

Chp 7.11

pump = 745 $\frac{\text{gal}}{\text{h}}$

pipe = 1" schedule 40 pipe

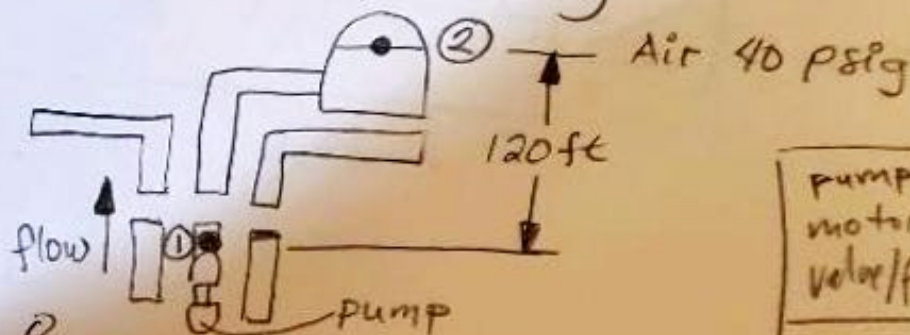
Energy loss of 10.5 $\frac{\text{lb-ft}}{\text{lb}}$

⑨ power delivered?

pump = 1hp, what is efficiency

Solution:

FBD



$$h_1 + \frac{P_1}{\gamma} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\gamma} + \frac{V_2^2}{2g} + z_2 + h_L + h_P$$

$$h_1 = \frac{P_2}{\gamma_w} + \frac{V_2^2}{2g} + z_2 + h_L$$

$$Q = \left(\frac{745 [\text{gal}]}{[\text{h}]} \right) \left(\frac{1 [\text{h}]}{60 [\text{min}]} \right) \left(\frac{1 \text{ ft}^3/\text{s}}{449 \frac{\text{gal}}{\text{min}}} \right) = 0.028 \frac{\text{ft}^3}{\text{s}}$$

$$h_1 = \frac{P_2}{\gamma_w} + \frac{Q_2^2}{A_2^2} + z_2 + h_L$$

$$h_1 = \frac{(40 \frac{\text{lb}}{\text{in}^2}) (\frac{144 \text{ in}^2}{1 \text{ ft}^2})}{62.4 [\frac{\text{lb}}{\text{ft}^3}]} + \frac{\left(\frac{0.028 [\frac{\text{ft}^3}{\text{s}}]}{0.006 \text{ ft}^2} \right)^2}{(2 (32.2 [\frac{\text{ft}}{\text{s}^2}]})} + 120 [\text{ft}] + 10.5 \frac{\text{lb-ft}}{\text{lb}}$$

pump = h_a
motor = h_p
valve/fitting = h_L

TABLE 7.1

$$f[\text{in}] = 0.006 [\text{ft}]$$

$$Q = \left(\frac{194}{\text{min}} \right) \left(\frac{1 \text{ ft}^3/\text{s}}{449 \frac{\text{gal}}{\text{min}}} \right)$$

$$Q = \frac{\text{ft}^3}{\text{s}}$$

Pump Efficiency
 $\eta_m = \frac{\text{Power delivered}}{\text{power put to pump}}$

$$1 \text{ PSI} = 144 \left[\frac{\text{lb}}{\text{ft}^2} \right]$$

$$\gamma_w = 62.4 \frac{\text{lb}}{\text{ft}^3}$$

$$h_f = 222.87 \text{ [ft]}$$

⑥ efficiency e_m if $P_I = 1 \text{ hp}$

$$e_m = \frac{P_A}{P_I} = \frac{h_f \gamma_w Q}{P_I} = \frac{(222.87 \text{ [ft]}) (62.4 \frac{\text{lb}}{\text{ft}^3}) (0.028 \frac{\text{ft}^3}{\text{s}})}{1 \text{ hp}}$$

$$e_m = \frac{(389.4 \frac{\text{ft} \cdot \text{lb}}{\text{s}})}{550 \frac{\text{ft} \cdot \text{lb}}{\text{s}}} = 0.7$$

