

- 7.11 A submersible deep-well pump delivers 745 gal/h of water through a 1-in Schedule 40 pipe when operating in the system sketched in Fig. 7.18. An energy loss of 10.5 lb-ft/lb occurs in the piping system. (a) Calculate the power delivered by the pump to the water. (b) If the pump draws 1 hp, calculate its efficiency."

Given:

Pump Rate:  $745 \frac{\text{gal}}{\text{hr}}$

Pipe: 1 in sch 40

Energy loss:  $-10.5 \frac{\text{lb-ft}}{\text{lb}}$

find: a) Cal Power delivered by pump

b) Cal Eff of pump @ 1 Hp

① Step 1 - Solve for  $h_A$

$$\frac{P_1}{\gamma_w} + z_1 + \frac{v_1^2}{2g} + h_A - h_L = \frac{P_2}{\gamma_w} + z_2 + \frac{v_2^2}{2g}$$

$$h_A = \frac{P_2}{\gamma_w} + (z_2 + z_1) + h_L$$

$$h_A = \frac{40 \frac{\text{lb}}{\text{in}^2} \cdot \frac{144 \text{ in}^2}{1 \text{ ft}^2}}{64.2 \frac{\text{lb}}{\text{ft}^3}} + (120 \text{ ft} + 10.5 \text{ ft})$$

$$h_A = 89.72 \text{ ft} + 130.5 \text{ ft}$$

$$h_A = \underline{\underline{220.22 \frac{\text{lb-ft}}{\text{lb}}}}$$

Solve for Q

$$Q = 745 \frac{\text{gal}}{\text{hr}} \left( \frac{1 \text{ hr}}{60 \text{ min}} \right)$$

$$12.42 \frac{\text{gal}}{\text{min}} \times \frac{1 \frac{\text{gal}}{\text{min}}}{0.002 \frac{\text{ft}^3}{\text{sec}}} = \underline{\underline{0.0273 \frac{\text{ft}^3}{\text{sec}}}}$$

$$P_1 = 0 \quad P_2 = 40 \frac{\text{lb}}{\text{in}^2}$$

$$v_1 = 0 \quad v_2 = 0$$

$$\gamma_w = 62.4 \frac{\text{lb}}{\text{ft}^3}$$

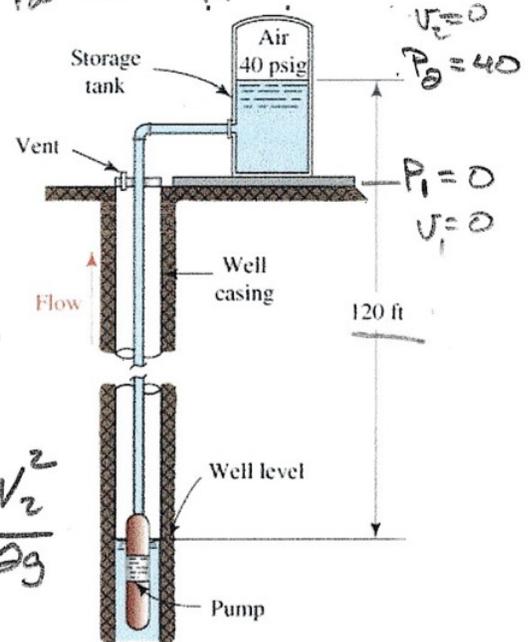


Figure 7.18

Conversion

$$1 \frac{\text{gal}}{\text{min}} = 0.002 \frac{\text{ft}^3}{\text{sec}}$$

$$449 \frac{\text{gal}}{\text{min}} = 1 \frac{\text{ft}^3}{\text{sec}}$$

7.11 continued

$$\textcircled{a} P_A = h_A \gamma_w Q$$

$$= \left( 220.22 \frac{\text{lb} \cdot \text{ft}}{\text{lb}} \right) \times \left( 62.4 \frac{\text{lb} \cdot \text{ft}}{\text{ft}^3} \right) \times \left( 0.0273 \frac{\text{ft}^3}{\text{sec}} \right)$$

