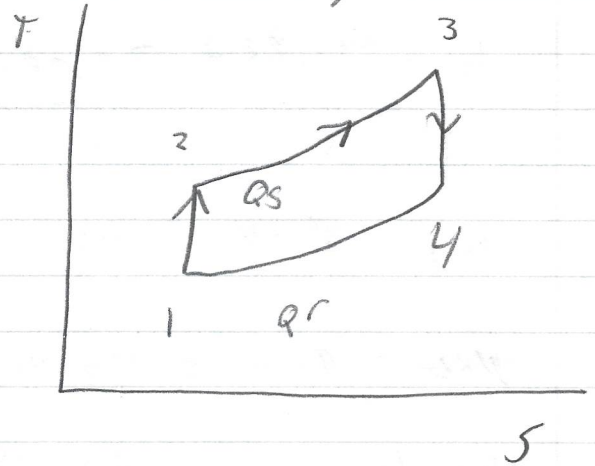
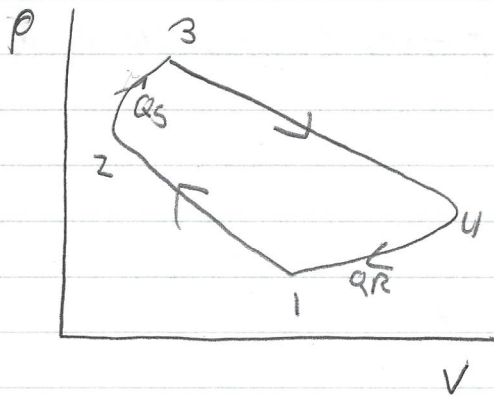


Thermal applications

HW 1 Ben Smithson

13.



① $P_1 = 100 \text{ kPa}$
 $T_1 = 295 \text{ K}$

② $P_2 = 600 \text{ kPa}$
 $T_2 = 500 \text{ K}$

③ $T_3 = 1500 \text{ K}$
 $P_{r2} = 7.84$

④ $P_4 = 100 \text{ kPa}$

$$h_1 = 295.17 \quad \phi_{r1} = 1.3068$$

$$\frac{P_{r2}}{P_{r1}} = \frac{P_2}{P_1} = \frac{P_{r2}}{1.3068} = \frac{600}{100} \quad P_{r2} = 7.84$$

$$P_{r2} = 7.84$$

$$4-17 \quad h_2 = 352.08 + \frac{7.84 - 7.83}{8.4 - 7.83} (359.4 - 352.08) = 352.28 \text{ kJ/kg}$$

$$T_2 = 490.3 \text{ K}$$

$$v_3 = 1205.41 \quad P_{r3} = 601.9 \quad P_3 = 1835.7 \text{ kPa}$$

$$\frac{P_{r4}}{P_{r3}} = \frac{P_4}{P_3} = \frac{P_{r4}}{601.9} = \frac{100}{1835.7} = 32.78$$

$$h_4 = 734.82 + \frac{32.78 - 32.02}{33.72 - 32.02} (745.62 - 734.82)$$

$$h_4 = 739.64 \text{ kJ/kg}$$

$$w_{net} = q_s - q_r = (u_3 - u_2) - h_4 - h_1$$

$$w_{net} = (1205.4 - 352.28) - (739.64 - 295.17)$$

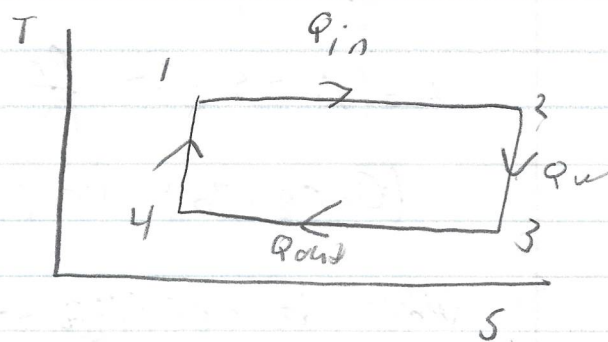
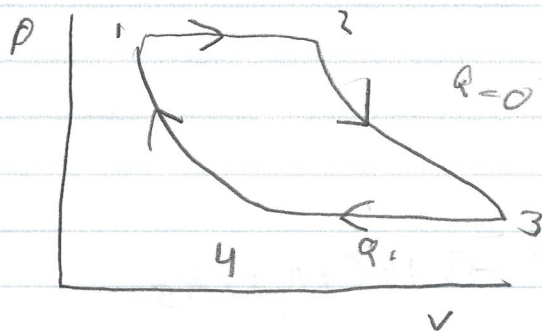
$$w_{net} = 408.66 \text{ kJ/kg}$$

$$\eta_{th} = \frac{w_{net}}{q_s} = \frac{w_{net}}{u_3 - u_2}$$

$$= \frac{408.66}{1205.4 - 352.28} = 47.99\%$$

Thermodynamics Applications Ben Smithson HW 1

18.



