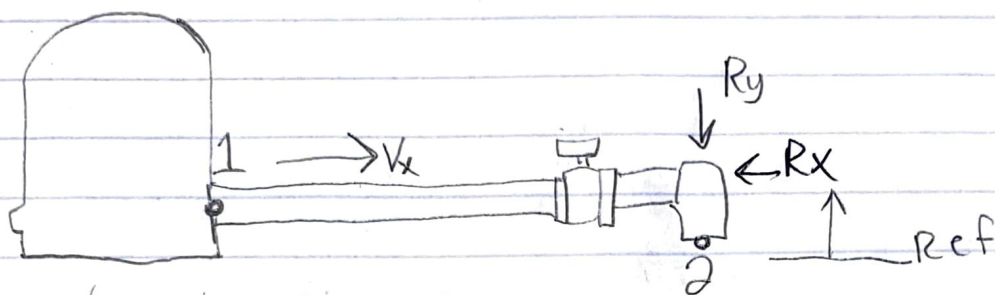
$$F_x = \rho Q \Delta V_x = \rho Q (-V)$$

$$F_y = \rho Q \Delta V_y = \rho Q (-V)$$

> Bernoullies Equation



Calculations Part B continued:



$$\frac{P_1}{\gamma} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\gamma} + \frac{V_2^2}{2g} + h_L \quad \text{Velocities are equal}$$

$$> P_1 = \gamma h_L = \frac{62.4 \text{ lb}}{\text{ft}^3} (105.1624 \text{ ft}) = 6562.13 \text{ lb/ft}^3$$

$$\text{Sum of forces} = \sum F_x = \rho Q \Delta V_x + P_1 + R_x = 0 \quad \Delta V = V_2 - V_1 : V_2 = 0$$

$$\sum F_y = \rho Q \Delta V_y + R_y = 0$$

Force in x-Direction:

$$\sum F_x = \frac{1.94 \text{ slug}}{\text{ft}^3} \left(\frac{.167 \text{ ft}^3}{\text{s}} \right) (-11.81 \text{ ft/s}) + (6562.13 \text{ lb/ft}^3) (.01414 \text{ ft}^2) + R_x$$

$$\sum F_x: \frac{1.94 \text{ slug}}{\text{ft}^3} = \frac{1.94 \text{ lb} \cdot \text{s}^2}{\text{ft}^3} \left(\frac{-1.97 \text{ ft}^4}{\text{s}^2} \right) + (6562.13 \text{ lb/ft}^3) (.01414 \text{ ft}^2) + R_x$$

$$\sum F_x: -3.826 \text{ lb} + 92.78 \text{ lb} + R_x = 0 \quad \boxed{R_x = 88.954 \text{ lb} \leftarrow}$$

ANS

Force in y-Direction:

$$\sum F_y: \frac{1.94 \text{ slug}}{\text{ft}^3} \left(\frac{.167 \text{ ft}^3}{\text{s}} \right) (-11.81 \frac{\text{ft}}{\text{s}}) + R_y = 0$$

$$\frac{1.94 \text{ lb} \cdot \text{s}^2}{\text{ft}^3} \cdot \left(\frac{-1.9706 \text{ ft}^4}{\text{s}^2} \right) = -R_y$$

$$\boxed{R_y = 3.822 \text{ lb} \downarrow}$$

ANS

Part C calculations

Channel depth found to be $.338 \text{ ft} = .103 \text{ m}$

Density of hickorywood = $830 \frac{\text{kg}}{\text{m}^3}$

$$\gamma_{\text{Hickory}} = \frac{830 \text{ kg}}{\text{m}^3} \cdot \frac{9.81 \text{ m}}{\text{s}^2} = 8142.3 \frac{\text{kg} \cdot \text{m}}{\text{m}^3 \text{ s}^2}$$

$$\gamma_{\text{Hickory}} = 8142.3 \text{ N/m}^3 \quad \text{or} \quad 8.14 \text{ kN/m}^3$$

$$\gamma_{\text{water}} = 9.81 \text{ kN/m}^3$$

Since Log is "barley floating" Weight = F_b

> Determine depth of immersion:

$$\text{Weight} = \gamma_{\text{Hickory}} V, \quad F_b = \gamma_{\text{water}} V_d \quad \therefore \gamma_{\text{Hickory}} V = \gamma_{\text{water}} V_d$$

