

14) Given $T_{air} = 20^\circ\text{C}$, $P_{air} = 85\text{ kPa}$, $\phi_{air} = 85\%$

- FIND
- partial pressure of dry air
 - specific humidity of air (W_{air})
 - enthalpy of dry air ($h_{air,dry}$)

Sol: $T = 293\text{ K} \Rightarrow C_p = 1.005\text{ kJ/kg}\cdot\text{K}$

$$P_{sat,20^\circ\text{C}} = 2.3392\text{ kPa}$$

$$h_{g,20^\circ\text{C}} = 2537.4\text{ kJ/kg}$$

$$\begin{aligned} \text{a) } P_g &= P - P_v & P_v &= \phi P_g = .85 (2.3392) \\ P_g &= 85 - 1.7544 & P_v &= 1.7544\text{ kPa} \end{aligned}$$

$$P_g = 83.25\text{ kPa}$$

$$\text{b) } W = \frac{0.622 P_v}{P - P_v} = \frac{0.622 (1.7544)}{85 - 1.7544}$$

$$W = 0.013\text{ kJ/kg dry air}$$

$$\begin{aligned} \text{c) } h &= h_g + W h_v \\ &= 1.005(20) + .0131(2537.4) \end{aligned}$$

$$h = 53.34\text{ kJ/kg}$$

16) Given $V = 8 \text{ m}^3$

Saturated Air @ 30°C , $P = 105 \text{ kPa}$

- FIND
- Mass of dry air
 - specific humidity (w)
 - enthalpy of air per unit mass dry air

Sol

$$T = 303 \text{ K}$$

$$P_g = 105 - 4.2469$$

$$P_{\text{sat}, 30^\circ\text{C}} = 4.2469 \text{ kPa}$$

$$P_a = 100.753 \text{ kPa}$$

$$c_p = 1.005 \text{ kJ/kg}\cdot\text{K}$$

$$P_v = 4.2469$$

$$h_{g, 30^\circ\text{C}} = 2555.6 \text{ kJ/kg}$$

$$a) m_a = \frac{P_a V_a}{R_a T} = \frac{100.753 \text{ kPa} \cdot 8 \text{ m}^3}{(0.287 \text{ kPa}\cdot\text{m}^3/\text{kg}\cdot\text{K}) 303 \text{ K}}$$

$$m_a = 9.27 \text{ kg}$$

$$b) w = \frac{.622 P_v}{P - P_v} = \frac{.622 (4.2469)}{105 - 4.2469}$$

$$w = 0.0262 \text{ kg/kg dry air}$$

$$c) h = c_p T + w h_g$$

$$= 1.005 (30) + .0262 (2555.6)$$

$$h = 97.1 \text{ kJ/kg dry air}$$

18) Given Humid Air $P_1 = 100 \text{ kPa}$
 $T_1 = 20^\circ\text{C} = 293 \text{ K}$
 $\phi_1 = 90\%$

Compressed in Steady flow, isentropic
 Compressor to 800 kPa

FIND a) relative humidity of air at outlet

SOL

$$P_2 = 800 \text{ kPa}$$

$$K = \frac{C_p}{C_v} = \frac{1.005}{1.714} = 1.4$$

$$T_2 = T_1 \left(\frac{P_2}{P_1} \right)^{\frac{K-1}{K}}$$

$$= 293 \left(\frac{800}{100} \right)^{\frac{1.4-1}{1.4}}$$

$$T_2 = 257.8^\circ\text{C}$$

$$P_{\text{Sat}, 20^\circ\text{C}} = 2.3392 \text{ kPa}$$

$$P_{v1} = 0.9 (2.3392) = 2.105 \text{ kPa}$$

$$w = \frac{0.622 P_v}{P - P_v} = \frac{0.622 (2.105)}{100 - 2.105}$$

$$w_1 = 0.0134 \text{ kg/kg dry air} = w_2$$

$$P_{\text{Sat}, 257.8^\circ\text{C}} = 4530 \text{ kPa}$$

200

18 cont

$$w_2 = \frac{0.622 (P_{2v})}{P_2 - P_{2v}}$$

$$w_2 P_2 - w_2 P_{2v} = 0.622 P_{2v}$$

$$w_2 P_2 = 0.622 P_{2v} + w_2 P_{2v}$$

$$w_2 P_2 = P_{2v} (0.622 + w_2)$$

$$P_{2v} = \frac{w_2 P_2}{0.622 + w_2} = \frac{0.134 (800)}{0.622 + 0.134}$$

$$P_{2v} = 16.87 \text{ kPa}$$

$$\phi_{\text{outlet}} = \frac{P_{2v}}{P_{2,\text{sat}}} = \frac{16.87 \text{ kPa}}{4530 \text{ kPa}} = \boxed{.372 \%}$$