$$= 375.15 \frac{\text{lb} \cdot \text{ft}}{\text{lb} \cdot \text{s}} \cdot \frac{1 \text{ HP}}{550 \frac{\text{lb} \cdot \text{ft}}{\text{sec}}}$$

$$P_A = \underline{\underline{0.682 \text{ HP}}}$$

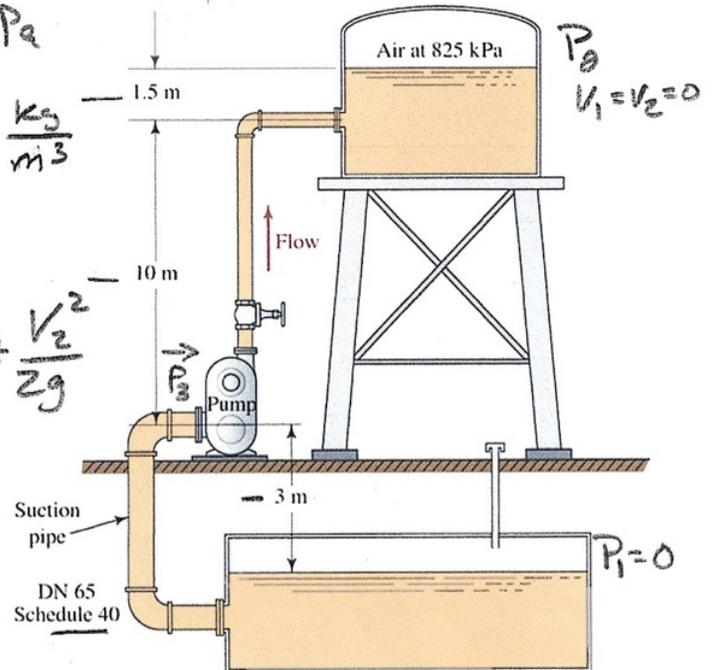
$$\textcircled{b} \text{EFF}_m = \frac{P_A}{P_I} = \frac{0.682 \text{ HP}}{1 \text{ HP}}$$

$$\text{EFF} = 0.682$$

$$\text{EFF} = \underline{\underline{68\%}}$$

7.16 Figure P7.16 shows a pump delivering 840L/MIN. of crude oil ( $sg = 0.85$ ) from an underground storage drum to the first stage of a processing system. (a) If the total energy loss in the system is  $4.2 \text{ N} \cdot \text{m/N}$  of oil flowing, calculate the power delivered by the pump. (b) If the energy loss in the suction pipe is  $1.4 \text{ N} \cdot \text{m/N}$  of oil flowing, calculate the pressure at the pump inlet.

Figure P7.16



Oil pump and tanks for Problem 7.16.

Given:

Pump  $840 \frac{\text{L}}{\text{min}}$   $P_2 = 825 \text{ kPa}$

Oil  $sg = 0.85 \cdot 1000 \rightarrow 850 \frac{\text{kg}}{\text{m}^3}$   
 $\rho = 850 \frac{\text{kg}}{\text{m}^3}$

$$\frac{P_1}{\gamma_0} + z_1 + \frac{V_1^2}{2g} + h_A - h_L = \frac{P_2}{\gamma_0} + z_2 + \frac{V_2^2}{2g}$$

$$h_A = \frac{P_2}{\gamma_0} + (z_2 - z_1) + h_L$$

$$h_A = \frac{825 \text{ kN/m}^3}{(0.85)(9.81 \text{ kN})} + 14.5 \text{ m} + 4.2 \text{ m}$$

$$h_A = 98.94 + 18.7$$

$$h_A = 117.64 \text{ m}$$

$$1 \frac{\text{m}^3}{\text{sec}} = 60000 \frac{\text{L}}{\text{min}}$$

$$Q = \frac{840 \frac{\text{L}}{\text{min}}}{60000 \frac{\text{L}}{\text{min}}} \cdot 1 \frac{\text{m}^3}{\text{sec}} = 0.014 \frac{\text{m}^3}{\text{sec}}$$

$$Q = 0.014 \frac{\text{m}^3}{\text{sec}}$$

$$P_A = h_A \gamma_0 Q$$

$$= (117.64 \text{ m}) (0.85) \left( \frac{9.81 \text{ kN}}{\text{m}^3} \right) \left( 0.014 \frac{\text{m}^3}{\text{sec}} \right)$$

$$= 980.94 \frac{\text{kN}}{\text{m}^2} \left( 0.014 \frac{\text{m}^3}{\text{sec}} \right)$$