$$\text{Volume} \approx \text{Volume displaced} \quad \frac{\gamma_{\text{Hickory}}}{\gamma_{\text{water}}} = \frac{V_d}{V} \quad \frac{8.14 \text{ kN/m}^3}{9.81 \text{ kN/m}^3} = .829$$

$$\frac{V_d}{V} = .829$$

$$\text{volume} = (L \times W \times h) = (L \times W^2)$$

$$V_d = (L \times W \times y) = (LW y)$$

$$\frac{LW y}{LW^2} = \frac{y}{W} = .829$$

$$\frac{.103 \text{ m}}{W} = .829$$

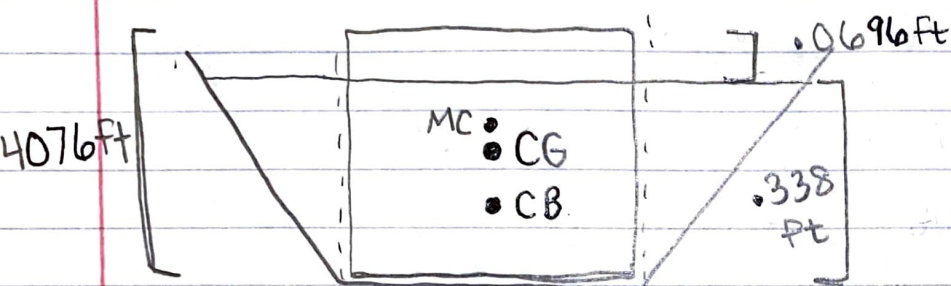
$$.124 \text{ m} \cdot \frac{1 \text{ ft}}{.3048 \text{ m}} = .4076 \text{ ft}$$

$$\frac{.103 \text{ m}}{.829} = W = .124 \text{ m}$$

Therefore, maximum Log size is $.124 \text{ m}$ or $.4076 \text{ ft}$ Ans

> Determine stability

Part C Calculations Continued...



Channel depth = .338 ft
 Max log size = .4076 ft

$$y_{CG} = .2038 \text{ ft}$$

$$y_{CB} = .169 \text{ ft}$$

$$y_{MC} = y_{CB} + MB$$

$$MB = \frac{.0112 \text{ ft}^4}{.2755 \text{ ft}^3}$$

$$MB = .041 \text{ ft}$$

$$y_{MC} = .169 \text{ ft} + .041 \text{ ft}$$

$$y_{MC} = .21 \text{ ft}$$

$$MB = \frac{I}{V_d} \quad V_d = L \times B \times .338$$

* Assume Log length of 2 ft *

$$V_d = 2 \text{ ft} \times .4076 \text{ ft} \times .338 \text{ ft}$$

$$V_d = .2755 \text{ ft}^3$$

$$I = \frac{LB^3}{12} = \frac{2 \text{ ft} \times (.4076 \text{ ft})^3}{12}$$

$$I = .0112 \text{ ft}^4$$

$$.21 \text{ ft} > .2038 \text{ ft}$$

Thus, M_C is slightly higher than Center of gravity.
 ∴ The log is stable

ANS

Calculations part D:

Find pressure drop across nozzle

Nozzle to pipe ratio = .5

Thus nozzle is .75 inch or .0625 ft Diameter

known: $Q = .167 \text{ ft}^3/\text{s}$ $V_k = 1.21 \times 10^{-5}$ $A_1 = .01414 \text{ ft}^2$
 $D = 1.5 \text{ in} = .125 \text{ ft}$ $2g = 64.4 \text{ ft/s}^2$ $A_2 = .003 \text{ ft}^2$
 $D/2 = .75 \text{ in} = .0625 \text{ ft}$ $V_1 = 11.81 \text{ ft/s}$
 $d = .75 \text{ in} = .0625 \text{ ft}$ $\gamma_{\text{water}} = 62.4 \text{ lb/ft}^3$