28) Given Dry + Wet Bulb of Air

$$P = 95 \text{ kPa}$$

$$T_2 = 25^\circ\text{C} \quad T_1 = 17^\circ\text{C}$$

- FIND
- w_1
 - ϕ
 - h

25°	17°
1	2
$h_{f2} = 2460.64 \text{ kJ/kg}$	
$h_{f2} = 71.3552 \text{ kJ/kg}$	
$h_{g11} = 2546.5 \text{ kJ/kg}$	

Sol

$$w_1 = \frac{c_p (T_2 - T_1) + w_2 h_{f2}}{h_{g1} - h_{f2}}$$

$$w_2 = \frac{.622 P_{g2}}{P_2 - P_{g2}}$$

$$P_{g1, 25^\circ\text{C}} = 3.1698 \text{ kPa}$$

$$P_{g2, 17^\circ\text{C}} = 1.9591 \text{ kPa}$$

$$= \frac{.622 (1.9591)}{95 - 1.9591}$$

$$w_2 = .0131 \text{ kg/kg dry air}$$

$$w_1 = \frac{1.005 (17 - 25) + .0131 (2460.64)}{2546.5 - 71.3552}$$

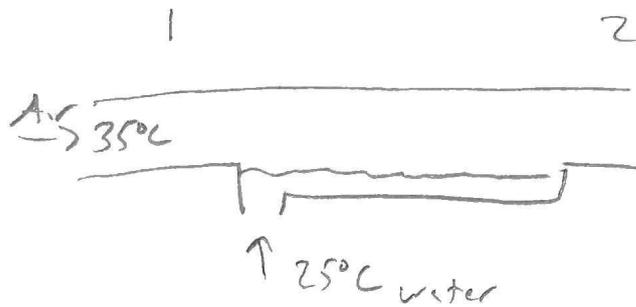
$$w_1 = .0098 \text{ kg H}_2\text{O/kg dry air}$$

$$\phi = \frac{w_1 P_2}{(.622 + w) P_{g1}} = \frac{(.0098)(95)}{(.622 + .0098)(3.1698)}$$

$$= \frac{.931}{2.072} = 46\%$$

$$h = h_g + w h_g = 1.005(25) + .0098(2546.5) = 49.8 \text{ kJ/kg}$$

32)



A diatomic saturation device

- leaves as saturated air mixture

$$P = 98 \text{ kPa}$$

FIND a) ϕ

b) w

$$T_1 = 35^\circ\text{C}$$

$$T_2 = 25^\circ\text{C}$$

$$h_{f2} = 2441.7$$

$$h_{g1} = 2564.6$$

$$h_{f2} = 104.83$$

$$w_1 = \frac{c_p (T_2 - T_1) + w_2 h_{f2}}{h_{g1} - h_{f2}}$$

$$w_2 = \frac{.622 P_{g2}}{P_2 - P_{g2}} = \frac{.622 (3.1698)}{98 - 3.1698} \quad P_{g2} = 3.1698 \text{ kPa}$$

$$w_2 = 0.0208 \text{ kg / kg dry air}$$

$$w_1 = \frac{1.005 (25 - 35) + 0.0208 (2441.7)}{2564.6 - 104.83}$$

$$w_1 = 0.0166 \text{ kg / kg dry air}$$

$$\phi = \frac{w_1 P}{(.622 + w_1) (P_{g1})} = \frac{0.0166 (98 \text{ kPa})}{(.622 + 0.0166) (3.1698)} = 80\%$$