①  $P_A = 13.73 \frac{\text{K} \cdot \text{N} \cdot \text{m}}{\text{Sec}} \rightarrow 13.73 \text{ kW}$

7.16 Continued...

(b)

$$\frac{P_1}{\gamma_0} + z_1 + \frac{V_1^2}{2g} - h_{Ls} = \frac{P_3}{\gamma_0} + z_3 + \frac{V_3^2}{2g}$$

$$V_3 = \frac{Q}{A_3} = \frac{0.014 \frac{m^3}{sec}}{0.003091 m^2} = \underline{4.63 \frac{m}{sec}}$$

→ DN Sch 40 pipe  
Table F.1  
Flow Rate  
→  $3.090 \times 10^{-3} m^2$

$$P_3 = \gamma_0 \left[ (z_1 - z_3) - \frac{V_3^2}{2g} - h_{Ls} \right]$$

$$P_3 = (0.85) \left( 9.81 \frac{kN}{m^3} \right) \left[ -3m - \frac{(4.63 \frac{m}{sec})^2}{2(9.81 \frac{m}{sec^2})} - \frac{1.4 N \cdot m}{N} \right]$$

$$P_3 = \left( 8.338 \frac{kN}{m} \right) \left( -3m - 1.093m - 1.4 \frac{N \cdot m}{N} \right)$$

-5.493

$$P_3 = \underline{\underline{-45.80 k \frac{N}{m^2}}} \Rightarrow \underline{\underline{-45.80 kPa}}$$

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7.22 Figure P7.22 shows the arrangement of a circuit for a hydraulic system. The pump oil with a specific gravity of 0.90 from a reservoir and delivers it to the hydraulic cylinder. The cylinder has an inside diameter of 5.0 in, and 15 sec the piston must travel 20 inches while exerting a force of 11000 lb. It is established that there are energy losses of 11.5 lb-ft/lb in the section pipe and 35.0 lb-ft/lb in the discharge pipe. Both pipes are 3/8 inches Schedule 80 steel pipe. Calculate:

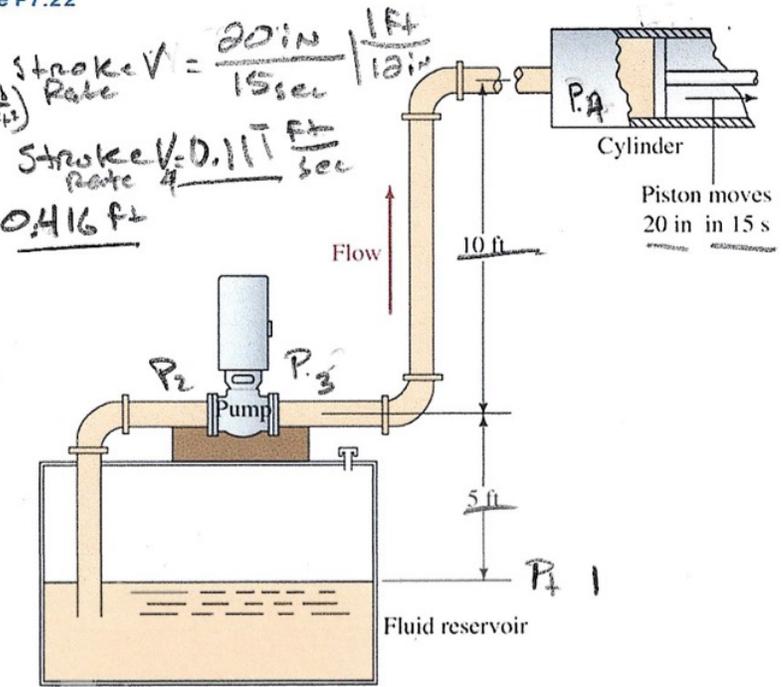
- ✓ a. The volume flow rate through the pump
- ✓ b. The pressure at the cylinder
- ✓ c. The pressure at the outlet of the pump
- ✓ d. The pressure at the inlet to the pump
- ✓ e. The power delivered to the oil by the pump