Nozzle Equation:

$$V_1 = C \sqrt{\frac{2g(\Delta P) / \gamma}{(A_1/A_2)^2 - 1}} \quad \text{- Manipulate to solve for } \Delta P$$

$$\Delta P = \frac{\gamma \left((A_1/A_2)^2 - 1 \right) \left(\frac{V_1}{C} \right)^2}{2g} \quad \text{- solve for unknowns: } C, N_R$$

$$C = .9975 - 6.53 \sqrt{\beta / N_R} \quad \text{when } \beta = d/D = .5$$

$$N_R = \frac{VD}{\nu} = \frac{(11.81 \text{ ft/s})(.125 \text{ ft})}{1.21 \times 10^{-5} \text{ ft}^2/\text{s}} = 122004.1322$$

$$C = .9975 - 6.53 \sqrt{.5 / 122004.1322} = .984$$

$$\Delta P = \frac{62.4 \text{ lb/ft}^3 \left((.01414 \text{ ft}^2 / .003 \text{ ft}^2)^2 - 1 \right) \left(12.00 \text{ ft/s} \right)^2}{64.4 \text{ ft/s}^2}$$

$$= \frac{62.4 \text{ lb/ft}^3 \left(22.215 - 1 \right) \left(144 \text{ ft}^2/\text{s}^2 \right)}{64.4 \text{ ft/s}^2}$$

part D Calculations Continued:

$$\Delta p = \frac{62.4 \text{ lb/ft}^3 (21.215) (144 \text{ ft}^2/\text{s}^2)}{64.4 \text{ ft/s}^2}$$

$$\Delta p = \frac{1323.82 \text{ lb/ft}^3 \cdot 144 \text{ ft}^2/\text{s}^2}{64.4 \text{ ft/s}^2}$$

$$\frac{1323.82 \text{ lb}}{\text{ft}^3} \cdot \frac{144 \cancel{\text{ft}^2}}{\cancel{\text{s}^2}} \cdot \frac{1 \cancel{\text{s}^2}}{64.4 \text{ ft}}$$

$$= 2960 \text{ lb/ft}^2 \cdot \frac{1 \text{ lb/in}^2}{144 \text{ lb/ft}^2} = \boxed{20.5 \text{ psi}} \quad \underline{\underline{\text{ANS}}}$$

Part E Calculations:

Find pressure increment

$$F = \rho C A V \quad \therefore \Delta p = \rho C V \quad P_{\max} = P_{\text{op}} + \Delta p$$

$$C = \frac{\sqrt{\frac{E_0}{\rho}}}{\sqrt{1 + \frac{E_0 D}{E \delta}}}$$

$$E_0 = \text{Bulk Modulus}_{\text{Fluid}} = 316,000 \text{ psi}$$

$$\rho = \text{Fluid density} = 981 \text{ slugs/ft}^3$$

$$D = \text{pipe diameter} = .1342 \text{ ft}$$

$$E = \text{elastic Modulus of pipe} = 200 \text{ GPa}$$

$$\delta = \text{pipe thickness} = .0120 \text{ ft}$$

$$\text{Convert: Psi} = 144 \text{ PSF}$$

$$E_0 = 45504000 \text{ psf} \quad \rho = 981 \frac{\text{lb} \cdot \text{s}^2}{\text{ft}^4} \quad E = (200 \text{ GPa}) \frac{145038 \text{ Psi}}{1 \text{ GPa}} = 29007600 \text{ Psi}$$

> solve for wave velocity

$$E = 4177094400 \text{ PSF}$$

$$C = \frac{\sqrt{\frac{45504000 \text{ lb/ft}^2}{981 \text{ lb} \cdot \text{s}^2/\text{ft}^4}}}{\sqrt{1 + \frac{(45504000 \text{ lb/ft}^2)(.1342 \text{ ft})}{(4177094400 \text{ lb/ft}^2)(.0120 \text{ ft})}}} = \frac{\sqrt{46385.32 \frac{\text{ft}^2}{\text{s}^2}}}{\sqrt{1 + 1.218}}$$

Note: units in denominator cancel (as they must)

$$C = \frac{215.37 \text{ ft/s}}{2.28} = 94.46 \text{ ft/s} \quad \text{Ans}$$

$$\Delta p = \rho C V = \left(981 \frac{\text{lb} \cdot \text{s}^2}{\text{ft}^4} \right) \left(94.46 \frac{\text{ft}}{\text{s}} \right) \left(11.81 \frac{\text{ft}}{\text{s}} \right)$$

$$\Delta p = 1094376.721 \text{ lb/ft}^2 = \boxed{7599.83 \text{ Psi}} \quad \underline{\underline{\text{Ans}}}$$

Part F Calculation:

$$\text{Max log size (part C)} = .4076 \text{ ft}$$

$$\text{New log} = .2038 \text{ ft}$$

$$F_D = C_D \left(\frac{\rho v^2}{2} \right) A$$

CD = Drag Coeff.