14-39) Given: 1 atm

$$T_1 = 24^\circ\text{C}$$

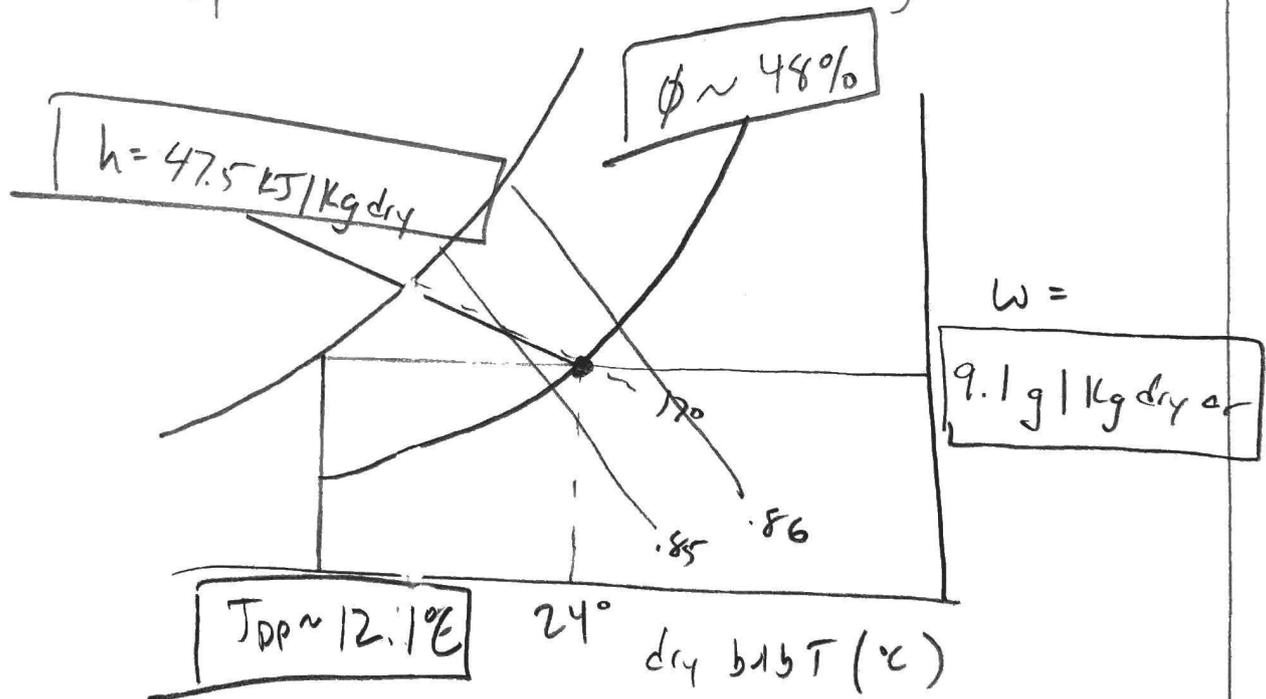
$$T_2 = 17^\circ\text{C}$$

$$T_{DB} = 24^\circ\text{C}$$

$$T_{WB} = 17^\circ\text{C}$$

Using chart find

- specific humidity (w)
- enthalpy (h)
- relative humidity (ϕ)
- dew point temp
- specific volume of air in m^3/kg