~~1 hp~~

$$e_m = 0.7$$

7.16

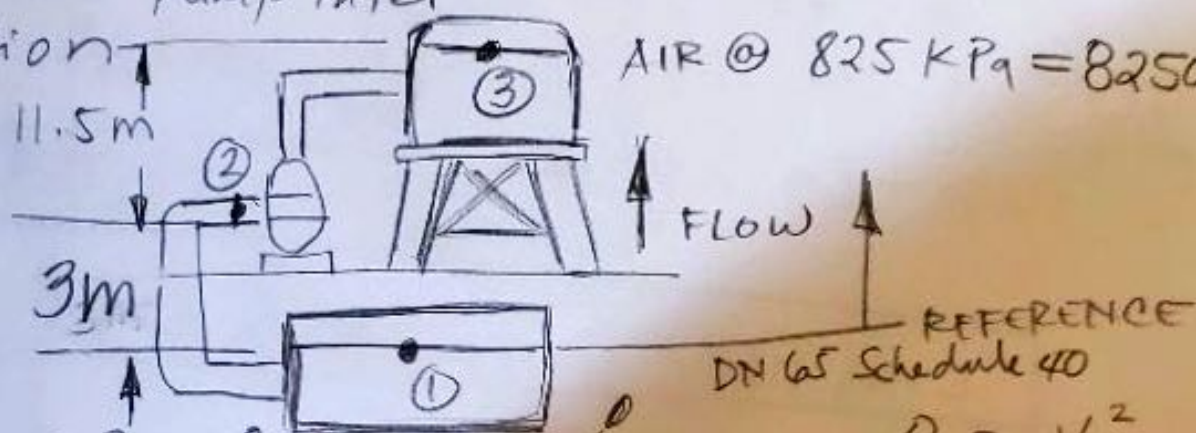
Problem: pump = $840 \frac{L}{min}$

$S_{g oil} = 0.85$

(a) Total loss = $4.2 \frac{N \cdot m}{N}$, power-delivered

(b) Energy suction pipe = $1.4 \frac{N \cdot m}{m}$, calculate the pressure @ the pump inlet

Solution: AIR @ $825 \text{ kPa} = 825000 \frac{N}{m^2}$



$$h_1 + \frac{P_1}{\gamma_w} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\gamma_w} + \frac{V_2^2}{2g} + z_2 + h_{L2} + \frac{P_3}{\gamma_w} + \frac{V_3^2}{2g} + z_3 + h_{L3}$$

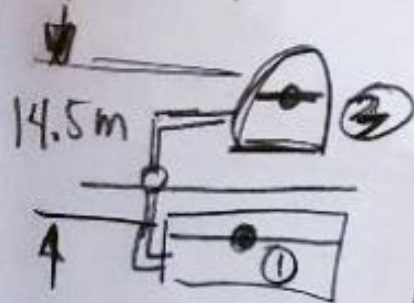
$$h_1 = \frac{P_2 + P_3}{\gamma_w} + \frac{V_3^2}{2g} + z_2 + z_3 + h_{L2} + h_{L3}$$

$$Q = \left(\frac{840 \text{ L}}{1 \text{ min}} \right) \left(\frac{1.0 \frac{m^3}{s}}{60000 \frac{L}{min}} \right) = 0.014 \left[\frac{m^3}{s} \right]$$

$$h_1 = \left(825000 \frac{N}{m^2} \right) + \frac{P_2}{\gamma_w} + \frac{\left(0.014 \left[\frac{m^3}{s} \right] \right)^2}{2 \left(9.81 \left[\frac{m}{s^2} \right] \right)} + 3m + 11.5m$$

$$+ 4.2 \frac{N \cdot m}{N} + 1.4 \frac{N \cdot m}{m}$$

FBD #1



$$h_1 + \frac{P_1}{\gamma_w} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\gamma_w} + \frac{V_2^2}{2g} + z_2 + h_{L2} + \frac{P_3}{\gamma_w}$$