 ρ = fluid density

V = Channel velocity

A = projected Area

$$\frac{Q}{A} = \frac{.167 \text{ ft}^3/\text{s}}{.198 \text{ ft}^2} = .843 \text{ ft/s}$$

$$A_p = .2038 = .0415 \text{ ft}^2$$

$$F_D = 1.16 \left(\frac{1.94 \text{ slugs/ft}^3}{2} \right) \left(.843 \text{ ft/s} \right)^2 \cdot .0415 \text{ ft}^2$$

$$F_D = \frac{(62.42 \text{ lb/ft}^3) (.843 \text{ ft/s})^2 (1.16) (.0415 \text{ ft}^2)}{2}$$

$$= \frac{(62.42 \text{ lb/ft}^3) (.7106 \text{ ft}^2/\text{s}^2) (1.16) (.0415 \text{ ft}^2)}{2}$$

$$= \frac{44.36 \text{ lb/ft} \cdot \text{s}^2}{2} = 22.18 \text{ lb/ft} \cdot \text{s}^2 (1.16) = \frac{25.73 \text{ lb}}{\text{ft} \cdot \text{s}^2}$$

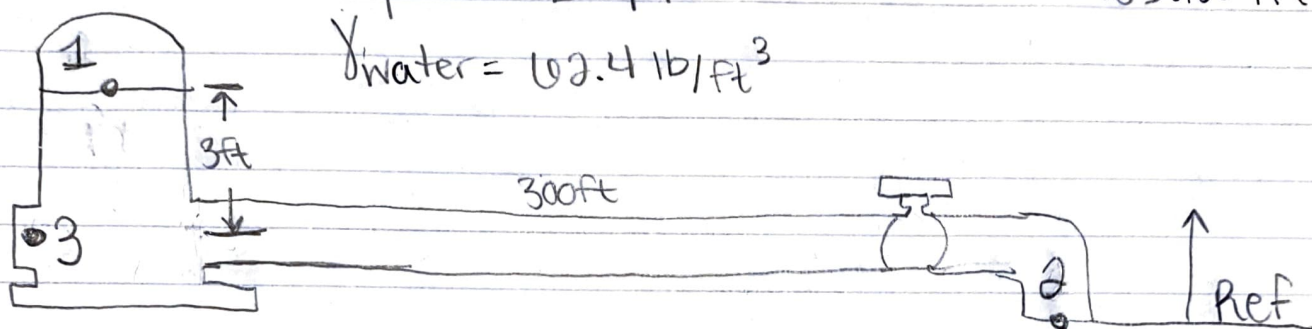
$$\frac{25.73 \text{ lb}}{\text{ft} \cdot \text{s}^2} (.0415) \text{ ft}^2 = 1.07 \text{ lb} \cdot \text{ft}/\text{s}^2 = \boxed{.1384 \text{ N}}$$

Part G calculations

> Compute force acting on flange: Diameter_{flange} = D_{pipe}

from part b: $h_L = \text{pipe} + \text{valve} + \text{elbow} = 105.1624 \text{ ft}$

$$\gamma_{\text{water}} = 62.4 \text{ lb/ft}^3$$



> Find pressure in tank (Air) using bernoulli's

$$\frac{P_1}{\gamma} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\gamma} + \frac{V_2^2}{2g} + z_2 + h_L$$

$$P_1 = 0$$

$$V_1 = 0$$

$$z_1 = 0$$

$$\frac{P_1}{\gamma} = \frac{V_2^2}{2g} + h_L - z_1$$

$$\frac{P_1}{\gamma} = \frac{(11.81 \text{ ft/s})^2}{2 \times 32.2 \text{ ft/s}^2} + 105.16 \text{ ft} - 3 \text{ ft} = 139.48 \text{ ft} + 105.16 \text{ ft} - 3 \text{ ft}$$

$$P_1 = \gamma (241.64) = 62.4 \text{ lb/ft}^3 (241.64 \text{ ft})$$

$$P_1 = 15078.3 \text{ lb/ft}^2$$

> Find pressure 3 ft below water surface to find pressure @ point 3 using gamma h equation:

$$P_3 = \gamma h = 62.4 \text{ lb/ft}^3 (3 \text{ ft}) = 187.2 \text{ lb/ft}^2$$

> pressure felt by flange = $P_1 + P_3$

$$P_1 + P_3 = 15078.3 \text{ lb/ft}^2 + 187.2 \text{ lb/ft}^2 = 15265.5 \text{ lb/ft}^2$$