=> specific volume

$$\sim 0.855 \text{ m}^3/\text{kg}$$

14-41

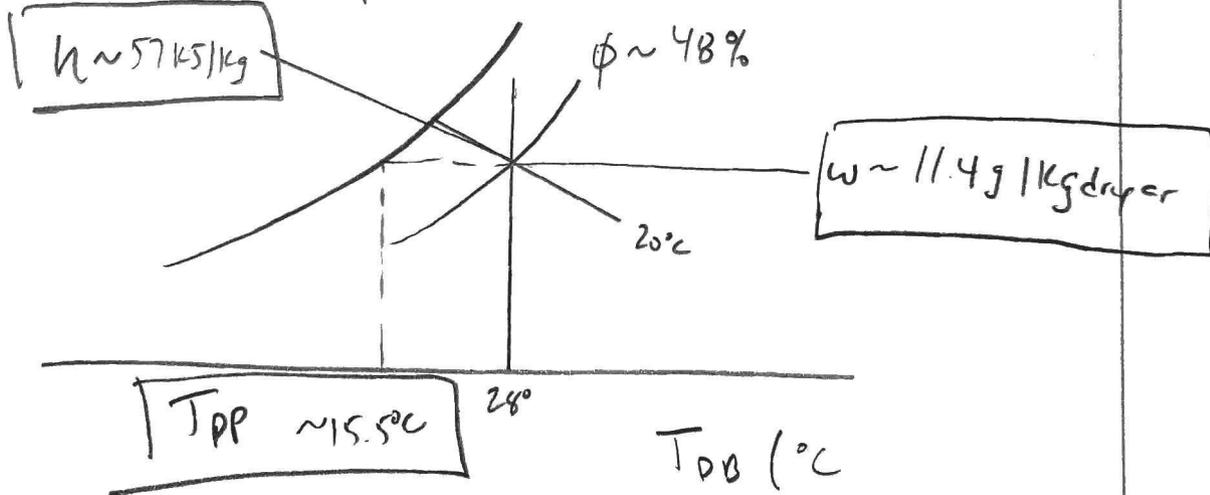
$$P = 1 \text{ atm}$$

$$T_{DB} = 28^\circ\text{C}$$

$$T_{WB} = 20^\circ\text{C}$$

FIND

- relative humidity
- humidity ratio
- enthalpy
- dew point temp
- water vapor pressure



$$P_v = \phi P_{v, 28^\circ\text{C}}$$

$$= 0.48 (3.81606)$$

$$P_v = 1.832 \text{ kPa}$$

$$P_{v, 28^\circ\text{C}} = 3.81606$$

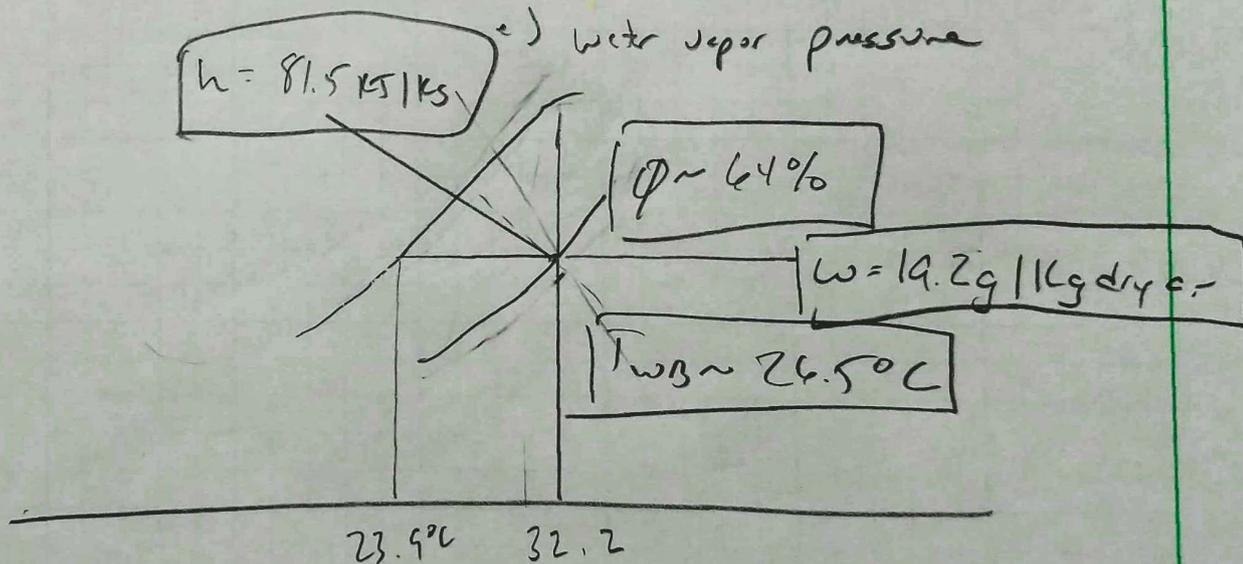
14.43 Air $P = 1 \text{ atm}$

$$T_{DB} = 90^\circ\text{F} = 32.2^\circ\text{C}$$

$$T_{DP} = 75^\circ\text{C} = 23.9^\circ\text{C}$$

Using chart Find

- ϕ
- w
- enthalpy
- T_{WB}
- water vapor pressure



$$1.891 \text{ m}^3 / \text{kg dry air}$$