Given:

Figure P7.22

$F = 11000 \text{ lb}$

Oil  $Sg = 0.90$   
 $\gamma_o(\omega) = Sg \gamma_{H_2O} = 0.90 (62.4 \frac{\text{lb}}{\text{ft}^3})$   
 → Cylinder  
 Inside Dia =  $\frac{5.0 \text{ in}}{12 \text{ in/ft}} = 0.416 \text{ ft}$   
 → Energy loss  
 suction side =  $11.5 \frac{\text{lb-ft}}{\text{lb}}$   
 discharge side =  $35 \frac{\text{lb-ft}}{\text{lb}}$   
 Pipe  $\frac{3}{8}$  in sch 80  
 $A = \frac{1}{4} \pi (\dots)$



Hydraulic system for Problem 7.22.

①  $Q = A_{cy} \cdot \text{stroke Rate (v)}$   
 $= \frac{\pi (0.416)^2}{4} \cdot 0.11 \frac{\text{ft}}{\text{sec}}$   
 $Q = 0.0152 \frac{\text{ft}^3}{\text{sec}}$

②  $P_{cyl} = \frac{F}{A_{cy}}$   
 $P_{cyl} = \frac{11000 \text{ lb}}{\left[ \frac{\pi (0.416 \text{ ft})^2}{4} \right]}$   
 $P_{cyl} = 80659.55 \frac{\text{lb}}{\text{ft}^2}$

7.22 continued...

c) Pressure @ outlet of pump

$$\frac{P_2}{\gamma_0} + z_2 + \frac{V_2^2}{2g} + h_L = \frac{P_3}{\gamma_0} + z_3 + \frac{V_3^2}{2g}$$

$$P_2 = P_3 + \gamma_0 (z_3 - z_2) + \frac{V_3^2 - V_2^2}{2g} + h_L$$

Find!

Velocity  
 @  $V_3 = 0.117 \frac{\text{ft}}{\text{sec}}$   
 @  $V_2$

$\gamma_0 = (0.90) 62.4 \frac{\text{lb}}{\text{ft}^3}$   
 $\gamma_0 = 56.16 \frac{\text{lb}}{\text{ft}^3}$

$V_2 = \frac{Q}{A_c}$   
 $V_2 = \frac{0.0152 \frac{\text{ft}^3}{\text{sec}}}{0.000976 \text{ft}^2}$   
 $V_2 = 15.57 \frac{\text{ft}}{\text{sec}}$

→ Table F.2  
 Flow Rate  
 $\frac{3}{8}$  sch 80  
 $0.000976 \text{ft}^2$   
 $P_3 = \frac{11000 \text{lb f}}{19.65 \text{in}^2 A_c}$   
 $P_3 = 560 \frac{\text{lb}}{\text{in}^2}$

$$\rightarrow P_2 = 560 \frac{\text{lb}}{\text{in}^2} + 56.16 \frac{\text{lb}}{\text{ft}^3} \left( 10 \text{ft} + \frac{(0.117 \text{ft}^2 - 15.57 \text{ft}^2)}{2 \cdot (32.2 \frac{\text{ft}}{\text{sec}^2})} \right) + 35 \text{ft}$$

$$= 560 \frac{\text{lb}}{\text{in}^2} + 56.16 \frac{\text{lb}}{\text{ft}^3} \left( 10 \text{ft} + \frac{-243.051}{64.4} \right) + 35 \text{ft}$$

$$= 560 \frac{\text{lb}}{\text{in}^2} + \left[ 56.16 \frac{\text{lb}}{\text{ft}^3} \right]$$

$$\left[ \frac{2315.80 \frac{\text{lb}}{\text{ft}^3} \text{ft}^2}{144 \text{in}^2} \right]$$

$$= 560 \frac{\text{lb}}{\text{in}^2} + 16.08 \frac{\text{lb}}{\text{in}^2}$$

$$P_2 = \underline{\underline{576.08 \frac{\text{lb}}{\text{in}^2}}}$$

7.22

d. FIND Pressure @ inlet PUMP.