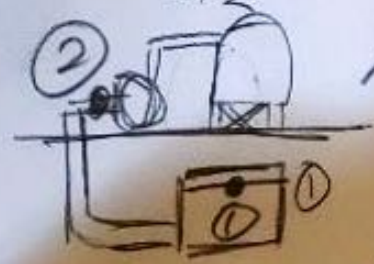
$$h_1 = \frac{P_3}{\gamma_w} + z_2 + h_{L2}$$

$$h_1 = 825000 \left[\frac{N}{m^2} \right]$$

$$(0.85) 9.81 \times 10^3 \left[\frac{N}{m^2} \right] + 14.5 [m] + 4.2 \left[\frac{N \cdot m}{N} \right]$$

$$h_1 = 99 + 18.7 [m] = 117.7 [m]$$

FBD #2



$$h_1 + \frac{P_1}{\gamma_w} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\gamma_w} + \frac{V_2^2}{2g} + z_2 + h_{L2} + \frac{P_3}{\gamma_w}$$

$$0 = \frac{P_2}{\gamma_w} + \frac{V_2^2}{2g} + z_2 + h_{L2}$$

$$0 = \frac{P_2}{(0.85) (9.81 \times 10^3 \left[\frac{N}{m^2} \right])} + \frac{(0.014 \left[\frac{m}{s} \right])^2}{2 (9.81 \left[\frac{m}{s^2} \right])} + 3 [m] + 1.4 \frac{m}{m}$$

$$0 = \frac{P_2}{8338.5 \left[\frac{N}{m^2} \right]} + \frac{1075.84 \frac{m^2}{s^2}}{19.62 \left[\frac{m}{s^2} \right]} + 4.4 [m]$$

$$0 = P_2 \left(\frac{1}{8338.5 \left[\frac{N}{m^2} \right]} \right) + 59.2 [m]$$

$$8338.5 \frac{N}{m^3}$$

$$x - 59.2 [m] = P_2 \left(\frac{1}{8338.5 \left[\frac{N}{m^3} \right]} \right) \left(8338.5 \frac{N}{m^3} \right)$$

