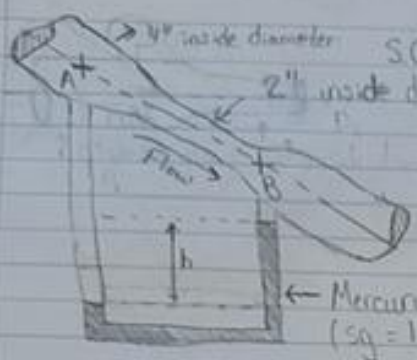



HW1.3

6.79 

SG_{oil} = 0.90 Manometer deflection h = 28 in ($\frac{1}{12}$)
 $Q_A = Q_B = Q$
 $A_A V_A = A_B V_B$
 $\frac{\pi D_A^2}{4} V_A = \frac{\pi D_B^2}{4} V_B$
 $V_B = \left(\frac{D_A}{D_B}\right)^2 V_A$
 $V_B = 4 V_A$
 $P_A = P_B$
 $P_A + \gamma_{oil} Z_A = P_B + \gamma_{oil} (Z_B - h) + \gamma_{Hg} h$
 $P_A - P_B = \gamma_{oil} (Z_B - Z_A - h) + \gamma_{Hg} h$
 $P_A - P_B = 56.16 (Z_B - Z_A - 2.333) + 844.896 (2.333)$
 $P_A - P_B = 56.16 (Z_B - Z_A) + 1971.141 - 131.021$
 $P_A - P_B = 56.16 (Z_B - Z_A) + 1840.121$
 (Pressure difference)
 $E_A = E_B$
 $\frac{P_A}{\gamma_A} + \frac{V_A^2}{2g} + Z_A = \frac{P_B}{\gamma_B} + \frac{V_B^2}{2g} + Z_B$ (Coulter-Like Terms)
 $\frac{(P_A - P_B)}{\gamma_{oil}} + \frac{\gamma_{oil} (Z_B - Z_A)}{2g} = \frac{V_B^2}{2g} - \frac{V_A^2}{2g}$
 $\frac{56.16 (Z_B - Z_A) + 1840.121}{56.16} + \frac{56.16 (Z_B - Z_A)}{2(32.2)(17.33)} = \frac{(4V_A)^2 - V_A^2}{2(32.2)(17.33)}$
 $(32.765)(64.4) = 15 V_A^2$
 $V_A = \sqrt{116.6744 \text{ ft}^2/\text{s}^2} = 10.80 \text{ ft/s}$
 $Q = A_A V_A$
 $Q = \frac{\pi D_A^2}{4} V_A$
 $Q = \frac{\pi \left(4 \text{ in} \left(\frac{1}{12} \text{ ft/in}\right)\right)^2}{4} (10.80 \text{ ft/s}) = 1.0349 \text{ ft}^3/\text{s}$

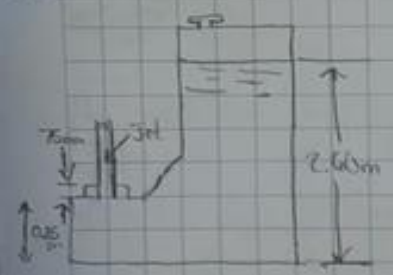
6.82 

2 in Schedule 40 Pipe
 Flow
 24 in
 water

$P_A - P_B = -56.16 \text{ ft}^3 \left(\frac{1}{12} \text{ ft/in}\right) + 62.4 \text{ lb/ft}^3 \left(\frac{8}{12} \text{ ft}\right) + 56.16 \text{ ft}^3 \left(\frac{8}{12} \text{ ft}\right)$
 $P_A - P_B = 114.93 \text{ lb/ft}^2$
 $d_A = (4.5 - 2) \times 0.375 = 4.076 \text{ in}$
 $d_B = (3.375 - 2) \times 0.375 = 2.067 \text{ in}$
 $A_A V_A = A_B V_B$
 $\frac{\pi (4.076 \text{ in})^2}{4} V_A = \frac{\pi (2.067 \text{ in})^2}{4} V_B$
 $V_B = 3.744 V_A$
 $P_A - P_B = \frac{\gamma_A}{2g} (V_B^2 - V_A^2) + \gamma_A (Z_B - Z_A)$
 $\frac{114.93 \text{ lb/ft}^2}{62.4 \text{ lb/ft}^3} = \frac{V_B^2 - V_A^2}{2(32.2 \text{ ft/s}^2)} + 0$
 $V_B = 0.6525 \text{ ft/s}$
 $Q = A_A V_A$
 $Q = \frac{\pi (4.076 \text{ in})^2}{4} \times 0.6525 \text{ ft/s}$
 $Q = 0.058 \text{ ft}^3/\text{s}$

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6.96



$P_1 = \rho g h$
 $(1000 \text{ kg/m}^3)(9.81 \text{ m/s}^2)(2.60 \text{ m})$
 $P_1 = 25,506 \text{ N/m}^2$

$25,506 \text{ N/m}^2 = \rho g h_1 + \rho g h_2$
 $= (1000 \text{ kg/m}^3)(9.81 \text{ m/s}^2)(2.60 \text{ m} - (0.85 \text{ m} + 0.075 \text{ m}))$
 $+ (1000 \text{ kg/m}^3)(9.81 \text{ m/s}^2) h_2$
 $25,506 \text{ N/m}^2 = 16,481.25 \text{ N/m}^2 + 9,810 h_2$
 $9,024.75 \text{ N/m}^2 = 9,810 h_2$
 $h_2 = 0.925 \text{ m}$

$0.85 \text{ m} \left(\frac{1 \text{ m}}{1000 \text{ mm}} \right) = 0.075 \text{ m}$

During class and through the lectures posted on canvas we learned several different things. One of the things we learned is that in a closed loop with a pump we must make sure the Bernoulli's points are placed in the correct position to include the pump. At times, this could even be at the same spot as we saw in 8.49. When working with pipes that bend, we have to make sure to take into account both the horizontal and vertical distances, number of bends and shape of the inlet pipe when figuring out equations. This all helps determine the friction loss in the system.