$$\frac{P_1}{\gamma_0} + z_1 + \frac{V_1^2}{2g} - h_{L4} = \frac{P_4}{\gamma_0} + z_4 + \frac{V_4^2}{2g}$$

$$P_4 = \gamma_0 \left( z_1 - z_4 - \frac{V_4^2}{2g} - h_{L4} \right)$$

$$P_4 = 56.16 \frac{\text{lb}}{\text{ft}^3} \left( -5 \text{ ft} - \frac{(15.57 \frac{\text{ft}}{\text{sec}})^2}{2(32.2 \frac{\text{ft}}{\text{sec}^2})} - 11.5 \text{ ft} \right)$$

$$= 56.16 \frac{\text{lb}}{\text{ft}^3} (-5 - 3.76 - 11.5)$$

$$= (56.16 \frac{\text{lb}}{\text{ft}^3}) (-12.74 \text{ ft})$$

$$= -715.23 \frac{\text{lb}}{\text{ft}^2} \left| \frac{1 \text{ ft}^2}{144 \text{ in}^2} \right.$$

$$= \underline{\underline{-4.97 \frac{\text{lb}}{\text{in}^2}}} \quad \text{OR} \quad \underline{\underline{-4.97 \text{ PSI}}}$$

7.22 e) Power to oil by Pump.

$$\frac{P_1}{\gamma_o} + z_1 + \frac{V_1^2}{2g} + h_1 - h_{s4} - h_{L4} = \frac{P_3}{\gamma_o} + z_3 + \frac{V_3^2}{2g}$$

$$h_1 = \frac{P_3}{\gamma_o} + (z_3 - z_1) + \frac{V_4^2}{2g} + h_{s4} + h_{L4}$$

$$= \frac{80659.55 \frac{\text{lb}}{\text{ft}^2}}{56.16 \frac{\text{lb}}{\text{ft}^3}} + \frac{(0.117 \frac{\text{ft}}{\text{sec}})^2}{2(32.2 \frac{\text{ft}}{\text{sec}^2})} + 11.5 \text{ ft} + 35 \text{ ft}$$

$$\gamma_o = 56.16 \frac{\text{lb}}{\text{ft}^3} \quad = 1436.25 \text{ ft} + [0.000192 \text{ ft} + 11.5 \text{ ft} + 35 \text{ ft}]$$

$$P_3 = 80659.5 \frac{\text{lb}}{\text{ft}^2} \quad h_1 = 1482.75 \text{ ft}$$

$$V_4 = 0.117 \frac{\text{ft}}{\text{sec}}$$

$$P_1 = h_1 \gamma_o Q$$

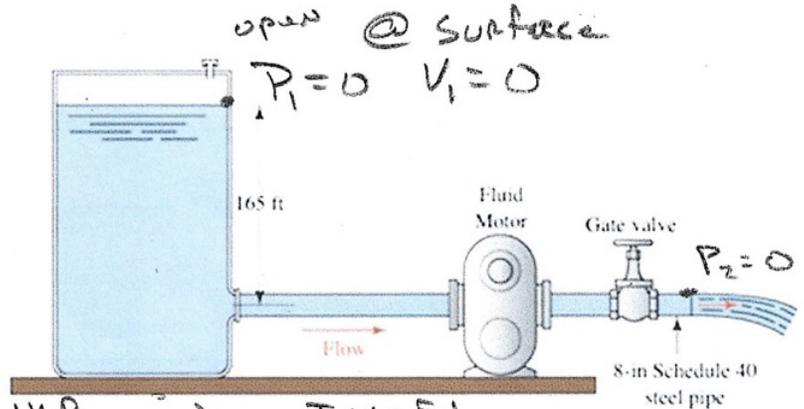
$$P_1 = (1482.75 \text{ ft}) (56.16 \frac{\text{lb}}{\text{ft}^3}) (0.0152 \frac{\text{ft}^3}{\text{sec}})$$