$$P_2 = -493921.4 \left[\frac{N}{m^2} \right]$$

Chp 8

Prob 33

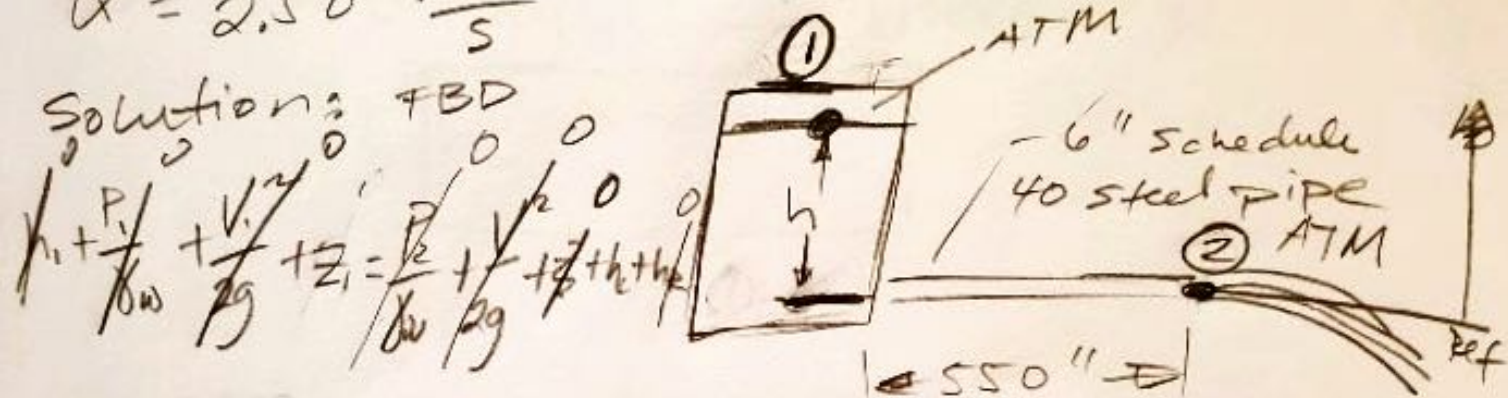
Problem: Water @ 80°F

Pipe = 6 in Schedule 40 steel pipe

* Energy loss due to friction
Calculate h above the pipe inlet to produce Q

$$Q = 2.50 \frac{\text{ft}^3}{\text{s}}$$

Solution: FBD



$$z_1 = -h_L$$

$$h_L = f \times \frac{L}{D} \times \frac{V^2}{2g}$$

$$Q = VA$$

$$V = \frac{Q}{A} = \frac{2.50 \frac{\text{ft}^3}{\text{s}}}{0.2006}$$

$$z_1 = f \times \frac{L}{D} \times \frac{V^2}{2g}$$

Page 188

$$* N_R = \frac{VD}{\nu} = \frac{\left(\frac{2.50 \frac{\text{ft}^3}{\text{s}}}{0.2006 \text{ ft}^2}\right) (0.5054 \text{ ft})}{9.15 \times 10^{-6} \frac{\text{ft}^2}{\text{s}}} = \frac{6.29 \text{ ft}^2}{9.15 \times 10^{-6} \frac{\text{ft}^2}{\text{s}}}$$

$$N_R = 688372 \frac{1}{\text{s}}$$

$$* \frac{D}{\epsilon} = \frac{0.5054 \text{ ft}}{1.5 \times 10^{-4} \text{ ft}} = 3369.3$$

$$f = \frac{0.25}{\left[\log \left(\frac{1}{(3.7)(3369.3)} + \left(\frac{5.74}{688572} \right)^{1/4} \right) \right]^2} = 0.016$$

$$h_L = f \times \frac{L}{D} \times \frac{V^2}{2g} = (0.016) \left(\frac{550 \text{ ft}}{.5054 \text{ ft}} \right) \left(\frac{\left(\frac{2.5 \text{ ft}^3}{5} \right)^{2/3}}{2(32.2 \text{ ft/s}^2)} \right)^2$$

$$h_L = 42 \text{ ft}$$

Chp 10.20 problem:

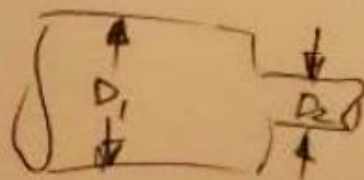
* Determine the energy loss for a sudden contraction from a DN 125 schedule 80 steel pipe to a DN 50 schedule 80 pipe for a $Q = 500 \frac{L}{min}$

	$\phi (mm)$	$\phi (m)$	Flow Area (m^2)
DN 125 =	122.3	.1223	1.173×10^{-2}
DN 50 =	49.3	.0493	1.905×10^{-3}

$$Q = \left(\frac{500 \frac{L}{min}}{min} \right) \left(\frac{1 \frac{m^3}{s}}{60000 \frac{L}{min}} \right) = .0083 \left[\frac{m^3}{s} \right]$$