Part G calculations Continued

$$F = \frac{P}{A}, \text{ total pressure at flange was found to be } 15265.5 \text{ lb/ft}^2$$

To find force, divide pressure by area of flange, $D_{\text{flange}} = D_{\text{pipe}}$

$$A_{\text{flange}} = \frac{\pi D^2}{4} = \frac{\pi (.125)^2}{4} = 1.77 \text{ ft}^2$$

$$\frac{15265.5 \text{ PSF}}{1.77 \text{ ft}^2} = \boxed{8624.6 \text{ lb force}} \quad \underline{\underline{\text{ANS}}}$$

Where is the location of the force?

> Since flange is circular, force is exerted on the center of the flange

ANS

> Summary: a-g

- a) After iteration, channel depth was determined to be .388 ft or 4.06 in. (see excel sheet)
- b) Total h_L was found to be 105.16 ft. Sum of force equation yield a horizontal force of 88.95 lb and a vertical force of 3.877 lb.
- c) The largest log was found to be .4076 ft or .124 m. Calculating MB yielded a ymc of .21 ft. Since M_C is slightly higher than the center of gravity, the log used is indeed stable. (Barely stable)
- d) The pressure drop across the nozzle was found to be 20.5 psi.
- e) Solving the wave velocity equation yielded a wave velocity of 94.46 ft/s. plugging this value into the pressure equation yielded a Δp of 7599.83 PSI. Therefore, no cavitation occurs in the system since Cavitation requires extreme pressure drop.
- f) The drag force experienced by a log half the size of maximum size was calculated to be .1384 N
- g) The pressure at the fluid surface of the tank was found to be 15078.3 lb/ft³, and at the flange was found to be 15265.5 lb/ft³. Dividing by the area of the flange yielded a force of 8624.6 lb. Location of force was assumed to be centered on the flange.

> Materials:

- 300ft Sched 40 steel pipe $1\frac{1}{2}$ inch - Water @ 60°
- Hickory Wood log(s)
- Open channel to carry logs

> Analysis: a-g

- The key to solving this problem was to realize the flow rate equation used could be manipulated to solve for the unknowns using the "left hand - right hand" rule. Furthermore, understanding that since all variables were in terms of "y", except for Q , y could be assumed and iterated until $Q_{act} = Q_{calc}$, proving "y" assumed correctly.
- A crucial part of solving this part was manipulating Bernoulli's to solve for P_1 . In addition, determining the losses in the pipe and elbow were essential to define the forces acting on the system. As expected, the forces in the horizontal were much greater than that of the vertical. Such information should assist the Civil Engineer in creating adequate support for the pipe.
- The key to solving part C was realizing the relationship between V and V_d under the given conditions. Once max log size was found, it was very straightforward to determine stability. It should be noted that although the log was found to be stable, it was BARELY so. Therefore the logs are not stable beyond all doubt. Such is to be expected for a square-cross section.

- d) Part d was simply a matter of locating required constants and variables. In addition, it required the manipulation of the nozzle equation to isolate Δp . A key part of solving this part was realizing β was given and N_R could be calculated and used to solve for C. The found answer of 80.5 psi seems to make sense given large size of the nozzle.
- e) This part was very straight forward once units were made to match. Plugging in wave velocity to the Δp equation a high pressure, which is to be expected under extreme conditions of a waterhammer. Furthermore, no cavitation occurred since it requires the pressure to drop below vapor pressure.
- f) Drag force of the half-sized log was found to be relatively small at .1384 N, which makes sense given the log size and fluid velocity creating said drag force.
- g) The key to part g was to recognize the pressure within the tank, thus the need to use Bernoulli's to determine tank pressure. However, the force exerted on the flange was found to be 8624.6 lb. which seems slightly high for a tank storing 3ft of pressurized fluid.