$$P_1 = 1265.70 \frac{\text{ft} \cdot \text{lb}}{\text{sec}} \quad \left| \frac{1 \text{ HP}}{550 \frac{\text{ft} \cdot \text{lb}}{\text{sec}}} \right|$$

$$P_1 = \underline{\underline{2.30 \text{ HP}}}$$

7.30 Water at 60 OF flows from a large reservoir through a fluid motor at a rate of 1000 gal/min in the system shown in Fig. 7.33. If the motor removes 37 hp from the fluid, calculate the energy losses in the system.

Given:  
- Water  
Temp = 60 OF  
Flow Rate = 1000  $\frac{\text{gal}}{\text{min}}$   
 $1 \frac{\text{ft}^3}{\text{sec}} = 449 \frac{\text{gal}}{\text{min}}$



Energy Loss

Power = 37 HP  $(550 \frac{\text{ft} \cdot \text{lb}}{\text{sec}})$   
Figure 7.33

conversion  
Power = 20350  $\frac{\text{ft} \cdot \text{lb}}{\text{sec}}$

Problem 7.30

Table F.1

8 in sch 40  
steel pipe  
→ Flow Area  
0.3420  $\text{ft}^2$

$$\frac{P_1}{\gamma_w} + z_1 + \frac{V_1^2}{2g} - h_R - h_L = \frac{P_2}{\gamma_w} + z_2 + \frac{V_2^2}{2g}$$

$$h_L = (z_1 - z_2) - \frac{V_2^2}{2g} - h_R$$

$$h_R = \frac{\text{Power}}{\gamma_w Q} = \frac{20350 \frac{\text{ft} \cdot \text{lb}}{\text{sec}}}{(62.4 \frac{\text{lb}}{\text{ft}^3}) (2.227 \frac{\text{ft}^3}{\text{sec}})}$$

$$h_R = 146.43 \text{ ft}$$

$$Q = V_2 A$$

$$V_2 = \frac{Q}{A} = \frac{1000 \frac{\text{gal}}{\text{min}}}{0.3420 \text{ ft}^2} \cdot \frac{1 \frac{\text{ft}^3}{\text{sec}}}{449 \frac{\text{gal}}{\text{min}}} = 6.42 \frac{\text{ft}}{\text{sec}}$$

$$h_L = 165 \text{ ft} - \frac{(6.42 \frac{\text{ft}}{\text{sec}})^2}{2 \cdot 32.2 \frac{\text{ft}}{\text{sec}^2}} - 146.43 \text{ ft}$$