* sudden contraction

$$h_L = K \left(\frac{V_2^2}{2g} \right)$$



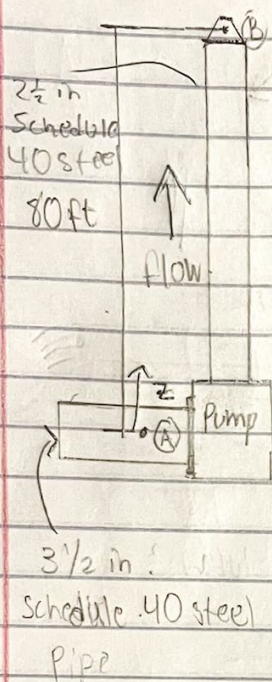
$$\frac{D_1}{D_2} = \frac{.1223 [m]}{.0493 [m]} = 2.48 [m]$$

$$V = \frac{Q}{A} = \frac{.0083 \left[\frac{m^3}{s} \right]}{1.905 \times 10^{-3} [m^2]} = 4.36 \frac{m}{s}$$

$$h_L = (.4) \left(\frac{(4.4 \left[\frac{m}{s} \right])^2}{2(9.8 \frac{m}{s^2})} \right) = .39 m$$

$$h_L = .39 m$$

8.44 The pressure at point B just ahead of the nozzle must be 25 psig for proper nozzle performance. Pressure at A is -3.5 psig
 $Q = 0.50 \text{ ft}^3/\text{s} + \eta = 4.0 \times 10^{-5} \text{ lb} \cdot \text{s}/\text{ft}^2$. The $SG = 1.026$ compute the



power delivered by the pump to the fluid considering friction energy loss.

$$E = 1.5 \times 10^{-4} \text{ ft}$$

$$V_A = \frac{Q}{A}$$

$$D_A = 0.2957 \text{ ft}$$

$$A_A = 0.06868 \text{ ft}^2$$

$$D_B = 0.2058 \text{ ft}$$

$$A_B = 0.03326 \text{ ft}^2$$

$$V_A = \frac{0.5 \text{ ft}^3/\text{s}}{0.06868 \text{ ft}^2}$$

$$V_A = 7.28 \text{ ft/s}$$

$$V_A A_A = V_B A_B$$

$$(7.28)(0.06868) = V_B (0.03326)$$

$$V_B = 15.0 \text{ ft/s}$$

$$SG = 1.026$$

$$(1.026)(1.44 \frac{\text{slug}}{\text{ft}^3})$$

$$\rho = 2.0 \frac{\text{lb} \cdot \text{s}^2}{\text{ft}}$$

$$V = \eta / \rho = \frac{4.0 \times 10^{-5} \frac{\text{lb} \cdot \text{s}}{\text{ft}^2}}{2.0 \frac{\text{lb} \cdot \text{s}^2}{\text{ft}}} = 2.0 \times 10^{-5} \text{ ft}^2/\text{s}$$

$$V = 2.0 \times 10^{-5} \text{ ft}^2/\text{s}$$

$$N_R = \frac{V D}{\nu} = \frac{(15 \text{ ft/s})(0.2058 \text{ ft})}{2.0 \times 10^{-5} \text{ ft}^2/\text{s}}$$

$$N_R = 1.54 \times 10^5$$

$$f = \frac{0.25}{\left[\log \left(\frac{1}{3.7 \left(\frac{0.2058 \text{ ft}}{7.5 \times 10^{-4} \text{ ft}} \right)} + \left(\frac{5.74}{(1.54 \times 10^5)^{0.9}} \right) \right] ^2}$$

$$f = 0.02047$$

$$h_L = f \cdot \frac{L}{D} \cdot \frac{V^2}{2g}$$

$$h_L = (0.02047) \left(\frac{80 \text{ ft}}{0.2058 \text{ ft}} \right) \left(\frac{15 \text{ ft/s}}{64.4 \text{ ft/s}^2} \right)$$

$$h_L = 27.8 \text{ ft} \quad h_A = \frac{504 \text{ lb/ft}^2}{64.4 \text{ lb/ft}^2} + \frac{(7.28 \text{ ft/s})^2}{2 \cdot 32.2 \text{ ft/s}^2} = \frac{3600 \text{ lb/ft}^2}{64.4 \text{ lb/ft}^2} + \frac{(15 \text{ ft/s})^2}{2 \cdot 32.2 \text{ ft/s}^2} + 80 \text{ ft}$$