$$T_H = 1200K$$

$$T_L = 350K$$

$$W_{net} = 0.8 \text{ J}$$

①

$$T_1 = 1200K$$

$$P_{r1} = 2.3K$$

$$P_1 = 30.0 \text{ MPa}$$

$$s_1 = 3.19$$

②

$$T_2 = 1200K$$

$$P_{r2} = 2.3K$$

$$s_2 = 3.178$$

③

$$T_3 = 350K$$

$$P_{r3} = 2.379$$

$$P_3 = 150.1 \text{ MPa}$$

$$s_3 = 1.897$$

④

$$T_4 = 350K$$

$$P_{r4} = 2.38$$

$$P_4 = 300.1 \text{ MPa}$$

$$s_4 = 1.587$$

$$\frac{P_1}{P_4} = \frac{P_{r1}}{P_{r4}}$$

$$P_1 \left(\frac{2.38}{2.379} \right) (300K) \quad P_1 = 30.012.6 = 30.01 \text{ MPa}$$

$$W_{net} = Q_{in} - Q_{out}$$

$$\eta_{th} = 1 - \frac{350K}{1200K} = 0.7083$$

$$Q_{in} = 0.9 \text{ kJ} / 0.7083 = 0.706 \text{ kJ}$$

$$ds = \frac{80}{9}$$

$$ds = (s_1 - s_2) - \frac{p_1}{p_3}$$

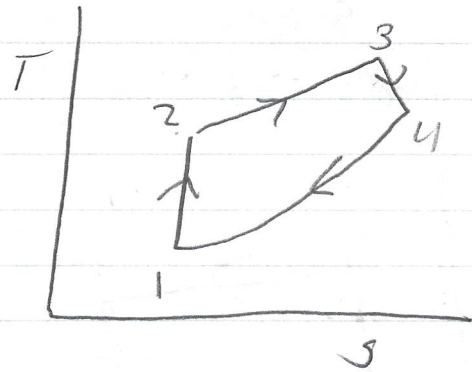
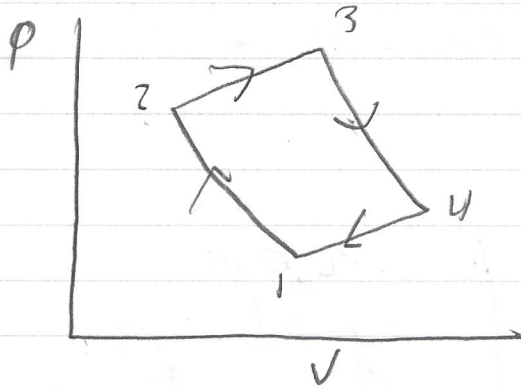
$$(0.08 \cdot 70) \cdot \ln \left(\frac{300 \text{ K}}{180 \text{ K}} \right) = 0.1984 \text{ KJ/Kg}$$

$$w_{net} = 0.1984 (1200 - 350) \text{ K}$$

$$m_{air} = \frac{0.5 \text{ Kg}}{169.89} = 0.0023 \text{ Kg}$$

Thermal applications Ben Smithson HW 1

22



$$T_1 V_1^{k-1} = T_2 V_2^{k-1}$$

① $T_1 = 20^\circ\text{C} = 293\text{K}$
 $V_1 = 1$

② $T_2 = 583.5\text{K}$
 $V_2 = 0.7$

③ $T_3 = 2917.4$

$$T_2 = T_1 \left(\frac{V_1}{V_2} \right)^{k-1}$$

$$k = \frac{C_p}{C_v} = \frac{1}{0.7} = 1.43$$

$$293 \times 5^{1.43-1} = 583.5\text{K}$$

$$W_{1 \rightarrow 2} = R \frac{(T_1 - T_2)}{k-1} = \frac{0.3}{1.43-1} \cdot (293 - 583.5) = 203.6 \frac{\text{kJ}}{\text{kg}}$$

$$Q_{2 \rightarrow 3} = C_p (T_3 - T_2) = 1 \cdot 2917 - 583.43 = 2333.9 \text{ kJ/kg}$$

$$W_{2 \rightarrow 3} = Q_{2 \rightarrow 3} - C_v (T_3 - T_2) = 2333.9 - 0.7(2917.4 - 583.5) = 700.18 \frac{\text{kJ}}{\text{kg}}$$

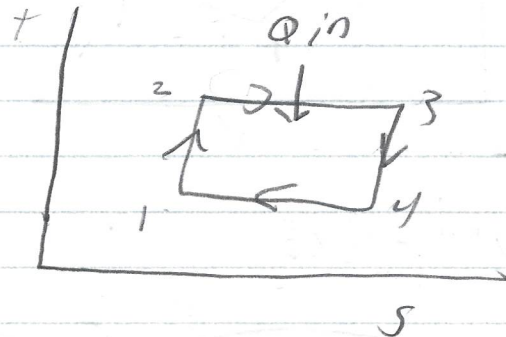
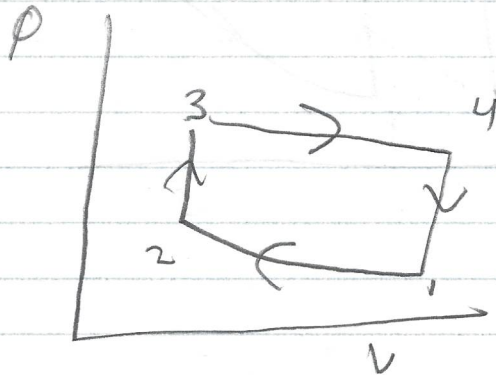
b. $Q_{3 \rightarrow 1} = C_v (T_3 - T_1) = 1837.01 \text{ kJ/kg}$

c. $\eta = 1 - \frac{Q_r}{Q_s} = \frac{Q_{3 \rightarrow 1}}{Q_{2 \rightarrow 3}} = \frac{1837}{2333} = 21\%$

d?

31

$$\frac{90 \text{ kPa}}{40^\circ\text{C} = 313.15 \text{ K}} = 2500 \text{ rpm} = 90 \text{ kW}$$



$$\frac{T_2}{T_1} = \left(\frac{v_1}{v_2} \right)^{\gamma-1}$$

$$T_2 = (313.15) (10.6)^{1.4-1} = 802 \text{ K}$$

$$\eta_{th} = 1 - \left(\frac{313.15}{802} \right) = 0.6095 = 60.9\%$$

$$\dot{Q}_{in} = \frac{90 \text{ kW}}{0.609} = 148 \text{ kW}$$