$$h_L = 165 \text{ ft} - 0.640 \text{ ft} - 146.43 \text{ ft}$$

$$h_R = 17.94 \text{ ft} = 17.94 \frac{\text{ft} \cdot \text{lb}}{\text{lb}}$$

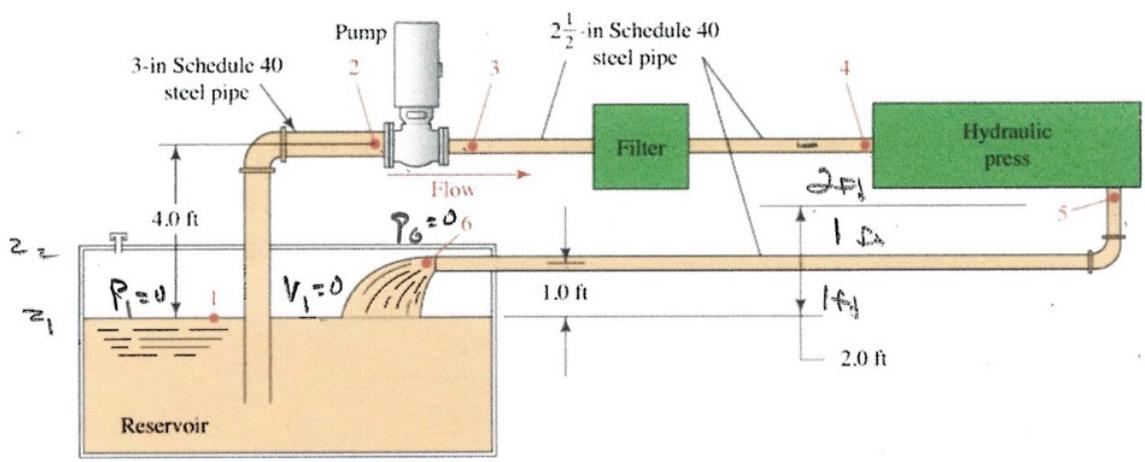
	ODU MET 330 Fluid MEC	HW 1.4
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7.35 Shows a diagram of a fluid power system for a hydraulic press used to extrude rubber parts. The following data are known:

- a. The fluid is oil ( $sg = 0.90$ )
- b. Volume flow rate is 175 gal/min.
- c. Power input to the pump is 28.4 hp.
- d. Pump efficiency is 80 percent.

Table F.1  
3 in Sch 40  
Flow Rate  
 $\rightarrow 0.05132 \text{ ft}^2$   
2 1/2 in Sch 40  
Flow Rate  
 $\rightarrow 0.03326 \text{ ft}^2$   
 $Q = 175 \frac{\text{gal}}{\text{min}} \left| \frac{1 \frac{\text{ft}^3}{30}}{144 \frac{\text{gal}}{\text{min}} \cdot \frac{\text{min}}{60 \text{ sec}}} \right| = 0.390 \frac{\text{ft}^3}{\text{sec}}$

- $h_{L_{1-6}}$  {
- e. Energy loss from point 1 to 2 is 2.80 lb-ft/lb.
  - f. Energy loss from point 3 to 4 is 28.50 lb-ft/lb.
  - g. Energy loss from point 5 to 6 is 3.50 lb-ft/lb."



$$\frac{P_1}{\gamma} + z_1 + \frac{V_1^2}{2g} - h_{L_{1-6}} + h_A - h_R = \frac{P_6}{\gamma} + z_6 + \frac{V_6^2}{2g}$$

$$h_R = (z_1 - z_6) - \frac{V_6^2}{2g} - h_{L_{1-6}} + h_A$$

$$V_6 = \frac{Q}{A_6} = \frac{0.390 \frac{\text{ft}^3}{\text{sec}}}{0.03326 \text{ ft}^2} = 11.73 \frac{\text{ft}}{\text{sec}}$$

7.35.  $V_6 = \frac{Q}{A_6} = \frac{0.390 \frac{ft^3}{sec}}{0.03326 ft^2} = 11.73 \frac{ft}{sec}$

$$h_R = (z_1 - z_6) - \frac{V_6^2}{2g} - h_{L1-6} + h_A$$

$$h_R = -1 ft - \frac{(11.73 \frac{ft}{sec})^2}{2(32.2 \frac{ft}{sec^2})} - [2.80 + 28.5 + 3.50] + h_A$$

→ 34.80 ft

$$h_R = -1 ft - 2.14 ft - 34.80 ft + 552.43 ft$$

$$h_R = \underline{512.49 ft}$$

$Q = 0.390 \frac{ft^3}{sec}$   
 $\gamma_0 = 58.03 \frac{lb}{ft^3}$   
 $P_A = 12496 \frac{ft \cdot lb}{sec}$

$P_R = h_R \gamma_0 Q$   
 $P_R = (512.49 ft)(58 \frac{lb}{ft^3})(0.390 \frac{ft^3}{sec})$   
 $P_R = 11592.5 \frac{ft \cdot lb}{sec} \quad | \quad 1 HP$   


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 $550 \frac{ft \cdot lb}{sec}$