$$\gamma = \rho g$$

$$\gamma = 2.0 \frac{\text{lb} \cdot \text{s}^2}{\text{ft}^3} \cdot 32.2 \text{ ft/s}^2 + 27.8 \text{ ft}$$

$$= 64.4 \frac{\text{lb}}{\text{ft}^3}$$

Next Page

$$h_A = 174.21 \text{ ft}$$

$$P_A = h_A \gamma Q$$

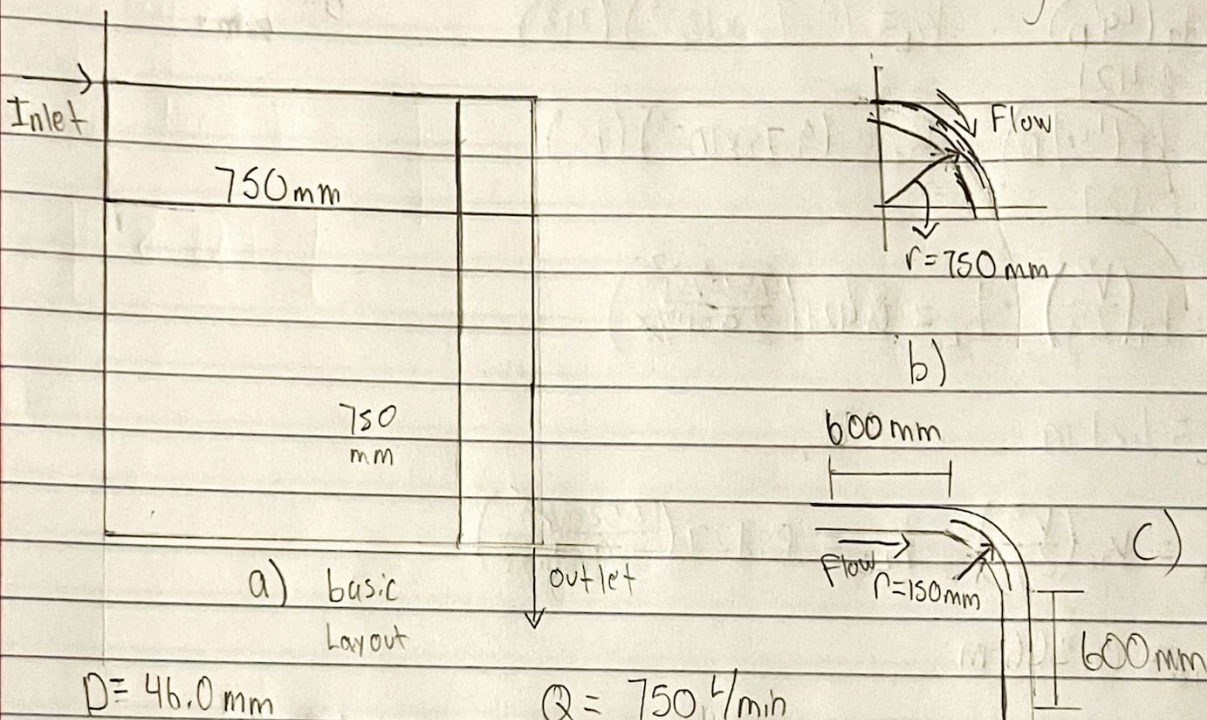
$$P_A = (174.21 \text{ ft}) (64.4 \text{ lb/ft}^3) (0.5 \text{ ft}^3/\text{s})$$

$$P_A = 5609.6 \frac{\text{ft} \cdot \text{lb}}{\text{s}}$$

$$P_A = 5609.6 \frac{\text{ft} \cdot \text{lb}}{\text{s}} \left| \frac{1 \text{ hp}}{550 \frac{\text{ft} \cdot \text{lb}}{\text{s}}} \right|$$