$P_A = h_A \gamma_0 Q$   
 $h_A = \frac{P_A}{\gamma_0 Q}$   
 $h_A = \frac{12496 \frac{ft \cdot lb}{sec}}{(58 \frac{lb}{ft^3})(0.390 \frac{ft^3}{sec})}$   
 $h_A = \underline{552.43 ft}$

$P_R = \underline{\underline{21.08 HP}}$

7.42 Professor Crocker is building a cabin on a hillside and has proposed the water system shown Fig 7.38. The distribution tank in the cabin maintains a pressure of 30.0 psig above the water. There is an energy loss of 15.5 lb-ft/lb in the piping. When the pump is delivering 40 gal/min of water, compute the horsepower delivered by the pump to the water.

Given:

(Cabin TANK)  $P_2 = 30 \frac{\text{lb}}{\text{in}^2} \left| \frac{144 \text{in}^2}{\text{ft}^2} \right| = 4320 \frac{\text{lb}}{\text{ft}^2}$

( $h_L$ ) Energy Loss =  $15.5 \frac{\text{lb-ft}}{\text{lb}}$

( $Q$ ) Pump flow rate =  $40 \frac{\text{gal}}{\text{min}} \left| \frac{1 \text{ ft}^3/\text{sec}}{449 \text{ gal}/\text{min}} \right|$   
 $Q = 0.0891 \frac{\text{ft}^3}{\text{sec}}$

$\gamma_w = 62.4 \frac{\text{lb}}{\text{ft}^3}$

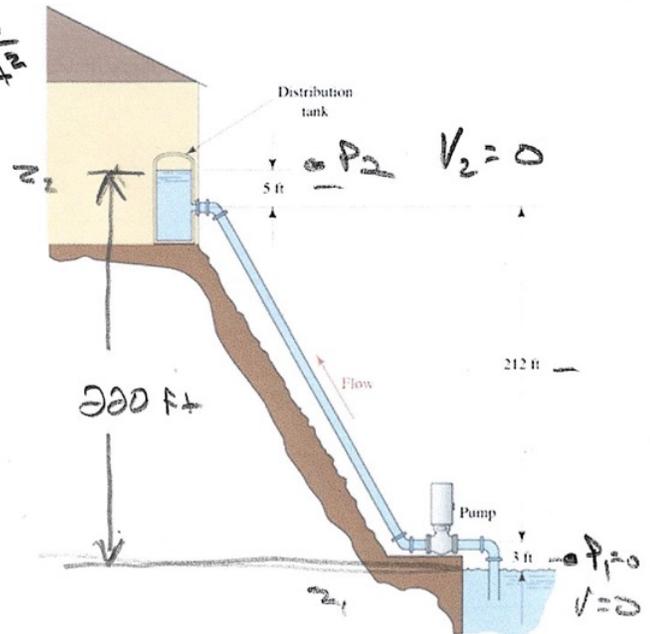


Figure 7.38  
Problems 7.42 and 7.43

$$\frac{P_1}{\gamma} + z_1 + \frac{V_1^2}{2g} - h_L + h_A = \frac{P_2}{\gamma} + z_2 + \frac{V_2^2}{2g}$$

$$h_A = \frac{P_2}{\gamma} + (z_2 - z_1) + h_L$$

$$= \frac{4320 \frac{\text{lb}}{\text{ft}^2}}{62.4 \frac{\text{lb}}{\text{ft}^3}} + 220 \text{ ft} + 15.5 \text{ ft}$$

$$= 69.23 \text{ ft} + 220 \text{ ft} + 15.5 \text{ ft}$$

$$\Rightarrow h_A = 304.73 \text{ ft}$$

$$P_A = h_A \gamma Q = (304.73 \text{ ft}) \left( 62.4 \frac{\text{lb}}{\text{ft}^3} \right) \left( 0.0891 \frac{\text{ft}^3}{\text{sec}} \right)$$

$$P_A = 1694.25 \frac{\text{ft-lb}}{\text{sec}} \left| \frac{1 \text{ HP}}{550 \frac{\text{ft-lb}}{\text{sec}}} \right| = 3.08 \text{ HP}$$