$$P_A = 10.2 \text{ hp}$$

The inlet and outlet a) are to be connected with a 50 mm OD x 2.0 mm wall copper tube to carry 750 l/min of propyl alcohol at 25°C. Evaluate the 2 schemes b) + c) with regard to the energy loss. Include the losses due to both the bend and the friction in the straight tube



$$\begin{aligned}
 D &= 46.0 \text{ mm} & Q &= 750 \text{ l/min} \\
 D_o &= 50.0 \text{ mm} & Q &= 750 \text{ l/min} = 1 \text{ m}^3/\text{s} \\
 A &= 1.662 \times 10^{-3} \text{ m}^2 & & 60,000 \text{ l/min}
 \end{aligned}$$

$$\begin{aligned}
 Q &= VA & V &= \frac{Q}{A} \\
 V &= 7.52 \text{ m/s} & Q &= 0.0125 \text{ m}^3/\text{s} \\
 & & V &= \frac{0.0125 \text{ m}^3/\text{s}}{1.662 \times 10^{-3} \text{ m}^2}
 \end{aligned}$$

$$\begin{aligned}
 L/D &= 750 \text{ mm} / 46 \text{ mm} = 16.3 \\
 L_e/D &= 43
 \end{aligned}$$

$$\begin{aligned}
 L/D &= 150 \text{ mm} / 46 \text{ mm} = 3.26 \\
 L_e/D &= 13
 \end{aligned}$$

$$\epsilon = 1.5 \times 10^{-6}$$

$$N_R = \frac{VD}{\nu} \quad V = 7.10 \times 10^{-7} \text{ m}^2/\text{s}$$

$$N_R = \frac{(7.52 \text{ m/s})(0.046 \text{ m})}{7.10 \times 10^{-7} \text{ m}^2/\text{s}}$$

$$N_R = 4.87 \times 10^5$$

Next page

$$f_T = \frac{0.25}{\left[\log \left(\frac{1}{3.7 \left(\frac{0.046 \text{ m}}{1.2 \times 10^{-3} \text{ m}} \right) + \left(\frac{5.74}{4.87 \times 10^6 \text{ Pa}} \right)} \right) \right]^2}$$

$$f_T = 9.78 \times 10^{-3}$$

$$k_b = f_T (L_b/D) \quad k_b = (9.78 \times 10^{-3}) (43)$$

$$k_b = 0.421$$

$$k_c = f_T (L_c/D) \quad k_c = (9.78 \times 10^{-3}) (13)$$

$$k_c = 0.127$$

$$h_{Lb} = k_b \left(\frac{V^2}{2g} \right) \quad h_{Lb} = 0.421 \left(\frac{(7.52 \text{ m/s})^2}{2 \cdot 9.81 \text{ m/s}^2} \right)$$

$$h_{Lb} = 1.21 \text{ m}$$

$$h_{Lc} = k_c \left(\frac{V^2}{2g} \right) \quad h_{Lc} = 0.127 \left(\frac{(7.52 \text{ m/s})^2}{2 \cdot 9.81 \text{ m/s}^2} \right)$$

$$h_{Lc} = 0.366 \text{ m}$$

$$h_{Ls} = \left(f_T \frac{L}{D} \cdot \frac{V^2}{2g} \right) \cdot 2 \quad h_{Ls} = \left[(9.78 \times 10^{-3}) \left(\frac{0.60 \text{ m}}{0.046 \text{ m}} \right) \left(\frac{(7.52 \text{ m/s})^2}{2 \cdot 9.81 \text{ m/s}^2} \right) \right] \cdot 2$$

$$h_{Ls} = (0.368) \cdot 2$$

$$h_{Ls} = (0.368) (2)$$

$$h_{Ls} = 0.735 \text{ m}$$

$$h_{L\text{total}} = h_{Ls} + h_{Lc}$$

$$h_{L\text{total}} = 0.735 \text{ m} + 0.366 \text{ m}$$

$$h_{L\text{total}} = 1.1 \text{ m}$$